## Photocatalytic removal of NO<sub>x</sub> using TiO<sub>2</sub>-coated zeolite

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#### **ABSTRACT**

Application of photocatalytic nanoparticles has been recently gaining an increased attention as air purifying material for sustainable urban development. The present work reports the photocatalytic removal of gaseous phase nitrogen oxides (NOx) using TiO2-coated zeolite to be applied as a filter media for the urban green infrastructure such as raingardens. The TiO<sub>2</sub>-coated zeolite was synthesized by simple wet chemistry method and tested in a continuous-flow photo-reactor for its removal efficiency of NO<sub>x</sub> under different conditions of the weight percentage of TiO<sub>2</sub> coated on the zeolite, and gas retention time. The removal efficiency of NOx in general increased as the weight percentage of TiO2 coated on the zeolite increased up to 15-20%. Greater than 90% of NO<sub>x</sub> was removed at a retention time of one minute using the TiO<sub>2</sub>-coated zeolite (TiO<sub>2</sub> weight percentage = 20%). Overall, TiO<sub>2</sub>-coated zeolite showed greater efficiency of NO<sub>x</sub> removal compared to TiO<sub>2</sub> powder probably by providing additional reaction sites from the porous structure of zeolite. It was presumed that the degradation of NOx is attributed to both the physical adsorption and photocatalytic oxidation that could simultaneously occur at the catalyst surface.

Keywords: Nanoparticles, NO<sub>x</sub>, Photocatalysis, TiO<sub>2</sub>, Zeolite

#### 1. Introduction

Nitrogen monoxide (NO) and dioxide (NO<sub>2</sub>), which are collectively called nitrogen oxides(NO<sub>x</sub>) are harmful and poisonous gases that are emitted mainly from anthropogenic sources such as industrial power plants and automobile engines [1-2]. Air pollution caused by photochemical oxidants, such as ozone and NOx, is one of the serious problems faced by urban areas [3]. The annual mean concentrations of NO<sub>x</sub> in urban areas globally are in the range of 20-90 ppb but hourly averages can often exceed 1000 ppb on heavy vehicular traffic conditions [4]. NO<sub>x</sub> has significant impacts on the environment, human and animal health, and plant vegetation. Adverse effects of NO<sub>x</sub> include acid rain, photochemical smog, ozone layer depletion, greenhouse effect, and ecological toxification [5]. Furthermore, NO<sub>x</sub> has been also a recurring problem of worsening indoor air quality (IAQ) in most building structures, and diseases related to lower IAQ have been reported [6]. Recent study done by Shakerkhatibi, et al. (2015) [7] showed that gaseous air pollutants of NO2, NO, and CO were associated with the hospital admissions for chronic obstructive pulmonary disease.

The needs for mitigating the negative effects of NO<sub>x</sub> have increased over the past few decades. Photocatalytic oxidation (PCO) has been suggested as an efficient and cost effective approach to control airborne pollutants such as NO<sub>x</sub> [8]. PCO relies on photo-

catalysts which utilize ultraviolet (UV) light radiation from sunlight or artificial light assisting in oxidizing various pollutants [9]. Among the photocatalysts used in PCO processes, titanium dioxide (TiO<sub>2</sub>) has been most widely used because of its chemical stability, non-toxicity, and relatively low cost [10-11]. In addition, TiO2 nanoparticles are able to provide more active sites than standard TiO2 powder [12], making the degradation of pollutants more effective. Upon irradiation of UV light, TiO2 generates electrons and holes in the conduction and valence bands, respectively which could participate in the oxidation-reduction (redox) reactions for pollutant degradation [13-15]. The proposed mechanism of NO<sub>x</sub> photocatalytic oxidation consist of three stages: NO initially reacts with the OH- radical formed from the TiO2 surface reaction of H<sub>2</sub>O and oxygen, resulting in HNO<sub>2</sub> (first stage) before subsequently becoming HNO<sub>3</sub> (second stage) that would be desorbed at the TiO<sub>2</sub> surface, and thus regenerating the catalyst (third stage). The mechanisms were described in more detail by various researchers [16-18].

Since the first discovery of super-hydrophilicity of TiO<sub>2</sub> by Fujishima, et al. (2000) [19],  $TiO_2$  has been applied to building materials with the aim of air cleaning, self-cleaning, and anti-fogging functions [20-23]. Recent applications of TiO2 has been widen to the outdoor building materials such as pavements and concrete surfaces to control urban airborne pollutants such as NO<sub>x</sub> [18, 23-28]. The present study is a preliminary study to eventually propose the application of photocatalytic nanoparticles to the surface media layer (i.e. zeolite) of urban green infrastructure practices such as



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Received January 28, 2016 Accepted April 27, 2016

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Tel: 82-2-2260-3776 Fax: 82-2-2266-8753 rain gardens, providing multiple functions of controlling air and water quality in urban settling. Rain garden, or also called as bio-retention area, is one of the urban stormwater management practices recommended by the United States' Environmental Protection Agency (US EPA) since 2000 [29]. Rain gardens are low depressions in the landscape that are planted with trees and/or shrubs, and covered with a bark mulch layer or ground cover allowing for the infiltration of storm water to recharge aquifers, and reduce surface runoffs. Various designs have been developed for rain garden systems [30] but researches on the use of nanoparticles on stormwater management practices are limited in number [24-26, 31-32].

The scope of the present research is directed on identifying the effectiveness of applying  $TiO_2$  nanoparticles on natural zeolites, which will be added within the rain garden system, for adding function of  $NO_x$  removal from the urban atmosphere. The photocatalytic removal of  $NO_x$  in air was investigated thru a lab-scale continuous flow reactor with  $TiO_2$  coated onto natural zeolite as a preliminary study for its applicability to actual rain garden systems.

### 2. Materials and Methods

#### 2.1. Synthesis of the Nanoparticle-coated Zeolite

Natural zeolite (DAEJUNG Chemicals, Korea) with a mean diameter of 3 mm was calcined at 600°C for 2 h to remove any organic impurities present, and subsequently cooled at room temperature. Then, the prepared zeolite was added to a flask with an aqueous suspension of TiO<sub>2</sub> (DAEJUNG Chemicals, Korea) nanoparticles (mean diameter was 300 nm), and was shaken at 150 rpm for 2 h to ensure homogenous coating of the TiO2 nanoparticles on the zeolite surface. Finally the mixed solution was oven dried at 105oC for 24 h followed by calcination at 600oC for 2 h, producing the TiO<sub>2</sub>-coated zeolite. Scanning electron microscope (SEM; JEOL-7800F, JEOL, Japan) with Energy Dispersive X-ray Spectrometer (EDS) and X-ray diffractometer (XRD; Ultima IV, Rigaku, Japan) were conducted to characterize the morphology, composition, and crystallinity of the TiO<sub>2</sub>-coated zeolite. Surface area measurements were carried out using the BET analysis method (Autosorb-iQ 2ST/MP, Quantachrome, U.S.A.).

#### 2.2. Photocatalytic NO<sub>x</sub> Degradation Experiments

A continuous-flow photo-reactor was used to measure the performance of the TiO $_2$ -coated zeolite in removing NO $_x$  in the air. Fig. 1 shows the laboratory setup consisting of NO $_x$  source (5 ppm NO in N $_2$ , DONG-AH Gas, Korea), purified air source (< 1% hydrocarbon impurities, DONG-AH Gas, Korea), flow controllers (DWYER, USA), box-type photo-reactor (made of acryl), UV-A lamp (20 W, SANKYO DENKI, Japan) and a chemiluminiscent NO $_x$  analyzer (ECOTECH, SERINUS 40, Australia). Either of the two photo-reactors with different dimensions (Reactor 1: L = 310 mm, W = 110 mm, H = 55, Reactor 2: L = 600 mm; W = 220 mm; H = 100 mm) was used when appropriate for the convenience of adjusting the gas retention time of the reactor to a required value during the test. A total of 6 UV-A lamps (20 W each with light intensity of 0.38 mW/cm $^2$ ) were simultaneously used to provide sufficient light energy for the photocatalytic reaction.

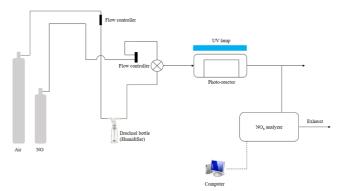


Fig. 1. Schematic of the laboratory setup for the  $NO_x$  removal experiment.

An appropriate amount of the TiO<sub>2</sub>-coated zeolite was loaded into the reactor and then the reactor was carefully sealed. Afterwards, the NO containing nitrogen gas and the purified air were allowed to flow into the reactor at flow rates of 0.2 L/min and 2 L/min, respectively, until equilibrium NO<sub>x</sub> concentration in the inflow has achieved. The purified air was passed through a humidifier before being mixed with NO containing nitrogen gas in order to achieve a required level of relative humidity (40-60%) in the reactor. The gas flow was continued for 30 minutes before the light source was turned on. Afterwards, the TiO2-coated zeolite was irradiated for 60 minutes during which the NO<sub>x</sub> concentration of the outflow gas was recorded at 1 min intervals by the  $NO_x$ analyzer. After the one hour of irradiation, the light source was turned off and then the gas valves were closed. All experiments were conducted at ambient temperature (18-20°C). The detailed experimental procedure can be referred to published literatures [25-27, 31-32] and the ISO 22197-1:2007 standard for air purification performance of semiconducting photocalytic materials [33].

### 3. Results and Discussion

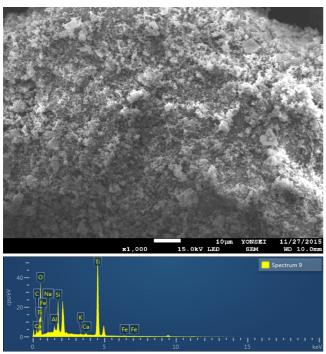
### 3.1. Characterization of the Synthesized Coated Zeolite

The scanning electron microscope (SEM) and energy dispersive X-ray spectrometer (EDS) images of the TiO<sub>2</sub>-coated zeolite were presented in Fig. 2. The TiO<sub>2</sub> nanoparticles are fairly distributed on the zeolite surface but particle agglomerations were often observed on the zeolite surface probably due to the sintering of TiO<sub>2</sub> particles at high temperature calcination [33, 36]. However, it should be mentioned that the controlled distribution of guest particles (TiO<sub>2</sub>) with minimal particle agglomeration on the host particle surface (zeolite) is still an active research in the nanotechnology field [8, 12-13, 18-19]. The EDS scan confirmed that TiO<sub>2</sub> particles were present on the zeolite surface based on the detected elements. The major peak of Ti at ~4.5 keV seen on the EDS spectrum represents the binding energy for the Ti4+ oxidation present in most TiO2 phases (such as anatase, rutile, and brookite). The crystal structure of the synthesized coated zeolite was examined using XRD. The diffraction peaks matched with that of tetragonal anatase  $TiO_2$  (a = 3.7892 Å, c = 9.5370 Å; Crystallography Open Database, No. 5000223) indicating that TiO<sub>2</sub> was successfully loaded on the zeolite surface as shown in Fig. 3.

The BET surface listed in Table 1 exhibits a decrease in surface area when  ${\rm TiO_2}$  was coated in zeolite. This could be due to the decrease of zeolite mesopore sites where N2 gas was adsorbed, which is also an indication of a successful coating of the zeolite surface with the  ${\rm TiO_2}$  nanoparticles. However, the decreased in BET surface area (i.e., mesopores) had negligible effects to the pollutant removal efficiency of the coated zeolite.

Table 1. BET Surface Area of the Tio2 Coated Zeolite and Bare Zeolite

Catalyst	BET Surface Area, m <sup>2</sup> /g
TiO <sub>2</sub> coated zeolite	80.593
Zeolite only	208.782



**Fig. 2.** Scanning electron microscope (SEM) and the energy dispersive X-ray spectrometer images for the TiO<sub>2</sub> coated zeolite.

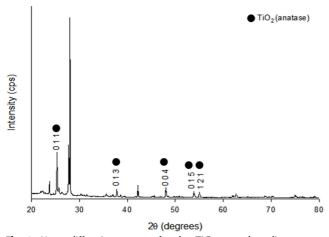


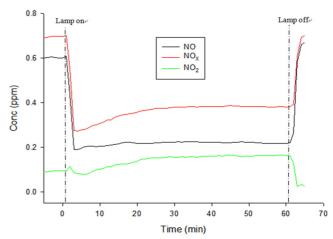
Fig. 3. X-ray diffraction pattern for the TiO<sub>2</sub>-coated zeolite.

# 3.2. Effect of $TiO_2$ Particles in the Photocatalytic $NO_x$ Degradation

Preliminary experiments were performed using  $TiO_2$  particles only as shown in Fig. 4. After the UV lamp was turned on, an immediate decrease in the NO and  $NO_x$  concentration was observed. NO concentration remained constant throughout the irradiation period of one hour while  $NO_x$  (NO +  $NO_2$ ) concentration gradually increased due to the increased concentration of  $NO_2$  created from the oxidation of NO. The  $NO_x$  removal efficiency (R.E.) was calculated using Eq. (1).

$$\%RE = \frac{(C_o - C_{Ave})}{C_o} \times 100\%$$
 (1)

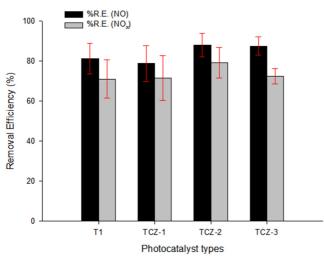
where  $C_{\rm ave}$  is the average concentration of  $NO_x$  in the outflow during the one hour of irradiation, and  $C_0$  is the  $NO_x$  concentration of the inflow. Before the light source was turned on, no significant change in the pollutant gas was observed, indicating that the chemical transformation of  $NO_x$  can be attributed to the photocatalytic mechanism [10, 13-14]. The calculated  $NO_x$  and NO removal efficiencies based on the concentration profile from Fig. 4 were 48% and 64%, respectively, which are similar to most of the previously reported values in the literature [18, 20, 26-28, 31-32]. When the light source was turned off after the one hour of irradiation,  $NO_x$  concentration immediately returned to its initial value, indicating no permanent physical adsorption of  $NO_x$  on the photocatalyst particles.



**Fig. 4.** Example of the  $NO_x$  concentration profile with respect to time during photocatalytic experiments.

#### 3.3. Role of Zeolite in the Photocatalytic Degradation

The removal efficiency generally improved when  $TiO_2$  was coated onto natural zeolite as shown in Fig. 5. The improved efficiency can be due to the capability of zeolite to act as adsorbent for the nitrate  $(NO_3^-)$  evolved from the photocatalytic oxidation of  $NO_x$ . Zeolite can also provide for increased active sites for NO gas to react with  $TiO_2$  because of its porous structure [35, 36]. That is zeolite can assist  $TiO_2$  nanoparticles in capturing the target pollutants for the subsequent photocatalytic reactions [37-39].



**Fig. 5.** Comparison of the  $NO_x$  degradation performance between  $TiO_2$  nanoparticles and  $TiO_2$  coated zeolite. Notes:  $T1 = TiO_2$  powders under UV-A irradiation;  $TCZ-1 = TiO_2$  (10 wt.%) coated zeolite;  $TCZ-2 = TiO_2$  (15 wt.%) coated zeolite;  $TCZ-3 = TiO_2$  (20 wt.%) coated zeolite. Error bars indicate standard deviations of four replicate experiments.

A control test was performed; the uncoated natural zeolite was placed inside the photo-reactor and subjected to the same irradiation procedure, and no significant change was observed in the  $NO_x$  concentration, indicating that there is a synergistic effect with the addition of  $TiO_2$  for the efficient removal of  $NO_x$ .

### 3.4. Effect of Varying TiO2 Mass Loadings in Zeolite Media

Three  $TiO_2$ -coated zeolite with different  $TiO_2$  weight percentages (i.e. 10 wt.%, 15 wt.%, and 20 wt.%) were compared in terms of the  $NO_x$  removal efficiency. Overall, as the weight percentage of  $TiO_2$  with respect to zeolite increased, the removal efficiency also increased, which might be due to the increased active sites for photocatalytic reactions in the media. However, variances were observed in the removal efficiency among different replicate samples of the coated zeolite, which could be due the uneven distribution of the  $TiO_2$  particles over the zeolite aggregates during the coating process. The variation in  $NO_x$  removal efficiency among different replicate samples decreased as the mass percentages of  $TiO_2$  increased due probably to the increased probability of the  $TiO_2$  particles to be well distributed over the zeolite aggregates. Therefore, the  $TiO_2$ -coated zeolite with 20 wt.%  $TiO_2$  was used for the subsequent photocatalytic experiments.

# 3.5. Effect of Gas Retention Time in the Photocatalytic Degradation

Fig. 6 shows the removal efficiencies of  $NO_x$  using the coated  $TiO_2$ -zeolite at different gas retention times. The removal efficiency increased as the gas retention time increased. Lower retention time values have lesser time for the pollutant gas to come into contact with the  $TiO_2$  catalyst and thereby reducing its efficiency. Greater than 90% of  $NO_x$  was removed at a retention time of one minute using the  $TiO_2$ -coated zeolite ( $TiO_2$  weight percentage = 20%).

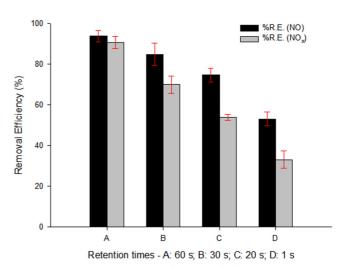


Fig. 6. Effect of retention time on the removal efficiency for (20 wt.%)  $TiO_2$  coated zeolite. Error bars indicate standard deviations of four replicate experiments

#### 4. Conclusions

The effectiveness of coating TiO2 particles into natural zeolite has been demonstrated in this study. Generally, the removal efficiency of NO<sub>x</sub> increased as the weight percentage of TiO<sub>2</sub> coated on the zeolite but variances in the  $NO_x$  removal were observed among different replicate samples of the coated zeolite, which could be due to the uneven TiO2 distribution on the zeolite aggregates during the coating process. Overall, TiO2-coated zeolite showed greater efficiency compared to TiO2 powder probably because zeolite can provide additional reaction sites from its porous structure. The degradation of NO<sub>x</sub> have been attributed to both the physical adsorption and photocatalytic mechanisms simultaneously happening on the catalyst surface. A proportional relationship was also seen between the removal efficiency and retention time as well. Sufficient contact time with the particles would be required to ensure adsorption and degradation of the pollutant. More than 90% of NO<sub>x</sub> was removed at a retention time of one minute using the TiO<sub>2</sub>-coated zeolite (with TiO<sub>2</sub> weight percentage at 20%).

## **Acknowledgments**

This research was supported by a grant (14CTAP-C086804-01) from the Technology Advancement Research Program funded by the Ministry of Land, Infrastructure and Transport of the Korean government.

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