

Occurrence and removals of micropollutants in water environment

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ABSTRACT

Micropollutants are often discharged to surface waters through untreated wastewater from sewage treatment plants and wastewater treatment plants. The presence of micropollutants in surface waters is a serious concern because surface water is usually provided to water treatment plants (WTP) to produce drinking water. Many micropollutants can withstand conventional WTP systems and stay in tap water. In particular, pharmaceuticals and endocrine disruptors are examples of micropollutants that are detected at the drinking water, ppb, or even ppb level. A variety of techniques and processes, especially advanced oxidation processes, have been applied to remove micropollutants from water to control drinking water contamination. This paper reviews recent researches on the occurrence and removal of micropollutants in the aquatic environments and during water treatment processes.

Keywords: Adsorption, Advanced oxidation processes (AOPs), Coagulation, Endocrine-disrupting chemicals (EDCs), Pharmaceuticals

1. Introduction

Micropollutants are compounds that are detected in the environment at trace concentrations ranging from μ g/L to below ng/L [1]. Micropollutants can be composed of various materials and can contain various compounds such as pesticides, pharmaceuticals, cosmetics, flame retardants, perfumes, waterproofing agents, plasticizers and insulating foams [2]. Pharmaceuticals and personal hygiene products (PPCPs) and endocrine disrupting chemicals (EDCs) are among the most frequently detected anthropogenic contaminants in water.

Micropollutants are ubiquitous, and are often used to improve human life. This makes it difficult to control the source of these compounds in the water environment. Many researches on monitoring contamination by pharmaceuticals and EDCs in a variety of environments, such as surface water, groundwater, drinking water and wastewater, have reported significant levels of micropollutants in the water environment [3-9].

Because conventional processes used in wastewater treatment plants (WWTPs) are not designed to remove micropollutants, these can persist in the treated wastewater effluent. As a result, many of these micropollutants can be present in aquatic environments, including surface waters, and surface waters are a threat to the ecosystem and human health. The occurrence of micropollutants in the aquatic environment is associated with a variety of negative effects including short- and long-term toxicity, EDC and antibiotic resistance in microorganisms [10-12].

To date, regulations have been adopted for small amounts of micro-contaminants in some countries and regions, but WWTPs are not subject to consistent emission guidelines and standards for micropollutants. For example, environmental quality standards for a small number of micropollutants (e.g., nonylphenol, bisphenol-A and diiron) have been regulated by the European Parliament through Directive 2008/105/EC [13]. Nonylphenol and nonylphenol ethoxylates are recognized by the Canadian government as a toxic substance [14]. Other micropollutants, such as pharmaceutical and personal care products (PPCPs) and steroid hormones, are not yet on the list of regulated substances. Further studies on the effects of these micropollutants on human health and ecological health are needed to establish regulatory standards for micropollutants.

Although several review papers have been published regarding the occurrence of micropollutants in different water bodies [15-17], still not enough work has been done to provide a comprehensive summary of the occurrence of micropollutants in aquatic systems or the removal of micropollutants in conventional and advanced water treatment processes. In this review, we summarize recent work on the occurrence and removal of various micropollutants via conventional, as well as advanced, water



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Received September 21, 2016 Accepted November 28, 2016

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treatment processes.

2. Sources and Transport of Micropollutants in the Environment

Micropollutants present in the water environment have diverse origins in which domestic wastewater is a major source of surface water (Fig. 1). Pharmaceuticals are frequently detected in aquatic environments, originating from hospitals, drug stores, and convenience stores; some of these drugs are available without prescription (e.g., acetaminophen, ibuprofen, naproxen and aspirin). Although these pharmaceuticals are produced for human and animal health-care, they are not metabolized completely in the body [18]. Both residual pharmaceuticals and their metabolites are excreted by humans and animals into wastewater. Waste from the manufacture process and from expired drugs can also be sources of pharmaceuticals.

EDCs such as natural hormones, insecticides, nonylphenol, bisphenol-A, and perfluorooctanesulfonic acids (PFOS) are also important micropollutants. These compounds are released into water from raw materials such as plastic products and flame retardants. They can also be generated directly by humans and animals [19, 20]. These hormone-like activities of EDC compounds have been shown to adversely affect human health [21, 22]. EDCs in human body are excreted in sewage and discharged into aquatic systems such as rivers and lakes. For this reason, sewage effluent is considered a major source of micropollutant contamination.

Physicochemical properties and bioavailability can affect the presence of micropollutants in natural waters. Caliman and Gavrilescu [23] categorized the generation and elimination of micropollutants based on five factors; physicochemical properties, environmental factors, transport and retention, transformation and accumulation. The volatility, water solubility, stability of the chemical structure, and particulate distribution characteristics are additional factors that determine whether micropollutants remain dissolved in water.

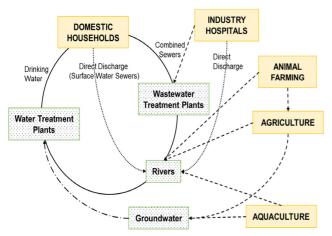


Fig. 1. Sources and pathways of PPCPs in the urban water cycle [22].

The physical properties of micropollutant can affect the movement of contaminants from one stage to another (e.g., soil-water movement). The mobility of the compounds is determined by transport/retention factors which are dependent on chemical related properties such as acid dissociation constant (pKa) and octanol-water partition coefficient (Kow). Adsorption, precipitation, complex formation and colloid formation all contribute to the retention of micropollutants in water. Transport mechanisms include advection, dispersion, diffusion and active transport.

Physical property of micropollutant can affect the movement of pollutants from one phase to another (e.g., soil-water transfer). The mobility of the compounds is determined by transportation/retention factors, which depend on chemical-related properties such as the logarithmic acid dissociation constant (pKa) and the octanol-water partitioning coefficient (Kow). Sorption, precipitation, complexation, and colloid formation all contribute to the retention of micropollutants in water. Mechanisms of transport include advection, dispersion, diffusion, and active transport.

Transformation processes, that is, the decomposition of the parent compound as a byproduct, does not completely prevent the micropollutants from reaching the natural environment. Unless appropriate conversion processes are applied in the wastewater treatment process, it is difficult to control the amount of miropollutants to be emitted and accumulation may occur in the aquatic environment.

3. Occurrence of Micropollutants in Water

The presence of micropollutants in surface water has recently been widely reported. WWTPs can discharge wastewater effluent containing untreated micropollutants directly into rivers, lakes, rivers and reservoirs. Emitted micropollutants can be naturally deposited on sediments or transported to other places due to hydrological impact. These compounds can also be simultaneously converted to by-products by chemical and biological degradation at surface water [24]. However, at least some micro-contaminants are likely to persist and accumulate in surface waters [25].

Table 1 shows the concentrations of micropollutants in surface water, ground water, sewage treatment plant (STP) influents or effluents, WWTP influents or effluents, and hospital effluents. These results indicate that micropollutants have been ubiquitous pollutants in water environment.

In most countries, surface water is the source of drinking water in an area of increasing urban population in general. Therefore, micropollutants in surface waters can enter WTPs, and their presence in drinking water has been reported by several researchers. For example, clofibric acid has been reported at high concentrations (> 165 ng/L) in tap water in Berlin [61]. People can be unconsciously exposed to these micropollutants through tap water used for drinking, cooking and bathing. Therefore, removal of micropollutant by WTP is important for drinking water production. However, the presence of micropollutant present in tap water means that existing water treatment systems can not completely remove micro-contaminants from WTP.

Table 1. Distributions of the Micropollutants in Various Water Matrixes

| Compounds | Water sample | Country | Concentration (ng/L) | References |
|---------------|-------------------|----------------|----------------------|------------|
| acetaminophen | surface water | Serbia | 78,170 | [26] |
| | surface water | Korea | 5-127 | [27] |
| | surface water | Korea | 4.1-7.3 | [6] |
| | ground water | USA | 380 | [28] |
| | STP influent | Korea | 13,406-56,944 | [27] |
| | STP influent | Spain | 24,600-29,000 | [29] |
| | STP effluent | Korea | 5-9 | [27] |
| | STP effluent | Korea | 1.9-19 | [6] |
| | STP effluent | Spain | 32-4,300 | [29] |
| | hospital effluent | Taiwan | 62,250 | [30] |
| caffeine | surface water | Germany | 65-6,798 | [31] |
| | surface water | Denmark | 65-382 | [32] |
| | surface water | China | 339 | [33] |
| | surface water | Korea | 0-373 | [27] |
| | ground water | Europe | 189 | [31] |
| | ground water | USA | 290 | [34] |
| | WWTP influent | Greece | 17,100-113,200 | [35] |
| | WWTP influent | Taiwan | 5,173-17,500 | [30] |
| | WWTP influent | USA | 26,567 | [36] |
| | WWTP effluent | Korea | 3,600 | [37] |
| | WWTP effluent | Korea Korea | 19-873 | [27] |
| | WWTP effluent | Korea | 23-776 | |
| | WWTP effluent | Taiwan | 19-1,727 | [6] |
| | WWTP effluent | usa Usa | 19-1,/2/ | [36] |
| | WWTP effluent | Greece | | [36] |
| | | | 1,900-13,900 | [35] |
| carbamazepine | surface water | Korea | 4.5-61 | [6] |
| | surface water | Korea | < 595 | [38] |
| | surface water | Korea | 5-36 | [27] |
| | surface water | USA | 6.8 | [39] |
| | STP influent | Korea | 5-451 | [27] |
| | STP effluent | Korea | 73-729 | [6] |
| | STP effluent | Sweden | 1,680 | [40] |
| | STP effluent | Japan | 10.8-163 | [41] |
| | hospital effluent | Spain | 30-70 | [29] |
| diclofenac | surface water | Korea | 8.8-127 | [6] |
| | surface water | China | < 147 | [42] |
| | surface water | Sweden | 10-120 | [40] |
| | surface water | UK | 20-91 | [43] |
| | STP influent | UK | 350-460 | [43] |
| | STP effluent | Korea | 8.8-127 | [6] |
| | STP effluent | Sweden | 120 | [40] |
| | STP effluent | Spain | 200-3,600 | [29] |
| | hospital effluent | Taiwan | 328 | [30] |
| ibuprofen | surface water | Korea | 11-38 | [6] |
| = | surface water | Germany | 60-152 | [44] |
| | surface water | Korea | 5-414 | [38] |
| | ground water | USA | 3,110 | [47] |
| | STP influent | Spain | 37-860 | [44] |
| | STP influent | Taiwan | 711-17,933 | [30] |
| | STP effluent | Korea | 10-137 | [6] |
| | STP effluent | Taiwan | 313-3,777 | [30] |

| Compounds | Water sample | Country | Concentration (ng/L) | References |
|------------------|-------------------|-------------|----------------------|------------|
| metoprolol | surface water | Spain | 90 | [12] |
| | surface water | China | 24.8 | [48] |
| | WWTP effluent | Sweden | 274 | [48] |
| naproxen | surface water | Sweden | 90-250 | [40] |
| | surface water | China | < 118 | [42] |
| | surface water | Germany | 70 | [44] |
| | surface water | Korea | 20-483 | [6] |
| | STP influent | Sweden | 3,650 | [40] |
| | STP influent | Spain | 109-455 | [44] |
| | STP influent | Japan | 38-230 | [41] |
| | STP effluent | Sweden | 250 | [40] |
| | STP effluent | Japan | 12-139 | [41] |
| | STP effluent | Belgium | 625 | [44] |
| sulfamethoxazole | surface water | Korea | 1.7-36 | [6] |
| | surface water | Korea | 5-82 | [27] |
| | surface water | USA | 150 | [45] |
| | surface water | USA | < 300 | [46] |
| | ground water | USA | 1,110 | [47] |
| | STP influent | USA | < 1,000 | [46] |
| | STP influent | Korea | 156-984 | [27] |
| | STP effluent | USA | 310 | [46] |
| | STP effluent | Korea | 3.8-407 | [6] |
| | hospital effluent | Taiwan | 1,335 | [30] |
| sulfamethazine | ground water | USA | 360 | [47] |
| | STP influent | Korea | 132 | [49] |
| | STP effluent | Korea | 114 | [49] |
| atrazine | surface water | USA | 4.7-3,600 | [50] |
| | surface water | Korea | 1.8-18 | [51] |
| | ground water | Europe | 8 | [52] |
| | ground water | Switzerland | 1-179 | [53] |
| | STP influent | Switzerland | 52-59 | [53] |
| | WWTP effluent | Spain | 124 | [54] |
| | WWTP effluent | Switzerland | 25-34 | [53] |
| bisphenol-A | surface water | USA | 81 | [50] |
| 1 | surface water | Korea | 4.5-61 | [51] |
| | surface water | Europe | 10 | [50] |
| | surface water | Germany | 28-68 | [31] |
| | surface water | USA | 6,000 | [39] |
| | STP effluent | UK | 19.2 | [55] |
| | WWTP effluent | USA | 281-3,642 | [55] |
| 2,4-D | surface water | China | 5.6-6.2 | [42] |
| -, - <i></i> | ground water | Europe | < 12 | [52] |
| | STP effluent | Spain | 33.4 | [56] |
| | STP effluent | Spain | 21.4 | [56] |
| triclosan | surface water | USA | 9-1,550 | |
| urciosali | surface water | | 9-1,550 4.6-55 | [57] |
| | | USA | | [57] |
| | surface water | USA | 3.3-41 | [57] |
| | surface water | USA | 8.8-75 | [57] |
| | surface water | USA | 10-2,230 | [58] |
| | surface water | USA | 10-600 | [58] |
| | surface water | USA | 0.45-486 | [58] |

| Compounds | Water sample | Country | Concentration (ng/L) | References |
|-------------|---------------|---------|----------------------|------------|
| nonylphenol | surface water | USA | 800 | [45] |
| | surface water | Korea | 23.2-187.6 | [59] |
| | surface water | China | 1,900-32,800 | [60] |
| | STP influent | Japan | 500-1,100 | [41] |
| | STP effluent | Japan | 100-900 | [41] |

STP: Sewage Treatment Plant; WWTP: Waste Water Treatment Plant

Table 2. Human Toxicological Values of Micropollutants in Drinking Water

| Compounds | Toxicological data (taxon, effect) | References | |
|------------------|--|------------|--|
| diclofenac | Maximum oral exposure: 4 μg/d, 36 weeks | [63] | |
| uicioienac | (Pregnant women, Premature closure of the ducts arteriosus or hemodynamic changes | [62] | |
| | Provisional guideline value = 1 μ g/L, 24 mon (Rats, Carcinogenetic) | | |
| carbamazepine | Maximum concentration in drinking water: 0.03 μg/L | [63] | |
| | Benchmark quotient: 0.03/1= 0.03 | | |
| ibuprofen | Maximum oral exposure = $24 \mu g/d$, 36 weeks | [63] | |
| inubioien | (Pregnant women, Premature closure of the ducts arteriosus or hemodynamic changes) | [63] | |
| | Provisional guideline value = $50 \mu g/L$ (Diabetic patients, hypoglycemia) | | |
| metoprolol | Maximum concentration in drinking water: 2.1 μg/L | [63] | |
| | Benchmark quotient: $2.1/50 = 0.04$ | | |
| | Provisional guideline value = $440 \mu g/L$, 60 weeks (Rats, thyroid tumors) | | |
| sulfamethoxazole | Maximum concentration in drinking water: 0.03 μg/L | [63] | |
| | Benchmark quotient: $0.03/440 = 0.00007$ | | |

Table 3. Water Quality Standards for the Micropollutants in Environmental Agencies

| Compounds | Country | Standards (µg/L) | References |
|------------------------------|---------------|------------------|------------|
| atrazine | International | < 100 | [64] |
| | USA | < 3 | [65] |
| | Canada | <5 | [66] |
| | Australia | < 20 | [67] |
| | Europe | < 0.6* | [68] |
| 2,4-D | International | < 30 | [64] |
| | USA | < 70 | [65] |
| | Canada | < 100 | [66] |
| | Australia | < 30 | [67] |
| diclofenac | Europe | < 0.1* | [69] |
| nonylphenol | Europe | < 0.3* | [69] |
| 17α -ethinylestradiol | Europe | < 0.000035* | [69] |
| 17β-estradiol | Europe | < 0.0004* | [69] |

^{*}This value is the Environmental quality standard (EQS) expressed as an annual average value (i.e., AA-EQS) in inland surface water. Here, "inland surface water" means the rivers and lakes and related artificial or heavily modified water bodies.

4. Human Health Impact of Micropollutants in Water

Pharmaceuticals among micropollutants raised concerns about the effects of unintended exposure to humans and ecosystems. When considering the food chain, these exposures can cause persistent bioaccumulation in the ecosystem. Chronic exposure to the human body can cause potentially unknown health effects. Previous studies reported health risks to humans through chronic pharmaceutical

exposure in drinking water (Table 2).

Contamination of micropollutants can have a potentially negative effect on human health. The health effects of trace micropollutants are not clear, but people can increase their negative attitudes towards reused tap water. Because micropollutants are emerging issues in public health, water quality standards and guidelines are needed to provide safe drinking water to people. The criteria for these micropollutants are currently set in a number of countries, such as the United States, Canada, the European Union and Australia, although the levels of water quality standards are currently quite different (Table 3).

5. Removal of Micropollutants in WTPs

Several studies have estimated the removal rate of micropollutants by WTP (Table 4). Gibs et al. [70] evaluated the removal of 113 contaminants during clotting/sedimentation, sand filtration and chlorination. Acetaminophen, diclofenac and sulfamethiazine showed high removal rate (> 95%) after the water treatment process. However, the removal rate was low for micropollutants such as caffeine, carbamazepine, and bisphenol-A. Recently, Nam et al. [71] reported that the removal

efficiencies of micropollutants detected in a WTP ranged from 6% to 100%. Diclofenac, acetaminophen, caffeine, carbamazepine, and 2,4-D were effectively removed (> 80%), whereas only small amounts of metoprolol (6%) were removed in the WTP process.

Removal rates of micropollutants are inconsistent among different studies [10, 39, 72]. In particular, caffeine (~42-99%), carbamazepine (~46-99%), atrazine (~53-99%), and bisphenol A (~78-99%) have shown both high and low removal rates by WTPs, because there are often differences among plants in terms of measurement method, and process configuration (Table 4).

Table 4. Removals of Micropollutants in Water Treatment Plants

| Compounds | Influent (ng/L) | Effluent (ng/L) | Removal (%) | References |
|----------------------|-------------------|------------------|-------------|------------|
| Pharmaceuticals | | | | |
| acetaminophen | 120-150 | 0-0.3 | 98 | [73] |
| | 163-260 | 10.7-22 | 94-98 | [74] |
| | 106.1 ± 147.1 | 5 ± 9.1 | 95.3 | [71] |
| caffeine | 100-190 | ND-60 | 42-99 | [73] |
| | 100,000 | ND-119 | 88-99 | [10] |
| | 45 | ND | 99 | [6] |
| | 291-526 | ND-27.7 | 93-101 | [74] |
| | 36.1 ± 20.8 | 5.8 ± 7.4 | 84 | [71] |
| carbamazepine | 13 | = | 99 | [12] |
| | 4.1-51 | 6-18 | -46-88 | [39] |
| | 4.8 | ND | 99 | [6] |
| | 10.3 ± 9.5 | 1.7 ± 4.2 | 84.7 | [71] |
| diclofenac | 1.1-1.2 | ND | 99 | [39] |
| | 175-292 | ND | 98.8-99.2 | [74] |
| | 7.8 ± 2.45 | ND | 100 | [71] |
| ibuprofen | 15 | ND | 99 | [6] |
| | 19.6 ± 21 | 4.3 ± 6 | 78 | [71] |
| metoprolol | 68.7 | 60 | 11 | [75] |
| | 37.4 ± 34.1 | 35.18 ± 22.4 | 6 | [71] |
| naproxen | 0.9-32 | ND | 99 | [39] |
| | 99-152 | ND | 98.8-99.2 | [74] |
| | 11.8 ± 12.4 | 2.7 ± 3.8 | 78 | [71] |
| sulfamethoxazole | 30 | ND | 99 | [73] |
| | 8,000 | ND | 99 | [10] |
| | 57.7-149 | ND | 98-100 | [74] |
| | 7.8 ± 5.4 | 2.1 ± 1.9 | 73 | [71] |
| sulfamethazine | 113 | ND | 98-100 | [74] |
| | 3.7 ± 2.4 | 2.31 ± 1.7 | 38 | [71] |
| Endocrine disrupters | | | | |
| atrazine | 32-870 | 49-870 | -53 | [39] |
| | 7 | ND | 99 | [72] |
| bisphenol-A | 6.1-14 | 25 | -78 | [39] |
| | 295 | 5 | 98.3 | [72] |
| | 88 ± 102.8 | 5 ± 9.1 | 95.3 | [71] |
| nonylphenol | 100-130 | 93-100 | 7 | [39] |
| | 14.5 ± 52.1 | 12.6 ± 5.9 | 70 | [71] |

ND: Not detected

6. Removal of Micropollutants by Each Water Treatment process

6.1. Coagulation/Sedimentation

Coagulation removes particulate matter, including colloidal and dissolved substances, from water. Chemical coagulation is the main process to remove suspended solids by the addition of coagulants to change the electrostatic state of contaminants [76, 77]. Natural particles, such as clay and natural organic matter (NOM), can be negatively charged to water and electrostatically interact [78]. Natural particles such as clays, and NOM are negatively charged in water, and can therefore interact electrostatically [78]. Small particles and NOM suspended in natural water are too small to precipitate out of surface water. Positively charged metal salts (often aluminum and iron salts) are often used as coagulants. Their efficacy is influenced by pH [76, 79]. The metal salt binds to suspended particles in water via electro-neutralization at pH 5-7 [80-82]. Charge neutralization causes floc formation and these aggregation products bind to each other via van der Waals forces (i.e., sweep flocculation). These mechanisms can separate water and NOM from water.

Several previous studies have evaluated the removal of micropollutants by coagulation, using jar tests among other methods. Table 6 summarizes the removals of micropollutants during coagulation processes. In a study by Matamoros and Salvadó [83], micropollutant removal via coagulation ranged from imperceptible elimi-

nation to 50%, with relatively high removals (20-50%) observed for compounds with a K_{ow} of 4 at pH ~7-8 (e.g., galaxolide, tonalide, and octylphenol). Suárez et al. [84] reported significant reduction (~80%) of musks (e.g., galaxolide and tonalide) during hospital wastewater coagulation treatment. Other micropollutants have shown similar rates of elimination (diclofenac, max. 46%; naproxen, max. 42%; and ibuprofen, max. 23%). Asakura and Matsuto [85] found that biphenol-A could not be removed by coagulation and sedimentation, but that high removal rates for DEHP and nonylphenol (70% and 90%, respectively) were achieved through leachate treatment.

The efficiency of micropollutant removal by coagulation varies depending on conditions such as pH, coagulant type and dose (Table 5). Most micropollutants had low elimination rates (< 50%) by coagulation. However, some studies have reported an electrostatic interaction between coagulants and micropollutants. Hydrophilic micropollutants such as acetaminophen (log K_{ow} = 0.46), sulfamethoxazole (log $K_{ow} = 0.68$) and sulfamethazine (log $K_{ow} = 0.62$) can be electrically aggregated with Al^{3+} or Fe^{3+} ions in the coagulants [71, 73]. Especially, due to pKa values (SMZ = 5.7, SMA = $2.6(pK_{a1})/7.7(pK_{a2})$), sulfamethoxazole and sulfamethazine exist as negative ions at neutral pH, therefore, these compounds can be effectively coagulated to Al3+ ion of PACl (polyalumium chloride) during coagulation process. Antibiotics, such as tetracycline antibiotics (log $K_{ow} < -1.37$), have been removed at rates of ~43-94% via the coagulation process [86]. These results indicate that electrical aggregation is an important mechanism in the coagulation step.

Table 5. Removal Efficiencies of Some Micropollutants by Coagulation (modified from Luo et al. [87])

| Coagulant | Dosage with pH value presented in the parentheses | Compound | Removal (%) | References |
|-------------------|---|-----------------------|-----------------|------------|
| FeCl ₃ | 25, 50 mg/L (7) | ibuprofen | 12.0 ± 4.8 | [84] |
| | | diclofenac | 21.6 ± 19.4 | |
| | | naproxen | 21.8 ± 10.2 | |
| | | carbamazepine | 6.3 ± 15.9 | |
| | | sulfamethoxazole | 6.0 ± 9.5 | |
| | | trimethoprim | 32.1 ± 51.1 | |
| | | galazxolide | 79.2 ± 9.9 | |
| $Al_2(SO_4)_3$ | 25 mg/L (7) | diazepam | 12.5 ± 18.4 | [84] |
| | | sulfamethoxazole | 0.9 ± 14.4 | |
| | | tonalide | 75.8 ± 11.0 | |
| | | galazxolide | 76.4 ± 5.5 | |
| FeCl_3 | 100, 200 mg/L (4,7,9) | bisphenol-A | 20 | |
| | | diethylhexylphthalate | 70 | [85] |
| | | nonylphenol | 90 | |
| $Al_2(SO_4)_3$ | 200 mg/L (7) | aldrin | 46 | [88] |
| | 100 mg/L (7) | bentazon | 15 | |
| PACl | 30 mg/L (7) | sulfamethoxazole | 43 | [71] |
| | | sulfamethazine | 52 | |
| | | caffeine | 16 | |
| | | acetaminophen | 17 | |
| | | diclofenac | 0 | |
| | | metoprolol | 10 | |

Other removal mechanisms (e.g., particle adsorption and sunlight photolysis) can be used during the coagulation process to enhance micropollutant removal. Hydrophobic compounds can be adsorbed into suspended particles, and co-removed through coagulation/sedimentation processes [89]. Higher removal efficiencies for acetaminophen (76.6% with the concentrations of 24.7 \pm 43.3 ng/L), caffeine (81.2% with the concentrations of 6.7 \pm 10.5 ng/L), and diclofenac (100% with the concentration of less than the method detection limit), which are photo-sensitives, have been observed during the WTP coagulation process [71]. This result implies that sunlight photo-degradation can be an additional mechanism for micropollutant removal, because coagulation occurs in the open air; these mechanisms can also act simultaneously.

6.2. Adsorption

Adsorption by activated carbons is commonly used to control

the taste and odor of drinking water. Adsorbate and adsorbent interactions in adsorption involve complex surface reactions, hydrophobic interactions at the surface, and adsorption of surfactant or polymers and polyelectrolytes [90].

Several studies on the efficacy of micropollutant removal by adsorption have been done using lab- and pilot-scale experiments (Table 6). Powdered activated carbon (PAC) and granular activated carbon (GAC) have been widely used in adsorption processes, which can be affected by both adsorbate and adsorbent properties [91]. Micropollutant removal has been improved with increased PAC doses, independent of the initial compound concentrations [92]. Batch tests performed by Hernández-Leal et al. [92] demonstrated marked removal (> 94%) of various micropollutants (i.e., with effluent concentrations of 173 ng/L for caffeine and 9 ng/L for buthylparaben) using PAC adsorption, with initial compound concentrations of \sim 100-1,600 µg/L at a dose of 1.25 g/L and a contact time of 5 min.

Table 6. Removal Efficiencies of Some Micropollutants by Adsorption (modified from Luo et al. [87])

| Adsorbent | Dosage | Compound | Removal (%) | References |
|-----------|---|----------------------|-------------|------------|
| PAC | 8, 23, 43 mg/L | diclofenac | 96, 98, 99 | [91] |
| | | carbamazepine | 98, 99, 100 | |
| | | sulfamethoxazole | 2, 33, 62 | |
| | 100 mg/L | caffeine | > 94 | |
| | | bisphenol-A | > 94 | [92] |
| | | nonylphenol | > 94 | |
| | 5 mg/L | acetaminophen | 70-79 | [93] |
| | | caffeine | 60-62 | |
| | | diclofenac | 30-57 | |
| | | naproxen | 52-57 | |
| | | sulfamethoxazole | 30-37 | |
| | | atrazine | 55-57 | |
| GAC | Full scale | diclofenac | > 98 | [94] |
| | | carbamazepine | 23 | |
| | | estrone | 64 | |
| | | 17β-estradiol | > 43 | |
| | | 17α-ethinylestradiol | > 43 | |
| | 29 g/70.6 mL bed volume | bisphenol-A | 66 | |
| | | nonylphenol | 84 | [92] |
| | | triclosan | 95 | |
| | Full scale, empty bed contact time:15 min | diclofenac | ~100 | [95] |
| | | trimethoprim | 90 | |
| | | carbamazepine | 75 | |
| | | caffeine | 45 | |
| | 1 mg/L | acetaminophen | 58 | [96] |
| | | caffeine | 71.3 | |
| | | atrazine | 53 | |
| | | carbamazepine | 69.9 | |
| | | diclofenac | 25.5 | |
| | | ibuprofen | 23.3 | |
| | | naproxen | 46.6 | |
| | | sulfamethoxazole | 27.1 | |

PAC: Powdered activated carbon; GAC: Granular activated carbon

Interestingly, sorption coefficients of hydrophilic compounds (i.e., caffeine, acetaminophen, sulfamethoxazole, and sulfamethazine) have been shown to fit a linear isotherm, while hydrophobic compounds (i.e., naproxen, diclofenac, 2,4-D, triclocarban, and atrazine) fit a Freundlich isotherm [79]. In this study, it was found that the removal of hydrophobic pollutants and caffeine was independent of pH changes, but acetaminophen, sulfamethazine, and sulfamethoxazole were adsorbed mainly by electrostatic interaction with PAC; therefore, they were affected by pH. Adsorption removal in surface water samples was decreased; this decrease was significant for hydrophobic compounds. The decline in adsorption capacity in surface water samples was caused by the competitive inhibition of dissolved organic matter (DOM) with micropollutants into PAC. Low temperature (5°C) also decreased the adsorption removal of micropollutants, and affected hydrophobic compounds more than hydrophilic compounds.

As the elimination of trace contaminants depends largely on particle-contaminant interactions, competition for adsorption sites and/or pore blocking (by particle solids) can reduce the removal efficiency of activated carbon [97]. Snyder et al. [93] suggested that a steam-treated GAC could be employed to overcome the drawbacks of GAC, due to its greater absorption capacity. Regular regeneration of GAC also seemed of vital importance to maintain minimal breakthrough of micropollutants. Furthermore, pore shape/size and volumes of activated carbons, as well as carbon type, surface charge of compounds, and operation year, influenced removal performances [27, 96].

6.3. Chlorination

Drinking water purification generally involves antibacterial treatment such as chlorination, ozone treatment (O_3) and ultraviolet (UV-C) to prevent the spread of waterborne diseases. This technique is effective in removing pathogens (> 99%) from WTPs [98-101]. Chlorination is a disinfection process commonly used by WTP in some regions, including Korea.

Chlorination is generally not recognized as an organic contaminant removal process, but it can degrade organic contaminants through the oxidation of free chlorine [101, 102]. Chlorine molecules showed higher reactivity to aromatic pharmaceuticals and higher electrical affinity for certain functional groups of micropollutant. Chlorination is more cost-effective than other technologies (e.g., ozonation and ultraviolet light) because it is easy to perform [104]. However, since degradation by chlorination is too slow (e.g., sulfamethoxazole, acetaminophen, caffeine, and ibuprofen), chlorination is less effective (less than 20%) to remove trace amounts of micropollutants [105, 106]. Production of harmful byproducts (e.g., trihalomethane (THM), haloacetic acid, haloacetonitrile) from drinking water chlorination has been a major concern, and chlorinated disinfection byproducts are considered as emerging contaminants that require elimination by WTPs [107, 108].

6.4. Ozonation

The main reasons for applying ozone to drinking water treatment are disinfection and oxidation (e.g., taste and odor control, de-coloration, elimination of micropollutants, etc.) or a combination of both [109, 110]. Ozonation can oxidize micropollutants either by a direct reaction with ozone or indirectly after formation of hydroxyl radicals, as follows in Table 7.

Table 7. Ozonation Processes with Micropollutants (modified from von Gunten [109, 110] and Šoiić et al. [111])

| Ozonation | Reference |
|--|------------|
| directly reaction | [109, 110] |
| O_3 +Contaminants \rightarrow End products | |
| O_3 +Contaminants \rightarrow Contaminants $^{\bullet+}$ + O_3 $^{\bullet-}$ | |
| indirectly reaction | |
| $H_2O \rightleftharpoons H^+ + OH^-$ | [109, 111] |
| $O_3 + OH^- \rightarrow HO_2^- + O_2$ | |
| $O_3+HO_2^- \rightarrow \bullet OH+O_2^{\bullet-}+O_2$ | |
| $O_3+O2^{\bullet-} \rightarrow O_3^{\bullet-}+O_2$ | |
| $Contaminants + \bullet OH \rightarrow Contaminants - H + H_2O$ | |
| Contaminants– $H+\bullet OH \rightarrow End$ products | |

6.5. Advanced Oxidation Processes (AOPs)

Various AOPs such as UV radiation, UV/Cl₂ and UV/O₃ have been attempted to remove micropollutants (Table 8). This process uses a radical species (e.g., chlorine radical ('Cl), hydroxyl radical ('OH), and ozonide radical ion (O₃ $^-$)) to degrade micropollutants by oxidation. The main removal mechanisms of these processes for micropollutants are shown in Table 8.

Table 8. Removal mechanisms of O₃, UV, Cl₂/UV, and UV/O₃ process for micropollutants removals

| ioi micropolidadio removais | |
|--|------------|
| Processes | References |
| UV radiation (UV) | |
| $H_2O+UV-C \rightarrow `H+`OH$ | [38, 112] |
| Contaminants+'OH \rightarrow Contaminants-H+H ₂ O | |
| Contaminants– $H+$ OH \rightarrow End products | |
| Chlorination-UV radiation (Cl ₂ /UV) | |
| $Cl_2+H_2O \rightarrow HOCl+HCl$ | [113, 114] |
| $HOCl+UV-C \rightarrow 'OH+'Cl$ | |
| Contaminants+'OH \rightarrow End products+H ₂ O | |
| Contaminants+'Cl \rightarrow End products+H ₂ O | |
| UV radiation-ozonation (UV/O ₃) | |
| $O_3+hv \rightarrow O_2+O$ | [111, 115] |
| $O'+H_2O \rightarrow 2HO'$ | |
| $O_3+hv+H_2O \rightarrow O_2+H_2O_2$ | |
| $H_2O_2+hv \rightarrow 2HO^{\bullet}$ | |
| Contaminants+'OH \rightarrow Contaminants-H+H ₂ O | |
| Contaminants– $H+$ OH \rightarrow End products | |

Micropollutants are rapidly degraded from parent compounds to byproducts through continuous radical attack. Micropollutants rapidly degrade from parent compounds to their byproducts through continuous radical attacks. A study by Sui et al. [116], on the efficiency of ozonation for the removal of various micropollutants, showed that carbamazepine, diclofenac, indomethacin, and trimethoprim concentrations were reduced by more than 95% at an applied ozone dose of 5 mg/L. A study conducted by Gerrity et al. [117] focused on the application of O₃/H₂O₂ for removing a suite of micropollutants during water reclamation. This process had considerable removal efficiency (> 90%, with the concentrations of $< 0.50 \sim < 25$ ng/L in the ozone effluents) for almost all of the target contaminants. Kim et al. [118] investigated the effects of UV (wavelength: 254 nm) -based processes (UV and UV/H2O2) to remove 41 micropollutants. While UV alone can only remove only a few compounds at a significant level (> 90%; e.g., ketoprofen, diclofenac and antipyrine), and macrolide has been observed to be ineffective removal (\sim 24-34%). In contrast, the addition of H_2O_2 (7.8 mg/L) in UV significantly improved the efficiency of the process and increased the removal efficiency to 90 for 39 out of 41 compounds.

Oxidation generally does not result in complete mineralization, but in many cases forms a transformed product with much lower biological activity than the parent compound [119-122]. Most organic compounds, including micropollutants, are converted to hydrophilic byproducts with similar or lower molecular weights [123-127]. Richardson et al. [128] reported that most conversion products formed during ozonation have found to contain oxygen in structures such as aldehydes, ketones, and carboxylic acids. In addition to the formation of the conversion products, other unwanted byproducts may be formed, such as bromate, which is a potential human carcinogen formed during the ozonation of the bromide-containing water by a complex mechanism involving both ozone and hydroxyl radicals [109, 110]. N-nitrosodimethylamine (NDMA) formation also has been reported during drinking-water ozonation [129, 130].

 UV/H_2O_2 oxidation is a promising drinking water production technology for the reduction of a wide range of organic pollutants and undesirable natural organic constituents [131-133]. Recent studies have reported that UV/H_2O_2 can increase the formation of controlled trihalomethanes (THMs) and haloacetic acid (HAA) under certain conditions [134, 135], whereas medium-pressure UV at high fluence (as in AOPs) could destroy some NDMA precursors [136]. Chu et al. [137] investigated changes in haloacetamide formation and speciation attributed to UV, H_2O_2 or UV/H_2O_2 , followed by the application of free chlorine to quench any excess hydrogen peroxide and to provide residual disinfection. The results showed that H_2O_2 preoxidation alone resulted in diiodoacetamide formation in two iodide-containing waters and increased bromine utilization.

It has recently been reported that a combination of disinfectants with AOP can be used to remove contaminant micropollutants. Šojić et al. [111] showed that 84% of metoprolol was degraded using the UV/O_3 reaction. Recently, Nam et al. [114] have shown that the UV/Cl_2 process is effective in treating methoproprol by generating OH and Cl radicals. After the filtration step in WTPs, the UV/chlorination process can be used not only for disinfection purposes but also for the removal of micropollutants.

7. Conclusions

Micropollutants are discharged to surface water from untreated STP and WWTP wastewaters. Some micropollutants enter WTPs after being discharged into surface waters. Conventional WTP processes such as coagulation, precipitation, chlorination and adsorption can remove trace amounts of micropollutants. However, the removal efficiency varies depending on the physicochemical properties of the micropollutants. Alternatively, AOP can be applied to improve removal of micropollutants in WTPs. Although advanced treatment techniques have proven to be promising alternatives for the removal of micropollutants, there are two problems associated with the application; high operating costs and the formation of undesirable by-products. Thus, a comprehensive understanding of the fate and toxicity of microorganisms and their byproducts in surface water and drinking water is essential to effectively predict effects of micropollutants on the receiving environment.

Acknowledgements

This review was supported by the International Research & Development Program of the National Research Foundation of Korea (NRF) funded by the Ministry of Science, ICT and future Planning (NRF-2014R1A2A1A11052928).

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