Emulsification of the Mixture of Catalytic Pyrolysis Oil Obtained under Methane and Nitrogen Environment in Diesel Using Span 80 and Atlox 4916 as Surfactants

Abid Farooq and Young-Kwon Park

School of Environmental Engineering, University of Seoul, Seoul 02504, Republic of Korea (Received April 1, 2021; Revised April 24, 2021; Accepted April 26, 2021)

Abstract

Emulsions were prepared using a mixture of bio-oil obtained from the pyrolysis of sawdust in an N_2 environment and *Quercus mongolica* in a CH_4 environment for both non-catalytic and catalytic cases. Both prepared emulsions were examined by measuring the physical stability and Fourier transform infrared spectroscopy. The emulsion with HLB 5.8 (Span 80 and Atlox 4916) for the ratio of bio-oil (B-oil and C-oil): surfactant: diesel = 10%: 3%: 87% showed stability for 15 days. Combining oils produced in N_2 and CH_4 environments could be a potential solution for generating high-quality emulsions with a high heating value.

Keywords: Emulsification, Bio-oil, Diesel, Catalytic pyrolysis

1. Introduction

The stringent environmental laws coming in place due to major environmental concerns have made it inevitable to search for sustainable energy resources[1-3]. Rapid pyrolysis is a thermochemical conversion process for the generation of bio-oil from waste biomass resources and is a potential candidate for replacing fossil fuels[4-7]. On the other hand, the bio-oil obtained from pyrolysis cannot be used directly as a fuel because of its high viscosity (40~100 cP), high oxygen content (40~60 wt.%), lower chemical and thermal stability, lower high heating value (16~19 MJ/kg), and higher water content (15~35 wt.%)[8,9]. Hence, upgrading is required to improve its properties for use as an engine fuel.

Zeolites provide a better solution for the upgrading of oil owing to their lower H/C_{eff} (hydrogen-to-carbon effective ratios $(0\sim0.3)[10-12]$. Moreover, methane is an inexpensive source of hydrogen that can be obtained by decomposition catalytically using metal-loaded zeolites [13]. Furthermore, methane pyrolysis under zeolites and metal-loaded zeolites enhance the generation of benzene, toluene, ethylbenzene, and xylene (BTEX), which ultimately enhances the quality of bio-oil[8,13].

Emulsification is a process to use the bio-oil obtained from pyrolysis [14] directly in a diesel engine as a mixture of bio-oil and diesel. In general, bio-oil and diesel do not mix because of the aforementioned properties. Hence surfactants/emulsifiers are required to make stable bio-oil and diesel emulsions[15-17]. Surfactants are selected based on their hydrophilic/lipophilic balance (HLB)[9,18]. Emulsifiers can be ap-

This study evaluated a mixture of bio-oil obtained from the pyrolysis of different waste biomass resources, such as sawdust and *Quercus mongolica*, in different gas environments (N₂ and CH₄). The bio-oil was produced for both non-catalytic and catalytic (HZSM-5 and Ni/HZSM-5) cases. To the best of the author's knowledge, no study has been performed to prepare emulsions with a mixture of bio-oils obtained from pyrolysis in different environments (N₂ and CH₄) in diesel. All the emulsions were prepared in an ultrasonicator reactor, observed both physically and with Fourier transform infrared (FTIR) spectroscopy, and stored at room temperature. The heating value was measured to check the feasibility of oil for diesel engine use.

2. Experimental

2.1. Production of catalytic upgraded oil

Both non-catalytic and catalytic pyrolysis oil were produced using sawdust (SD) as a feedstock in an N_2 environment and *Quercus mongolica* (QM) as a feedstock in a CH₄ environment at 550–650 $^{\circ}$ C. The catalysts used were HZSM-5 and Ni/HZSM-5. A mixture of bio-oil was prepared from pyrolysis under N_2 and CH₄ in the ratio of (Pyrolysis under N_2 /pyrolysis under CH₄ = 5 g/1.5 g). The following mixtures were prepared, and their stability in diesel was assessed in a laboratory-scale ultrasonicator:

pISSN: 1225-0112 eISSN: 2288-4505 @ 2021 The Korean Society of Industrial and Engineering Chemistry. All rights reserved.

plied individually or with a combination of two or more emulsifiers to obtain the optimal HLB for stabilizing bio-oil in diesel[19]. Researchers have tested several scenarios to develop emulsions using a range of emulsifiers under different conditions and reactor systems[9,15,20,21] and have produced stable emulsions. On the other hand, more insight is needed to use the produced emulsions as a replacement fuel in diesel engines.

[†] Corresponding Author: University of Seoul, School of Environmental Engineering, Seoul 02504, Republic of Korea Tel: +82-2-6490-2870 e-mail: catalica@uos.ac.kr

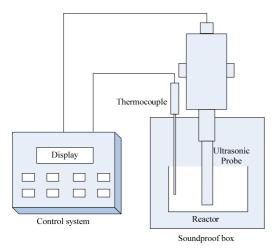


Figure 1. Experimental setup for the ultrasonicator.

- A-oil = SD Pyrolysis NC at 600 $^{\circ}$ C under N₂ + QM Pyrolysis over Ni/HZSM5 at 600 $^{\circ}$ C under CH₄ In-situ
- B-oil = SD Pyrolysis over HZSM-5 at 600 $^{\circ}$ C under N₂ + QM Pyrolysis over HZSM-5 (550 $^{\circ}$ C) at 650 $^{\circ}$ C under CH₄ Ex-situ
- · C-oil = SD Pyrolysis over HZSM-5 at 600 $^{\circ}$ C under N₂ + QM Pyrolysis over Ni/HZSM-5 (500 $^{\circ}$ C) at 600 $^{\circ}$ C under CH₄ Ex-situ
- D-oil = SD Pyrolysis NC at 600 $^{\circ}$ C under N₂ + QM Pyrolysis NC at 650 $^{\circ}$ C under CH₄

A combination of Span 80 and Atlox 4916 with HLB 5.8 was tested to obtain a stable emulsion with the above-mentioned mixtures of bio-oils.

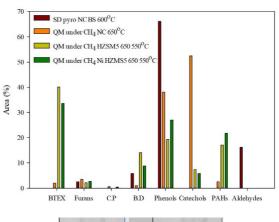
2.2. Emulsions preparation

The experimental setup consists of an ultrasonic probe with a thermocouple attached in a soundproof box. The ultrasonic probe consists of a 6 mm horn. Parameters, such as the ultrasonic power and time for an ultrasonic wave, can be adjusted using a digital control system, as shown in Figure 1.

The experiments were performed in a neck flask reactor with an ultrasonic probe and thermocouple. The HLB of 5.8 (Span 80 and Atlox 4916) was chosen based on previous studies for obtaining a stable emulsion[18]. A preset amount of a mixture of bio-oils (10%) was added to the blend and brought under the ultrasonic probe at 40% power. The ultrasonic pulse was controlled, so a pulse was generated (ultrasonic time) for 3 s and then off (gap time) for 1 s and on again for 3 s. The process was continued for 10 min. Finally, the blend was inserted into a 100 mL cylinder to observe the extent of stratification (phase separation) every 10 min. The stability of the emulsion was also tested periodically by FTIR spectroscopy to ensure stability.

3. Results and Discussions

Gas chromatography/mass spectrometry (GCMS) analysis of the bio-oils (Figure 2) produced under N_2 revealed phenols as the major



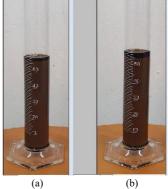


Figure 2. GCMS Analysis and phase separated emulsions (a) HLB 5.8 A-oil: 10% SA: 3% D: 87% (b) HLB 5.8 D-oil: 10% SA: 3% D: 87%.

compound. In contrast, the oils produced under CH_4 revealed benzene, toluene, ethylbenzene, and xylene (BTEX) and phenols as the major compounds, especially for the catalytic cases, HZSM5 and Ni-HZSM-5. The increase in the BTEX content under CH_4 environment pyrolysis is attributed to the increase in the H/C atomic ratio of feedstock due to enhanced catalytic and thermal cracking of CH_4 into H_2 . BTEX improves the quality of oil; hence, the stability of the bio-oil mixture produced under N_2 and CH_4 was tested in diesel.

Figure 3 shows the physical stability and FTIR spectra for the emulsions prepared through B-oil and C-oil. The HLB value of 5.8 for several mixtures of bio-oils (A-oil, B-oil, C-oil, and D-oil) was tested to check their stability in diesel. The emulsifier amount was kept minimal (3%) to maintain the optimal viscosity of the emulsion. The emulsions for A-oil and D-oil showed stratification (phase separation) within one day, as shown in Figure 2. In contrast, stable emulsions were observed when Span 80 and Atlox 4916 for HLB 5.8 [bio-oil (B and D): surfactant : diesel = 10% : 3% : 87%] were employed. The emulsions prepared through B-oil and C-oil showed stability for more than 15 days, observed by both physical state of emulsions and through FTIR spectroscopy. The peaks in the range of 1352~1448 cm⁻¹ were due to vibration of asymmetric, symmetric or scissoring bending of C-H. While the peak at 1744 cm⁻¹ reveals the stretching of carbonyl group. Moreover, the peaks in the range of 2845~2961 cm⁻¹ reveals the stretching of aliphatic C-H[18]. The FTIR peaks showed no change in in-

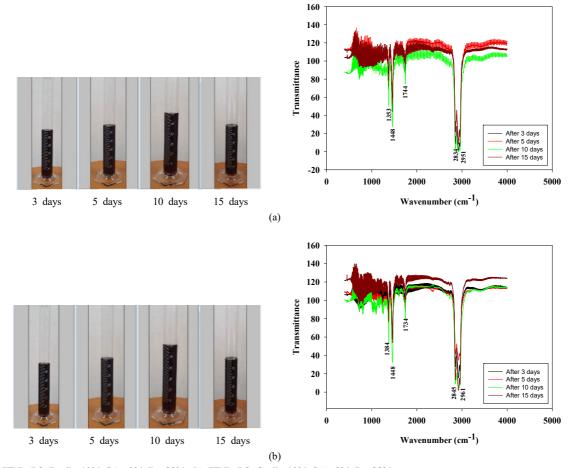


Figure 3. (a) HLB 5.8 B-oil: 10% SA: 2% D: 88% (b) HLB 5.8 C-oil: 10% SA: 2% D: 88%

tensity for 15 days, confirming the stability of the prepared emulsions. The presence of BTEX-containing oil (catalytic CH₄ pyrolysis) in the mixture enhanced the quality of the oil, thereby producing a stable emulsion with a higher heating value.

The heating values of the emulsion prepared using B-oil and C-oil were 45.26 MJ/kg and 45.02 MJ/kg, which are comparable to commercial diesel, 45.65 MJ/kg. Therefore, the prepared emulsion can be a potential candidate for use as a fuel in diesel engines.

4. Conclusions

Emulsions were prepared using a combination of bio-oils in N_2 and CH_4 environments for both non-catalytic and catalytic cases. The emulsions for the catalytic oils (B-oil and C-oil) were stable for 15 days. The addition of pyrolysis-derived oil under CH_4 provided an emulsion with a comparable heating value to diesel, highlighting its potential for commercial use in diesel engines.

Acknowledgments

This work was supported by the New and Renewable Energy Core Technology Program of the Korea Institute of Energy Technology Evaluation and Planning (KETEP), granted financial resource from the Ministry of Trade, Industry & Energy, Republic of Korea (No. 2017-3010092430).

References

- A. Abdullah, A. Ahmed, P. Akhter, A. Razzaq, M. Zafar, M. Hussain, N. Shahzad, K. Majeed, S. Khurrum, M. S. A. Bakar, and Y.-K. Park, Bioenergy potential and thermochemical characterization of lignocellulosic biomass residues available in Pakistan, Korean J. Chem. Eng., 37, 1899-1906 (2020).
- G. Özsin, M. Kılıç, E. Apaydin-Varol, A. E. Pütün, and E. Pütün, A thermo-kinetic study on co-pyrolysis of oil shale and polyethylene terephthalate using TGA/FT-IR, *Korean J. Chem. Eng.*, 37, 1888-1898 (2020).
- Y. Liu, Y. Wu, M. Su, W. Liu, X. Li, and F. Liu, Developing Brønsted-Lewis acids bifunctionalized ionic liquids based heteropolyacid hybrid as high-efficient solid acids in esterification and biomass conversion, J. Ind. Eng. Chem., 92, 200-209 (2020).
- S.-K. Choi, Y.-S. Choi, Y.-W. Jeong, S.-Y. Han, and Q. V. Nguyen, Combustion characteristics of fuel blends of coffee waste-derived oil and polystyrene foam waste-derived oil in a pilot-scale burner, J. Korea Soc. Waste Manag., 37, 574-582 (2020).
- 5. L. Zhu and Z. Zhong, Effects of cellulose, hemicellulose and lig-

- nin on biomass pyrolysis kinetics, Korean J. Chem. Eng., 37, 1660-1668 (2020).
- Q. K. Tran, S. Han, H. V. Ly, S.-S. Kim, and J. Kim, Hydrodeoxygenation of a bio-oil model compound derived from woody biomass using spray-pyrolysis-derived spherical γ-Al₂O₃-SiO₂ catalysts, J. Ind. Eng. Chem., 92, 243-251 (2020).
- L. Santamaria, G. Lopez, A. Arregi, M. Artetxe, M. Amutio, J. Bilbao, and M. Olazar, Catalytic steam reforming of biomass fast pyrolysis volatiles over Ni-Co bimetallic catalysts, *J. Ind. Eng. Chem.*, 91, 167-181 (2020).
- 8. R. S. Tshikesho, A. Kumar, R. L. Huhnke, and A. Apblett, Catalytic co-pyrolysis of red cedar with methane to produce upgraded bio-oil, *Bioresour. Technol.*, **285**, 121299 (2019).
- B.-J. Lin, W.-H. Chen, W. M. Budzianowski, C.-T. Hsieh, and P.-H. Lin, Emulsification analysis of bio-oil and diesel under various combinations of emulsifiers, *Appl. Energy*, 178, 746-757 (2016).
- C. Song, M. Y. Gim, Y. H. Lim, and D. H. Kim, Enhanced yield of benzene, toulene, and xylene from the co-aromatization of methane and propane over gallium supported on mesoporous ZSM-5 and ZSM-11, Fuel, 251, 404-412 (2019).
- Y.-T. Cheng, J. Jae, J. Shi, W. Fan, and G. W. Huber, Production of renewable aromatic compounds by catalytic fast pyrolysis of lignocellulosic biomass with bifunctional Ga/ZSM-5 catalysts, *Angew. Chem. Int.*, 51, 1387-1390 (2012).
- G. J. Woo and Y.-M. Kim, Effect of torrefaction on the catalytic pyrolysis of miscanthus over HZSM-5 and HY, *J. Korea Soc.* Waste Manag., 37, 542-548 (2020).
- S. Moogi, J. Jae, H. P. R. Kannapu, A. Ahmed, E. D. Park, and Y.-K. Park, Enhancement of aromatics from catalytic pyrolysis of yellow poplar: Role of hydrogen and methane decomposition, *Bioresour. Technol.*, 315, 123835 (2020).
- 14. Y.-H. Lee, C.-H. Jeong, H.-D. Jin, G. Y. Jeong, H.-J. Byeon, H.-M. Kim and D.-W. Jeong, A study on the optimization of fast pyrolysis system and deoxygenation for bio-oil production of unused agricultural by-products, *J. Korea Soc. Waste Manag.*, 37, 531-541 (2020).

- M. Ikura, M. Stanciulescu, and E. Hogan, Emulsification of pyrolysis derived bio-oil in diesel fuel, *Biomass Bioenergy*, 24, 221-232 (2003).
- K. Liu, W. Zhao, T. Guo, Q. Lei, Y. Guan, D. Wang, M. Cui, S. Fu, J. Zhao, Z. Zong, and X. Wei, Emulsification and performance measurement of bio-oil with diesel, *Waste Biomass Valori.*, 12, 2933-2944 (2019).
- 17. X. Jiang and N. Ellis, Upgrading bio-oil through emulsification with biodiesel: Mixture production, *Energy Fuels*, **24**, 1358-1364 (2010).
- A. Farooq, H. W. Lee, J. Jae, E. E. Kwon, and Y.-K. Park, Emulsification characteristics of ether extracted pyrolysis-oil in diesel using various combinations of emulsifiers (span 80, atlox 4916 and zephrym pd3315) in double reactor system, *Environ. Res.*, 184, 109267 (2020).
- Q. Yin, S. Wang, X. Li, Z. Guo, and Y. Gu, Review of bio-oil upgrading technologies and experimental study on emulsification of bio-oil and diesel, 2010 Int. Conf. Opt. Image Proce., pp 343-347 (2010).
- Y. Li, T. Wang, W. Liang, C. Wu, L. Ma, Q. Zhang, X. Zhang, and T. Jiang, Ultrasonic preparation of emulsions derived from aqueous bio-oil fraction and 0# diesel and combustion characteristics in diesel generator, *Energy Fuels*, 24, 1987-1995 (2010).
- Z. G. Guo, S. R. Wang, and X. Y. Wang, Emulsification of bio-oil heavy fraction with diesel by mechanical and ultrasonic technologies, *Appl. Mech. Mater.*, 316-317, 1133-1137 (2013).

Authors

- Abid Farooq; M.Sc., Graduate Student, School of Environmental Engineering, University of Seoul, Seoul 02504, Republic of Korea; abid.chem.eng@gmail.com
- Young-Kwon Park; Ph.D., Professor, School of Environmental Engineering, University of Seoul, Seoul 02504, Republic of Korea; catalica@ uos.ac.kr