

ORIGINAL ARTICLE

Efficient cell design and fabrication of concentration-gradient composite electrodes for high-power and high-energy-density all-solid-state batteries

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All-solid-state batteries are promising energy storage devices in which high-energy-density and superior safety can be obtained by efficient cell design and the use of nonflammable solid electrolytes, respectively. This paper presents a systematic study of experimental factors that affect the electrochemical performance of all-solid-state batteries. The morphological changes in composite electrodes fabricated using different mixing speeds are carefully observed, and the corresponding electrochemical performances are evaluated in symmetric cell and half-cell configurations. We also investigate the effect of the composite electrode thickness at different charge/discharge rates for the realization of all-solid-state batteries with high-energy-density. The results of this investigation confirm a consistent relationship between the cell capacity and the ionic resistance within the composite electrodes. Finally, a concentration-gradient composite electrode design is presented for enhanced power density in thick composite electrodes; it provides a promising route to improving the cell performance simply by composite electrode design.

KEYWORDS

all-solid-state batteries, composite electrode, concentration gradient, energy storage devices, solid electrolytes

1 | INTRODUCTION

All-solid-state batteries with a bipolar stacked configuration are promising next-generation secondary batteries owing to their high-energy-density [1–4]. In contrast to liquid electrolytes in conventional lithium-ion batteries, the solid electrolytes in all-solid-state batteries make it possible to design a highly compact cell, which enables reduction of the volumetric cell capacity [5–7]. To achieve this, it is essential to develop solid electrolytes with electrochemical

properties comparable to those of liquid electrolytes. To this end, researchers have performed intensive studies that have produced various solid electrolytes, such as inorganic oxide or sulfide solid electrolytes, organic polymeric electrolytes, and gel electrolytes [8–11]. In addition, an important issue in fabricating all-solid-state batteries with superior performance is the effective design of the composite electrode, and specifically of the spatial arrangement of individual composite components. In conventional lithium-ion batteries with liquid electrolytes, liquid electrolyte flow enables the formation of

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a continuous ionic pathway within the electrodes and conformal contact with the active materials in the electrodes, resulting in facile transport of lithium ions within the electrodes and low charge transfer resistance between the active materials and the liquid electrolyte. However, these advantages are absent when solid electrolytes are used.

To obtain a continuous ionic pathway and conformal contact, the solid-state electrodes need to include solid electrolytes as well as active materials [12]. Therefore, the fabrication method of the composite electrode becomes a crucial concern [13]. For example, the mixing processes are closely related to the distribution of each electrode component, and the cell specifications, such as the compositions of the solid electrolyte and active material and the thickness of the composite electrodes, can significantly affect the cell performance. To address these issues, various approaches have been suggested, for example, direct coating of solid electrolytes on active materials and infiltration of solid electrolytes within prefabricated electrodes [6,10,14–17].

Here we present a systematic study of the formation of composite electrodes with reasonable performance using electrochemical impedance measurement and morphological observation. The study confirms that the cell performance depends strongly on the mixing conditions of the electrode and that a mild mixing process is desirable. In addition, we studied the dependence of the cell performance on the electrode thickness, which is strongly related to the ion transport within the composite electrodes. On the basis of the results, we propose concentration-gradient composite electrodes. A composite configuration with a high concentration of the solid electrolyte near the solid electrolyte layer sandwiched between the anode and the cathode enables facile ion transport to the active materials within the composite electrodes, improving the cell rate performance.

2 | EXPERIMENTAL SECTION

2.1 | Fabrication of all-solid-state batteries

All syntheses were conducted in an argon-filled glove box (MBraun). $\text{Li}_2\text{S}-\text{P}_2\text{S}_5$ glass ceramics (LPS) was prepared by conventional mechanical milling and subsequent heat treatment [18]. For mechanical milling of stoichiometric amounts of the Li_2S (Sigma-Aldrich, 99.98%) and P_2S_5 (Sigma-Aldrich, 99%) precursors, a planetary ball mill (Pulverisette 7PL, Fritsch GmbH) was used with 5 mm zirconia balls. The rotation speed was 800 rpm, and the mixing time was 10 hours. The resulting mixture was heat-treated at 270 °C for 2 hours. To obtain composite electrodes, the active material and solid electrode were mixed at various weight ratios using a Thinky mixer with 5 mm zirconia balls for 20 minutes. The composite anode was demonstrated using natural graphite (NG).

To fabricate an all-solid-state anode half-cell, composite powders were spread on pre-pelletized LPS (150 mg) and pelletized by mechanical pressing (over 300 MPa) [19]. The amount of composite powder determined the loading level of the active material and the thickness of the composite electrode. The thickness of the composite electrode was measured by a conventional micrometer caliper. Lithium metal (300 μm thickness, Honjo Metal Co.) was attached to the other surface of the pre-pelletized LPS. To obtain a concentration-gradient composite electrode, repeated processes of spreading and pelletization of the composite powders with different blending ratios were performed. A concentration-gradient composite electrode with a three-layered composite structure was designed, and the composite electrodes were fabricated at a thickness of $\sim 33 \mu\text{m}$ regardless of the blending ratio.

2.2 | Characterization

Scanning electron microscopy (SEM, Hitachi S-4800) and energy-dispersive X-ray spectroscopy (EDS, Bruker XFlash 6i100) were used for morphological observation and elemental mapping, respectively. The ionic conductivity was determined from complex impedance spectra measured using a frequency response analyzer (Solartron HF 1225 Gain-Phase Analyzer) in a frequency range of 10^{-1} to 10^5 Hz at room temperature. The electrochemical performance of the all-solid-state batteries was investigated using a cycle tester (Toyo Systems) at 60 °C.

3 | RESULTS AND DISCUSSION

To determine the ionic transport properties of the composite electrodes, composite symmetric cells were used (Figure 1A). In a full-cell configuration with different anodes and cathodes, the impedance can be measured, but in this case, the reaction complexity of individual electrodes generally makes precise analysis difficult [20,21]. To circumvent this issue, symmetric cells with identical electrodes at each end of the solid electrolyte layer can be used. Thus, we fabricated a composite symmetric cell consisting of NG and LPS to evaluate the ionic transport within the composite electrodes.

According to the transmission line model (TLM) without Faradaic reactions, the impedance of the composite electrode in the composite symmetric cell, $Z_{\text{composite}}$, is given by [20–22]

$$Z_{\text{composite}} = R_{\text{electrolyte}} + \sqrt{\frac{R_{\text{ion}}}{i\omega C_{\text{dl}}}} \coth \sqrt{R_{\text{ion}} i\omega C_{\text{dl}}}, \quad (1)$$

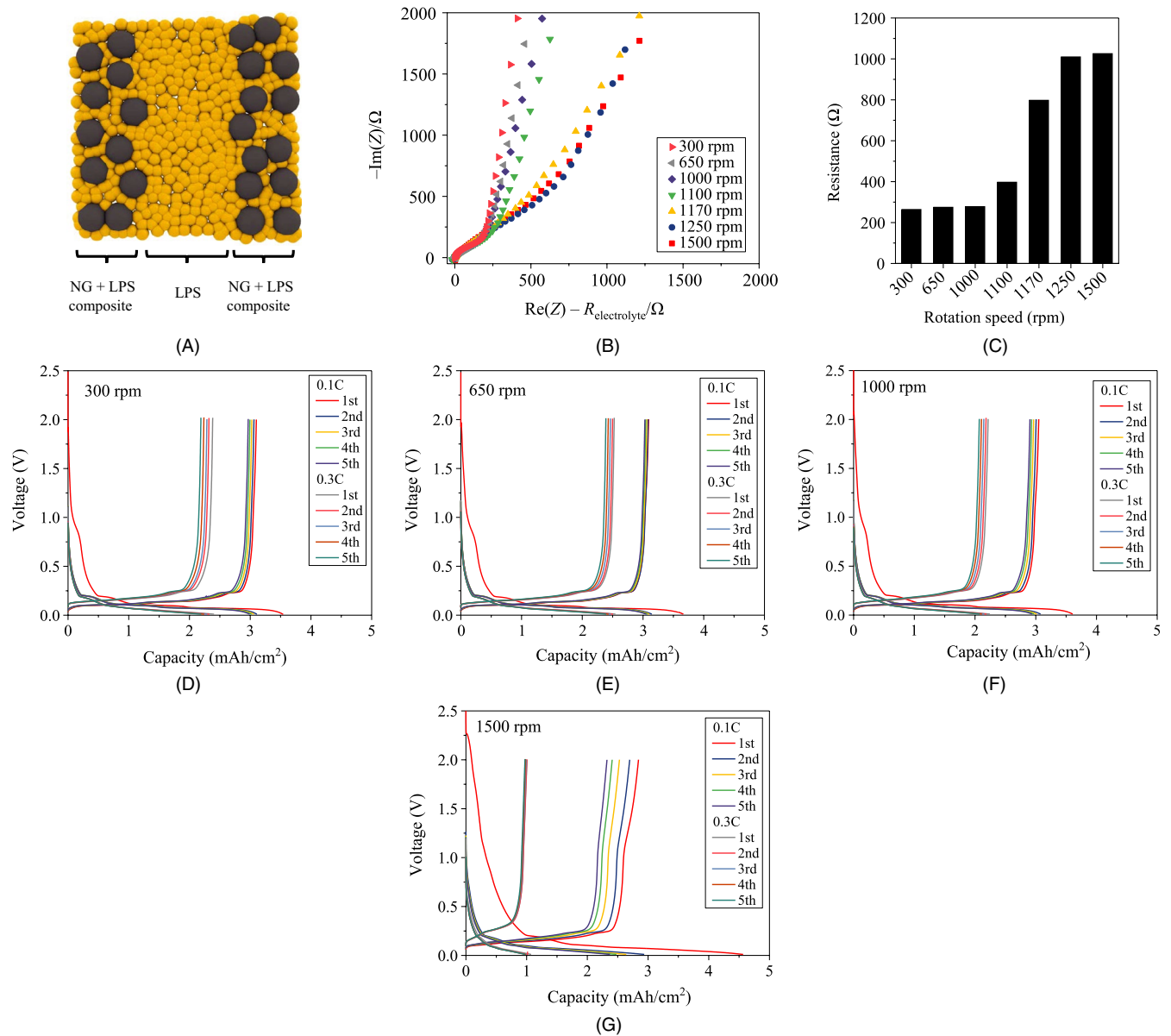


FIGURE 1 (A) Schematic illustration of composite symmetric cell, (B) impedance results of composite electrodes for various mixing conditions, and (C) corresponding resistance calculated from TLM analysis. (D–G) charge/discharge profiles of composite electrodes

where ω is the angular frequency, $R_{\text{electrolyte}}$ is the bulk ion transport resistance of the middle solid electrolyte layer, R_{ion} is the total ion transport resistance within the composite electrodes, and C_{dl} is the total double-layer capacitance at the interface between the active material and the solid electrolyte. The capacitances can be replaced by constant phase elements. The total ion transport resistance can be extracted from the real part of the impedance in the low-frequency regime as follows:

$$Z'_{\omega \rightarrow 0} = R_{\text{electrolyte}} = \frac{1}{3} R_{\text{ion}} \quad (2)$$

By using this approximation of the impedance results, the ion transport properties of the composite electrodes can be

obtained by measuring the impedance of the symmetric cells. Seven samples with NG as the active material (60 wt%) and LPS as the solid electrolyte (40 wt%) were prepared under different mixing conditions (300, 650, 1000, 1100, 1170, 1250, and 1500 rpm), and the ion transport properties were tested in the symmetric configuration. The loading level of each composite electrode was controlled at $15.2 \text{ mg}/\text{cm}^2$, and the corresponding composite thickness was $\sim 63 \mu\text{m}$. As shown in Figure 1B, these samples did not show any charge transfer reaction, so the approximation without Faradaic reactions can be used to describe our composite electrode [21]. The three samples with mixing conditions of 300, 650, and 1000 rpm exhibited similar profiles, but the other samples were different. Using the TLM approximation, we calculated

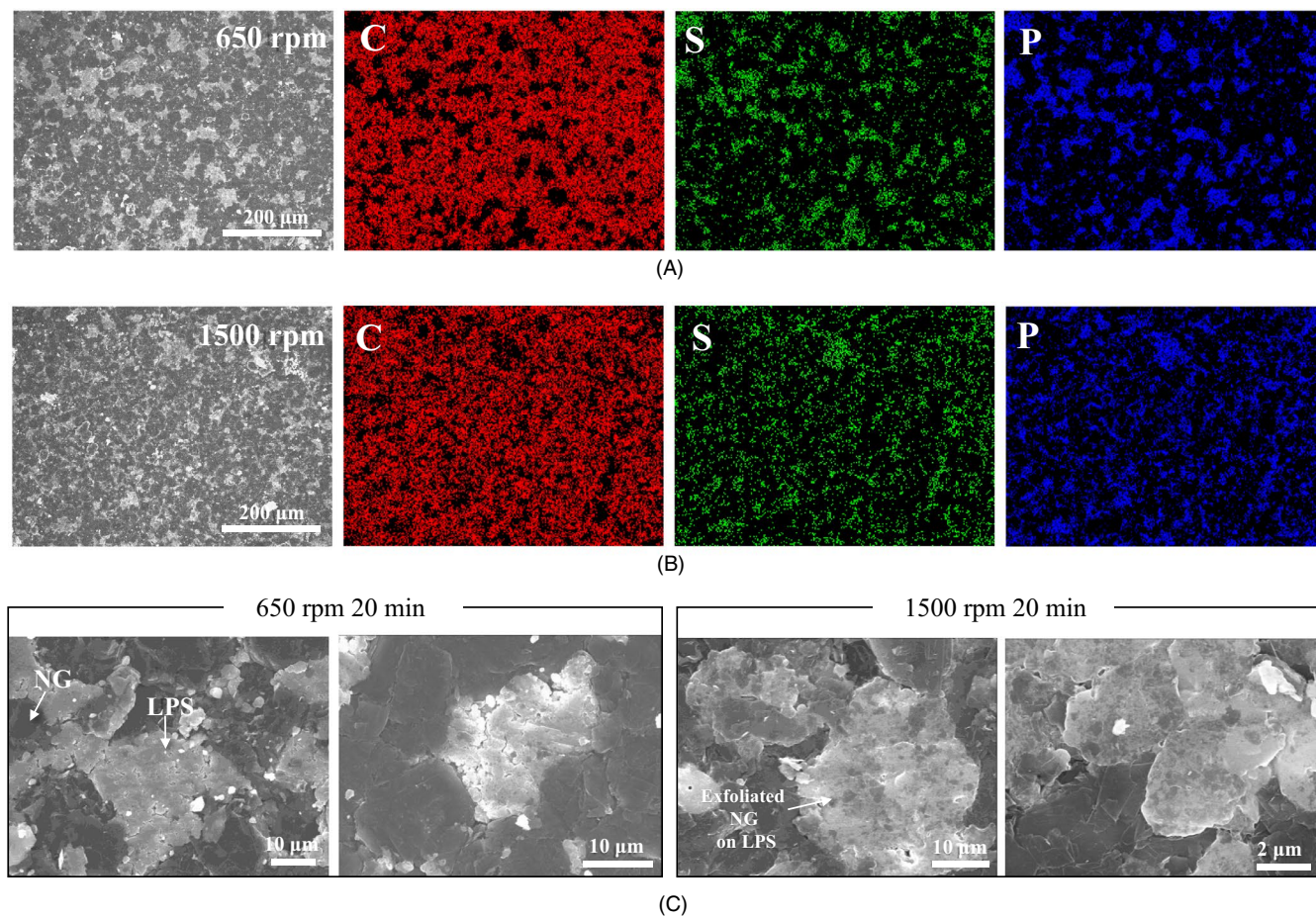


FIGURE 2 SEM and EDS images of composite electrodes mixed at (A) 650 rpm and (B) 1500 rpm and (C) higher resolution views of each electrode

the ion transport resistance within the composite electrodes (Figure 1C). The resistance of the composite electrodes mixed at 300, 650, and 1000 rpm was $\sim 260 \Omega$, whereas that of the electrode mixed at 1500 rpm was $\sim 1030 \Omega$, and a gradual increase in resistance was confirmed as the mixing speed increased above 1000 rpm.

To confirm the relationship between the ionic transport resistance and the cell performance, composite half-cells with a theoretical capacity of 3.38 mAh/cm^2 (loading level of 15.2 mg/cm^2) were fabricated and evaluated at rates of 0.1C and 0.3C for five cycles. The results showed that the three composite electrodes with similar resistances exhibited a similar discharge capacity of $\sim 3 \text{ mAh/cm}^2$ at a charge/discharge rate of 0.1C, but the capacity of the composite mixed at 1500 rpm was $\sim 2.56 \text{ mAh/cm}^2$, and the discharge capacity was significantly degraded. Furthermore, at an increased charge/discharge rate, the composite electrode mixed at 1500 rpm exhibited a capacity of $\sim 1 \text{ mAh/cm}^2$, whereas the others had discharge capacities of over 2 mAh/cm^2 . This significant capacity degradation is strongly related to the large resistance measured in Figure 1B and 1C. The large IR drop in the electrolyte may make it difficult to fully charge the active materials.

SEM analysis with EDS was performed to investigate the morphological changes in each composite electrode depending on the mixing conditions (Figure 2). We found no remarkable difference among the samples with similar capacities. However, the composite electrode mixed at 1500 rpm had a distinctively different morphology. The strong mixing process resulted in more uniform dispersion of NG and LPS particles in the composite electrode mixed at 1500 rpm than in the other samples (Figure 2A and 2B). The components of the composite electrode mixed at 650 rpm were dispersed to some degree, but localized NG and LPS regions also appeared. Therefore, simply considering the distributions of NG and LPS particles, the composite electrode mixed at a higher rotation speed seemed to be desirable for effective ionic conduction to the active material throughout the composite electrode. However, a high-resolution image revealed that many small particles decorated the surface of the LPS particles (Figure 2C), and we inferred that NG was exfoliated by ball milling at a high rotation speed, and fragments of NG became attached to the surfaces of the LPS particles (Figure S1) [23]. We speculated that eventually these fragments prevented facile ion transport among LPS particles by blocking the ionic pathway or increasing its tortuosity, which is highly

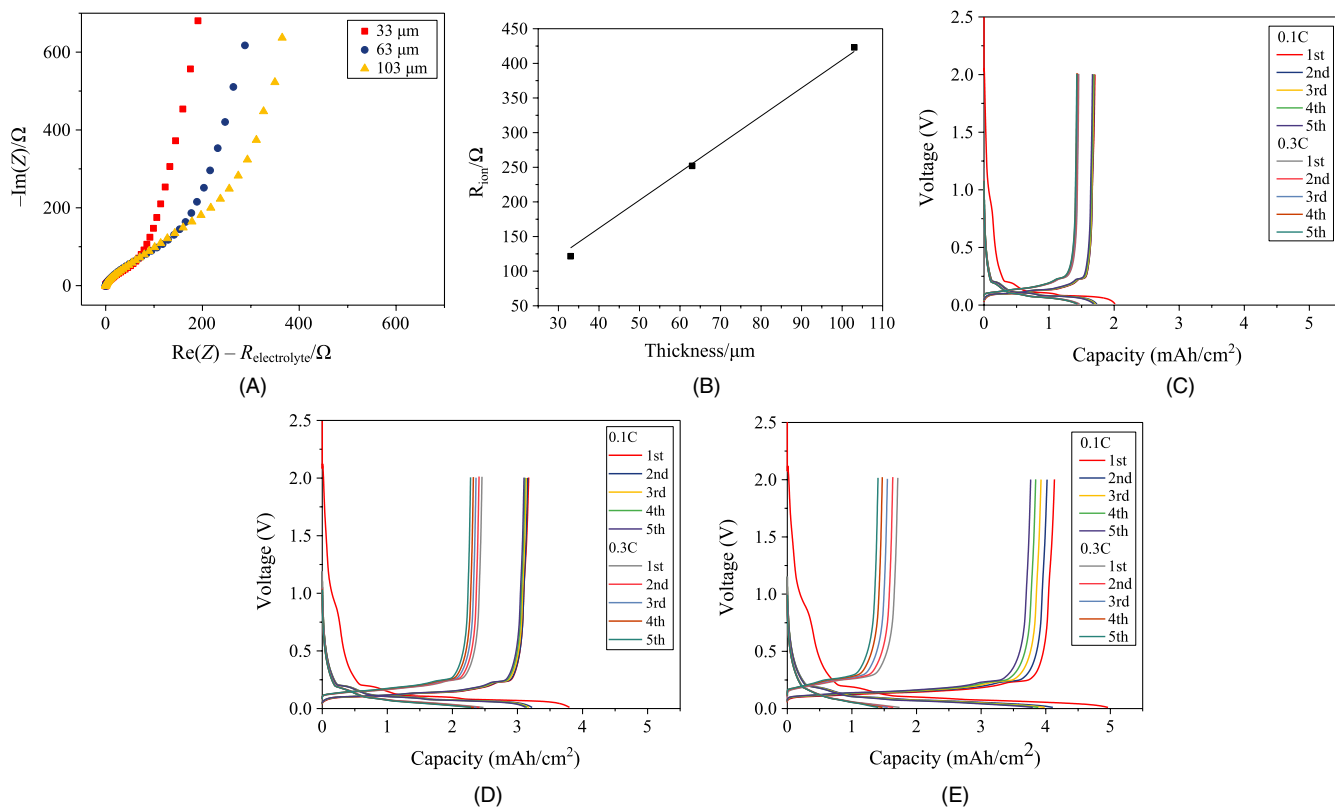


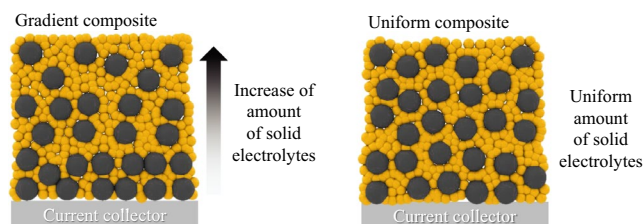
FIGURE 3 (A) Impedance results of composite electrodes of various thicknesses, (B) measured resistance versus composite thickness, and (C–E) charge/discharge profiles of composite electrodes

consistent with the high resistance measured in the symmetric cell (Figure 1B and 1C). In addition, this phenomenon may be related to the low Coulombic efficiency (62.28%) of the composite electrode mixed at 1500 rpm, which is attributed to the formation of a larger solid–electrolyte interphase owing to the increase in surface area due to exfoliation of NG (Figure 1G) [24]. Note that mild preparation of the composite electrode is essential [25,26].

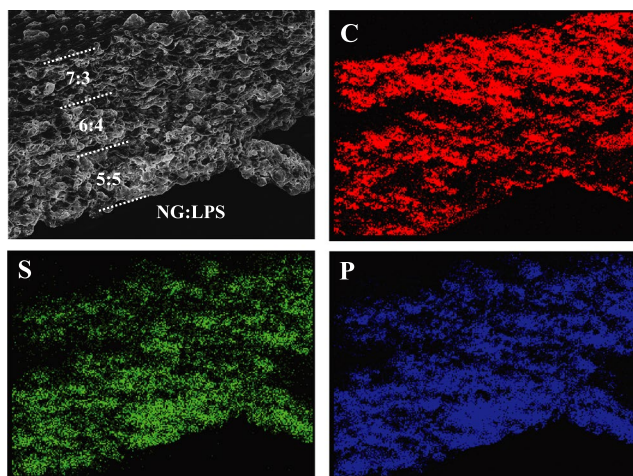
All-solid-state batteries with high-energy-density generally require a thick composite electrode, but increasing the thickness of the electrode is likely to decrease the power performance owing to retardation of ion transport within thick electrodes [27]. To optimize the trade-off between the energy density and power density, we tested the performance of cells with different electrode thicknesses (~ 33 , ~ 63 , and ~ 103 μm) or areal capacities (1.69, 3.38, and 5.07 mAh/cm^2) (Figure 3). The impedance results of the symmetric cells confirmed that the composite electrode thickness is proportional to the ion transport resistance (Figure 3A and 3B). From a plot of these resistance values as a function of composite electrode thickness, we obtained the apparent ionic resistivity of the composite electrode with NG (60 wt%) and LPS (40 wt%) as $\sim 5.35 \times 10^2$ Ωm (ionic conductivity: $\sim 1.86 \times 10^{-5}$ S/cm) (Figure 3B). The measured discharge capacities of the cells at 0.1C were ~ 1.68 , ~ 3.13 , and ~ 3.94 mAh/cm^2 , which corresponded to 99.4%, 92.6%, and 77.8% of their theoretical

capacities, respectively (Figure 3C). Notably, the increase in thickness clearly decreased the ratio of the measured capacities to the theoretical capacities, which suggested that increasing the resistance significantly impeded lithium-ion conduction to the active material, especially near the current collector (Figure 3B). This trend became more significant at a higher charge/discharge rate; the measured capacities and their ratios at 0.3C were ~ 1.44 , ~ 2.35 , and ~ 1.55 mAh/cm^2 and 85.2%, 69.7%, and 30.6%, respectively. Interestingly, the capacity of the cell with an electrode thickness of ~ 103 μm (~ 1.55 mAh/cm^2) was lower than that of the cell with an electrode thickness of ~ 63 μm (~ 2.35 mAh/cm^2) at 0.3C despite the large amount of active material, which indicates that good conduction within thick composite electrodes is particularly important for higher electrochemical performance [20].

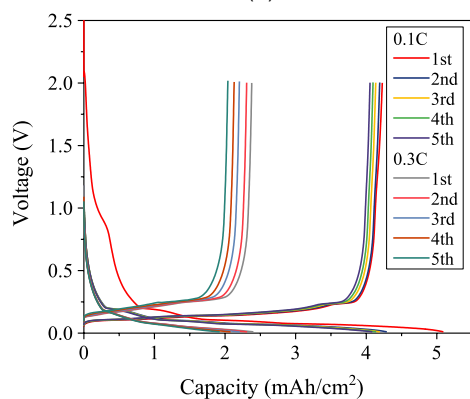
To enhance the power density of all-solid-state batteries while maintaining high-energy-density, we demonstrate a precise composite design using a concentration gradient in the solid electrolyte (Figure 4). As the ionic conductance is proportional to the volume of the solid electrolyte, lithium ions can easily access all parts of the active material in the concentration-gradient composite electrode configuration, where the solid electrolyte concentration in the composite electrode increases toward the middle solid electrolyte layer (Figure 4A). The concentration-gradient composite electrode can be simply fabricated by sequential deposition of composite



(A)



(B)



(C)

FIGURE 4 (A) Schematic illustrations of concentration-gradient and uniform composite electrodes and (B) SEM and EDS images and (C) charge/discharge profiles of the concentration-gradient electrode

powders with different ratios of NG and LPS. To confirm that a concentration gradient formed in the composite electrode, a tilted SEM observation with EDS was performed for a three-layered composite electrode (NG:LPS = 7:3, 6:4, and 5:5) and a uniform composite electrode. (For clear visualization, the thickness of the concentration-gradient composite electrode was increased.) As shown in Figure 4B, the upper region (NG:LPS = 7:3) had a higher C content than the lower region (NG:LPS = 5:5), and S and P exhibited the opposite trend. By contrast, C, S, and P were distributed uniformly in the uniform composite electrode (Figure S2). Note that the fabrication process can be further improved to form a continuous concentration gradient of a solid electrolyte and active materials.

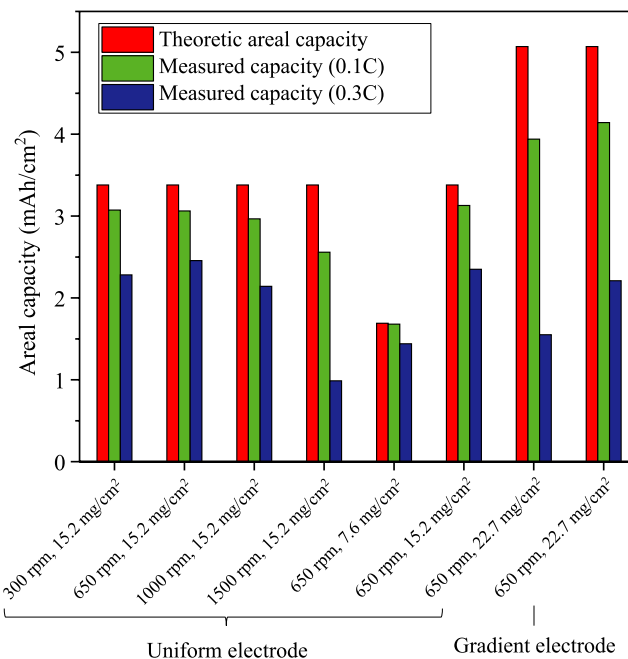


FIGURE 5 Capacities of the measured cells in this study

To obtain all-solid-state batteries with reasonable performance, we used concentration-gradient composite electrodes with a three-layered structure (NG:LPS = 7:3, 6:4, and 5:5) to fabricate a half-cell with a theoretical areal capacity of 5.07 mAh/cm². Before the half-cell test, we analyzed the impedance of the symmetric cells (Figure S3). This analysis revealed that the concentration-gradient composite electrode exhibited better impedance than the uniform composite electrode, but further detailed analysis must be conducted in future studies. The results of the half-cell test showed that the concentration-gradient electrode had a higher power density than the uniform composite electrode (Figures 3E and 4C). The capacities of the uniform and concentration-gradient electrodes at a charge/discharge rate of 0.1C were similar (~3.94 and ~4.142 mAh/cm², respectively), but at a charge/discharge rate of 0.3C, the capacity of the concentration-gradient composite was 2.21 mAh/cm², which was 42.6% higher than that of the uniform composite electrode. This result indicated that a simple change in the design of the composite electrodes can enhance the electrochemical performance even when identical components are used. Figure 5 summarizes the measured capacities of all the cells in this work for convenient comparison, and we again confirm that the concentration-gradient electrode can exhibit a reasonable energy density and power density. Further, to obtain a full cell with superior performance, it is necessary to optimize the middle solid electrolyte layer and composite cathodes, and we believe that a similar approach to tuning the composition of a solid electrolyte can be applied to composite cathodes as well.

4 | CONCLUSIONS

In summary, we presented a systematic study of composite electrodes consisting of an active material and a solid electrolyte in all-solid-state batteries. The ion transport properties were evaluated and compared using the TLM model of composite symmetric cells under various experimental conditions. It was confirmed that a strong mixing process can enhance the dispersity of the active material and solid electrolyte; however, fragmentation of active materials induced by severe ball milling can significantly impede ionic transport. Therefore, careful optimization is crucial to obtaining composite electrodes with desirable properties. Furthermore, to realize all-solid-state batteries with both high-energy-density and high-power-density, we investigated the cell performance using composite electrodes with various thicknesses and presented a concentration-gradient composite electrode. Our study confirmed that the electrochemical properties of the concentration-gradient composite electrode were better than those of a uniform composite electrode and provided a meaningful approach to enhancing cell performance by composite electrode design.

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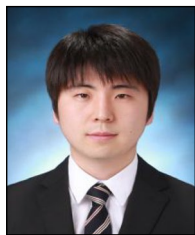
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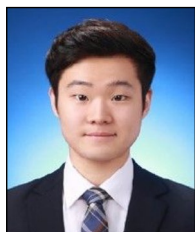
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