# Hazard Analysis and Risk Assessments for Industrial Processes Using FMEA and Bow-Tie Methodologies

### Islam H. Afefv\*

Industrial Engineering Department, Faculty of Engineering, Fayoum University, Fayoum, Egypt

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### **ABSTRACT**

Several risk assessment techniques have been presented and investigated in previous research, focusing mainly on the failure mode and effect analysis (FMEA). FMEA can be employed to determine where failures can occur within industrial systems and to assess the impact of such failures. This research proposes a novel methodology for hazard analysis and risk assessments that integrates FMEA with the bow-tie model. The proposed method has been applied and evaluated in a real industrial process, illustrating the effectiveness of the proposed method. Specifically, the bow-tie diagram of the critical equipment in the adopted plant in the case study was built. Safety critical barriers are identified and each of these is assigned to industrial process with an individual responsible. The detection rating to the failure mode and the values of risk priority number (RPN) are calculated. The analysis shows the high values of RPN are 500 and 490 in this process. A global corrective actions are suggested to improve the RPN measure. Further managerial insights have been provided.

Keywords: Safety, FMEA, RPN, Bow-tie

\* Corresponding Author, E-mail: islamhelaly@yahoo.com

### 1. INTRODUCTION

For any industry processes to be successful, it has become essential to identify and analysis of the hazards types and sources, to assess the associated risks and to bring the risks to an acceptable level. The bow-tie model was applied to large scale industries, for the probabilistic assessment of risks of major industrial accidents. Many researches on FMEA have been carried out but still some applied research in the industrial processes field is required so, about explore the successful utilization of the FMEA technique in the area of manufacturing and design in large industrial process scale. Liu *et al.* (2011) discussed traditional FMEA Using fuzzy evidential reasoning approach and grey theory. A Novel approach for prioritization of failure modes in FMEA us-

ing multi criteria decision making techniques (MCDMT) is discussed by Maheswaran and Logan (Maheswaran and Logan, 2013).

Bow-tie diagram combines fault tree (FT) and event tree (ET) analyses to explore the primary causes and consequences of a critical event (Kahn *et al.*, 2014). The bow-tie diagram has widely been used in risk analysis, reliability engineering and safety assessment presented by Aneziris *et al.* (2008). Bellamy *et al.* (2013) introduced an application of bow-tie in industrial practice, the "Storybuilder" method, to identify the dominant patterns of safety barrier failures, barrier task failures, and underlying management flaws. An evaluation of barrier performance can be achieved with this approach. An important and useful feature is that this barrier analysis helps to identify missing or ill-designed barriers that is a key-

issue in risk assessment. Kurowicka et al. (2006) gives a detailed account of bow-tie diagram and the barrier functions associated with it. A semi-quantitative assessment of occupational risks using bow-tie representation is presented by Celeste and Cristina (2010). They presented and discussed a specific case study, in the shipyard's technological area of surface treatment and protection, to demonstrate the method's applicability and usefulness. Techniques to identify and evaluate risks in the process and to decide how to act on them in order to eliminate or reduce them to protect the population and the environment are often mistaken. Summarizing these two categories of techniques, they can distinguish the following general components (Catalin et al., 2013): (1) to identify risks: is the intrinsic presence, observation of what happens. Hazard and operability analysis (HAZOP) method is a method for identifying operational problems associated with the design, maintenance or operation of the safety system. It is an objective process to evaluate the different parts of a given system that provides a systematic and well-documented potential hazard and (2) risk assessment: their intrinsic presence, previous experience, codes of practice use the method hazard analysis (HAZAN) estimation method used to assess hazards to decide how to take action to eliminate or reduce the risk.

From all the above, it is apparent that bow-tie methodology represents a step forward in the current state of the art concerning the management of risks, including those associated with occupational safety. This is the context in which the authors equated the use of the qualitative bow-tie diagram in combination with a matrix approach, based on accident statistics of the activity under analysis. To demonstrate the proposed methodology for hazard and risk assessments analyses, this paper describes an application case in a large industrial scale, called Emisal company which located in Fayoum city, Egypt, whose main activity is to produce anhydrous Sodium Sulphate and Sodium Chloride refined salt), Magnesium sulphate Heptahydrate (Epsom salt), Sodium chloride Pure.

Hence, the main objective of this paper, though, is twofold: (1) to explore FMEA methodology for identifying potential failure modes for process, assess the risk associated with those failure modes and prioritize issues for corrective action and identify and carry out corrective actions to address the most serious concerns and (2) to as certain to what extent the bow-tie diagram would

be successfully applied to occupational risks, in individual firms, by their own people.

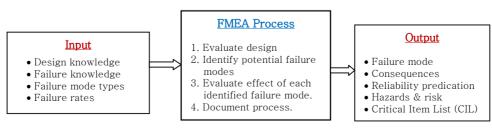
### 3. METHODOLOGY

There are several techniques developed to perform the risk assessment to mitigate the suffering. FMEA is one of the most widely used risk assessment tool. Recently, FMEA has been adopted in wide spectrum of fields such as the chemical, aerospace, military, automobile, electrical, mechanical and large scale industries. The FMEA provides reliability and safety of a plant and helps to identify the potential process failures existing in a plant (Arun *et al.*, 2013). Bow-tie model is one of the best tools developed for this communication. Barriers may be strong against a specific accident sequence and hence have smaller holes or weak which contribute to reduction of human error routes and which would permit larger holes (Celeste and Cristina, 2010).

### 3.1 Failure Mode and Effect Analysis (FMEA)

The basic FMEA process is presented in Figure 1. The FMEA process evaluates the overall impact of each and every component failure mode. The FMEA objective is to determine the effect on system reliability from component failures, but the technique can be extended to determine the effect on safety. FMEA input data includes detailed hardware/function design information. Design data may be in the form of the design concept, the operational concept, and major components planned for use in the system and major system functions. FMEA output information includes identification of failure modes in the system under analysis, evaluation of the failure effects, identification of hazards, and identification of system critical items in the form of a critical items list (AIAG, 2002).

Actually, the FMEA methodology is designed to identify potential failure modes for process, assess the risk associated with these failure modes and prioritize issues for corrective action and identify and carry out corrective actions to address the most serious concerns (Virtanen and Hagmark, 2007). In FMEA, failures are prioritized according to how serious their consequences are, how frequently they occur and how easily they can



**Figure 1.** FMEA overview.

be detected. Ideally, FMEA begins during the earliest conceptual stages of design and continues throughout the life of the product or service. Results are used to identify high-vulnerability elements to guide resource deployment.

An FMEA can be done any time in the system. RPN is simply calculated by the following equation:

The total RPN is calculated by adding all of the risk priority numbers. The small RPN is always better than the high RPN. It could be computed for the entire process and/or for the design process only. Once it is calculated, it is easy to determine the areas of greatest concern. There could be less severe failures, but which occur more often and are less detectable. These actions can include specific inspection, testing or quality procedures, redesign (such as selection of new components), adding more redundancy and limiting environmental stresses or operating range. Once the actions have been implemented in the design/process, the new RPN should be checked, to confirm the improvements (Janarthanan, 2013; Abdel-Aziz and Helal, 2012).

## 3.2 Bow-Tie Methodology

It is used for risk assessment, risk management and risk communication. This methodology is designed to give a better overview of the situation in which certain risks. In addition, bow-tie methodology helps people understand the relationship between the risks and organizational events. It is a graphical tool to illustrate an accident scenario, starting from accident causes and ending with its consequences. While centered on a critical event, bow-tie is composed of FT on the left-hand side identifying the possible events causing the critical event (or top event), and ET on the right-hand side showing the possible consequences of the critical event based on the failure or success of safety barriers (Zuijderduijn, 2000; Nicola et al., 2013). Figure 2 identifies the main threats on the left hand-side and demonstrates in a "bow-tie" shape how barriers prevent the escalation of the initial threats to one of several final outcomes. Safety critical barriers are identified and each of these is assigned to a business group with an individual responsible. Outline of bow-tie construction is introduced in Figure 3. Risk in bow-tie methodology is elaborated by the relationship between hazards, top events, threats and consequences (see Figure 4). Barriers are used to display what meas-

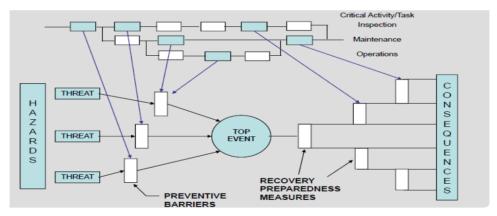


Figure 2. Bow-tie modeling.

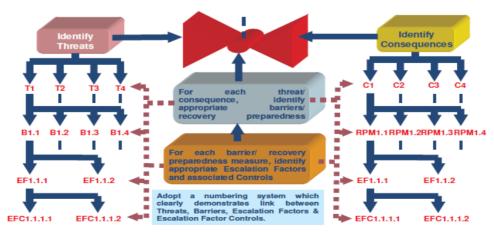


Figure 3. Bow-tie construction (Ramzan, 2006).

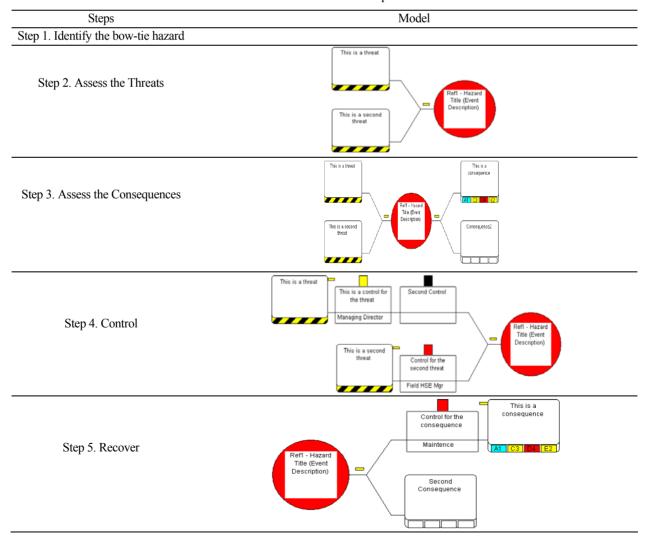
ures an organization has in place to control the risk. The process involves the systematic identification of hazards and effects, assessment of the associated risks and the

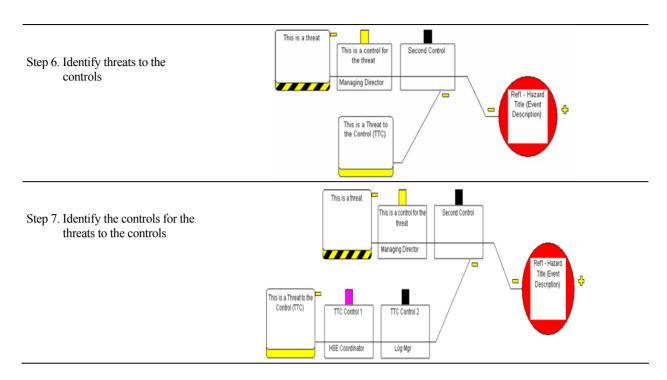
specification of the control and recovery measures which must be in place and maintained in place. Bow-tie diagrams of industrial processes critical components will be

		CONSEQ	UENCES		LIKELIHOOD					
			=		1	2	3	4	5	
SEVERITY	People	Asset	Environment	Reputation	Very Unlikely	Unlikely	Possible	Likely	Very Likely	
1	No/ Slight Injury	No/ Slight damage	No/ Slight effect	No/ Slight Impact	Low	Low	Low	Low	Low	
2	Minor Injury	Minor damage	Minor effect	Limited Impact	Low	Low	Low	Medium	Medium	
3	Major Injury	Local damage	Local effect	Major Impact	Low	Low	Medium	Medium	High	
4	Fatality	Major damage	Major effect	Nat. Impact	Low	Medium	Medium	High	High	
5	Multiple fatalities	Extensive damage	Massive effect	Internat. Impact	Medium	Medium	High	High	High	

Figure 4. Risk assessment matrix.

**Table 1.** The bow-tie steps





built using risk analysis software (bowtiexp-6.03). From bowtiexp-6.03 software, bow-tie steps are listed in Table 1.

## 4. CASE STUDY

In this paper, the FMEA and bow-tie methodology areapplied to a particular type of accident in the anhydrous Sodium Sulphate factory, The critical equipment in factoryconsists of (melter, boiler, crystallizer, thickener, evaporators, packing machines, centrifugal pump, plate heat exchanger and screw pumps). This equipment was selected based on analysis of historical data of the factory and interviews with key personnel involved in the safety, maintenance and operation.

# 5. RESULTS AND DISCUSSIONS

In this section, results and discussions of real case study analyses are presented. First, the results for hazard analysis through FMEA in case study are discussed. Second, the results associated to the risk analysis through the bow-tie diagram are carried out.

### 5.1 Hazard Analysis Through FMEA

There are nine subsystems identified, at which potential failure mode (FM) can occur, as shown in Table 2. In this table, FMEA punctuation form is presented. It shows the form of FMEA for S, O and D. The calculated RPN values and criticality for the failure modes are presented. There are several FM with high values of RPN. It can be observed that the values of RPN for packing

and sewing machines are 500, 490 respectively. Packing machines are the highest criticality values of failure modes. In Figure 4 and Figure 5, comparison between current and new values of RPN for potential failure mode is presented. These figures show that the difference ( $\Delta d = RPN$ Current-RPN New) and difference percentage ( $\Delta d\%$  = (Δd/RPN Current)×100) values of RPN for potential failure modes. It is found that there are improvements of these FM which reflect the reducing values of RPN for potential failure modes. Also, it is noticed that the value of RPN for packing machines decreases from 500 in the current conditions to 36 in the new conditions and value of RPN for sewing machine decreases from 490 in the current conditions to 48 in the new conditions. Based on these results, global corrective actions were suggested to improve the RPN.

# 5.2 Risk Analysis Through the Bow-Tie Diagram

As shown in Figure 7 to Figure 14, the main threats on the left hand-side and demonstrates in a "Bow-tie diagram" shape how barriers prevent the escalation of the initial threats to one of several final outcomes are introduced. As can be seen from these figures, safety critical barriers are identified and each of these is as-signed to industrial process with an individual responsible. Some shell sites use a feature called matrix of permitted operations which defines in matrix format what activities may or may not be done if the relevant barrier is not functional. This is a form of risk based operations, but it focuses on forbidden operations and it is understood the approach has not found favor in ope-rating sites as it is too restrictive on operations. Figure 9 shows bow-tie diagram of packing worker injury. The main

Table 2. FMEA Sheet for factory

RPN	New 24 16		40	20	∞	9		
Corrective Actions Recommended		Maintenance and cleaning the heat Exchanger     Precaution signs.	I. Isolation by guard rail.     Preventive maintenance.     Warning signs.     Wearing PPE at all time.	<ol> <li>Isolation by guard rail.</li> <li>Warning signs.</li> <li>Training of workers to increase awareness.</li> </ol>	Preventive maintenance.     Wearing PPE at all time.     S. Following Operation manual correctly.	No recommendation	Checking two electrical line and inspection generators continuously	
RPN	Current	96	06	120	80	168	210	
	D	∞	3	5	10	4	ĸ	
	Current Controls	None	Isolation	None	None Preventive main- tenance		Diesel generator stand by	
	0	$\omega$	5	4	1	7	7	
Risk Factors (or) Criteria	Potential Causes	Deposits inside pipes	Bad insulation	Operator contact with rotating parts	- Over load - No preventive - maintenance	Increase sodium sulfate crystals concentrations	- Interruption in secondary electric line Diesel generator out of service.	
	S	4	9	9	∞	9	9	
	Potential Failure Effects	factory trip	Burning and scalds to operator.	Cut and other injuries and may lead to death due to the high kinetic energy involved in centrifuge	Total destruction to the machine	Pumps out of service		
Ŋä	LIM	FM 1: Burst of pipe due to pipe blockage FM 2: Buming skin of operator		FM 3: Draw bodies	FM 4: Mechanical failure.	FM 5: Mechanical failure (operational problem)	FM 6: Electricity supply fails	
Cuberntom	Subsystem		Heat exchanger	Continues	discontinues	Pumps		

 Fable 2. (Cont.)

	RPN New	14	14	48	30	36	48	18	9	
	Corrective Actions Recommended  1. Training to operators 2. Following Operation manuals correctly 3. Regular preventive maintenance and		o. Regular preventive maintenance and inspection.	Personnel protective equipment. Installing mechanical guard.	Use three source of energy applying preventive maintenance	Applying preventive maintenance of valve FCV 158 and pipeline	Inspection sensor continuously use pressure safety and relief valves	Inspection sensor continuously use pressure safety and relief valves	Use three source of energy applying preventive maintenance	
	RPN Current	105	105	490	196	192	252	160	28	
	D	5	5	10	7	8	7	4	m	
	Current Controls	Overload and speed indicator	Alignment sensor	None	Using another energy source corrective maintenance	Checking pipes and valves	Checking sensor and valve	Checking sensor and valve	Using another energy source corrective maintenance	
	0	w w		7	4	ε 4		v	4	
Risk Factors (or) Criteria	Potential Causes	Overload and speed indicator not operating	Alignment sensor not operating	Operator not focused while performing the work.	Mechanical failure electricity fails	Valve FCV 15 fails to open. Steam pipe defect. Valve FCV 158 fails to open.	Sensor TI144 fail to detect pressure increase steam flow	Sensor PI115 fail to detect temperature increase steam flow	Mechanical failure electricity fails	
	S			7	7	L         8         9         8			٢	
	Potential Failure Effects	Factorytrip.		Injury to worker				Evaporator fail to operate		
	FM	FM 7: Belt damage		FM 8: Injury of the hand of the operator	FM 9: Feed pumps trip	FM 10: No heating steam	FM 11: Increase steam pressure	FM 12: Increase steam temperature	FM 13: Flipping pump P1334A fail	
Subsystem		Belt conveyor transporting the salt from Dryer to storage		Sewing machine (close up the salt bag)				Evaporator		

Table 2. (Cont.)

		New	8	g of 20 mce	ıce 12	e ck 27	Jse f 18	ing 12	9 9	18	e of 36	36
	Corrective Actions	Recommended	Valve preventive maintenance	- Continuous checking of safety valve - Preventive maintenance of safety valve	Preventive maintenance	Checking temperature Use automatic interlock of temperature	Fuel valve checking Use automatic interlock of safety valve	Inspection and checking water feed pump	Continuous checking of pump Preventive maintenance of pump	Continuous checking of pump Preventive maintenance of pump	Personnel protective equipment.     Manual activation of machine clamps.     Training.	Personnel protective equipment.
	RPN	Current	224	245	192	288	216	294	168	192	500	336
		D	4	5	4	9	9	7	9	9	10	∞
	Criteria	Current Controls	Inspection of safety valve	Checking of pump	Corrective maintenance	Temperature sensor checking	Temperature sensor checking	Checking water feed pump	Checking / inspection of pump	Checking and inspection of pump shaft	None	
	ors (or) (	0	8	7	8	8	9	7	7	8	10	7
,	Risk Factors (or) Criteria	Potential Causes	- Valve defects - control fails	Feed-water pump failure	Control failure	Incorrect burner sequence	Too much fuel being fired	Low water	Pump rotation incorrect	Impeller damaged or loose on shaft	Operator not focused while performing the work.	Worker lifting the salt bags the wrong way.
		S	7	7	9	9	9	9	4 4		v.	9
	Potential Failure	Effects	Boiler failure (operate-explosion)				- Boiler trip - Co-generation plan Trip - Sodium Sulphate factory Shutdown					
		FIVI	FM 14: Drum safety valve	FM 15: Low level drum	FM 16: Flame failure	FM 17: Excessive high	superheated outlet temperature	FM 18: Low steam pressure	FM 18: Low steam pressure FM 19: Low discharge pressure		FM 20: Machine trapping worker hands while he is feeding the bags.	FM 21: Back ach of the
	Subsystem					Packing machines.						

Table 2. (Cont.)

RPN	New	27	45	49	48	09		
Corrective Actions	Recommended	Use three source of energy applying preventive maintenance	Use three source of energy applying preventive maintenance	Inspection of pipeline and applying preventive maintenance in system pies	Use three source of energy applying preventive maintenance	Inspection and calibrating sensors continuously applying preventive maintenance in sensor		
RPN	Current	84	96	112	72	120		
	D	4	3	4	3	5		
	Current Controls	Using another energy source corrective maintenance	Using another energy source corrective maintenance	Checking pipeline and pump	Using another energy source corrective maintenance	Calibrating sensors		
teria	0	3	ε 4		3	4		
Risk Factors (or) Criteria	Potential Causes	Mechanical failure electricity fails	Mechanical failure electricity fails	Feeding pumpstrip Defects in cooling material pipeline	Pumps trip	Sensor failure and not calibrated		
	S	7	8	7	8	9		
	Potential Failure Effects			Crystallizer fail to operate				
	НМ	FM 22: Cooling pump fails	FM 23: Brine pump fails	FM 24: No cooling in crystallizer shell	FM 25: No brine in crystallizer	FM2 6: Sensors (to detect temperature) trip		
Subsystem	The second			Crystallizer				

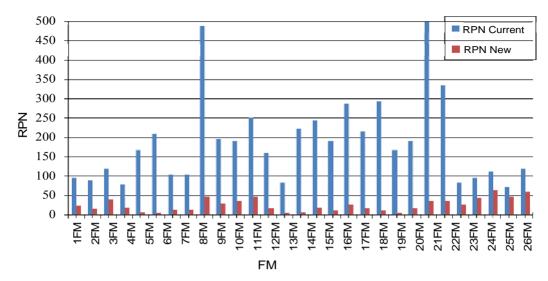
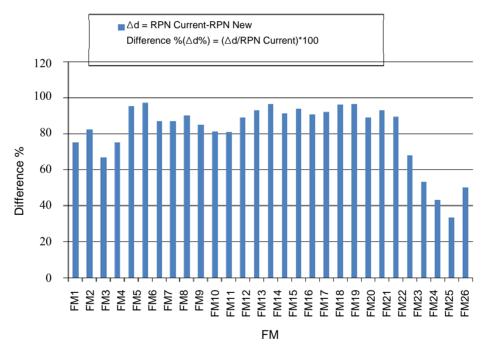


Figure 5. Comparison between current and new RPN values for FM.



**Figure 6.** Shows the RPN difference for FM.

threats of the working injury are safety working montoring, install, and regular inspection. The main consequence of corrective action of packing worker injury is application of OSHA. Figure 11 shows bow-tie diagram of noise injury. In Figure 15, bow-tie risk assessment is plotted. As can be seen from this figure, risk categories in factory for people, asset, environment and reputation. From this figure, the values in red and brown are considered critical. The subsystem on each zone found to have RPN highest value were studied further to minimize the S, reduce the O of the failure mode, and improve the D. Based on these results, the main conse-

quence of the corrective action should be applied in critical equipment for factory.

# 6. CONCLUSION

In this paper, bow-tie and FMEA methodologies are suggested to hazard analysis and risk assessments for the industrial processes. FMEA is a systematic tool for identifying the effects or consequences of FM and is used to eliminate or reduce the chance of failure. Bow-tie is considered as an approach that has both proactive

and reactive elements and that systematically works through the hazard and its management. Moreover, bowtie is particularly useful to represent the influence of safety systems on the progression of accident scenarios. Safety systems, either technical or organizational elements, are placed in two main branches of the diagram.

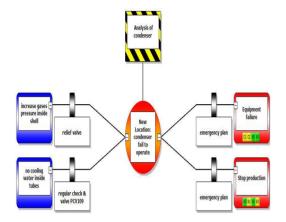


Figure 7. Bow-tie diagram of condenser.

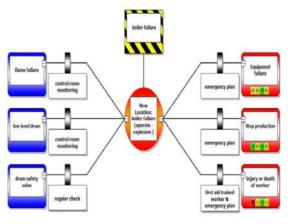


Figure 8. Bow-tie diagram of boiler.

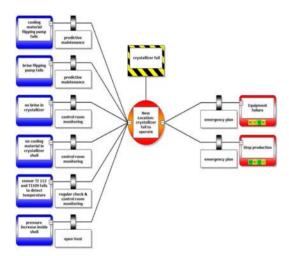


Figure 9. Bow-tie diagram of crystallizer.

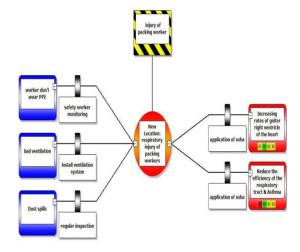


Figure 10. Bow-tie diagram of packing worker injury.

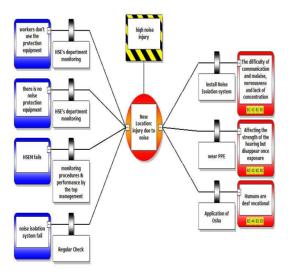


Figure 11. Bow-tie diagram of noise injury.

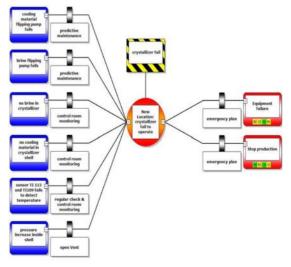


Figure 12. Bow-tie diagram of crystallizer damage.

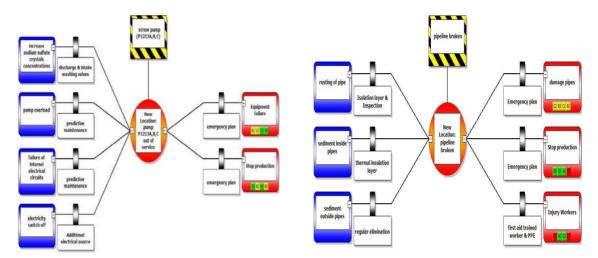


Figure 13. Bow-tie diagram of screw pump Failure.

Figure 14. Bow-tie diagram of piping subsystem.

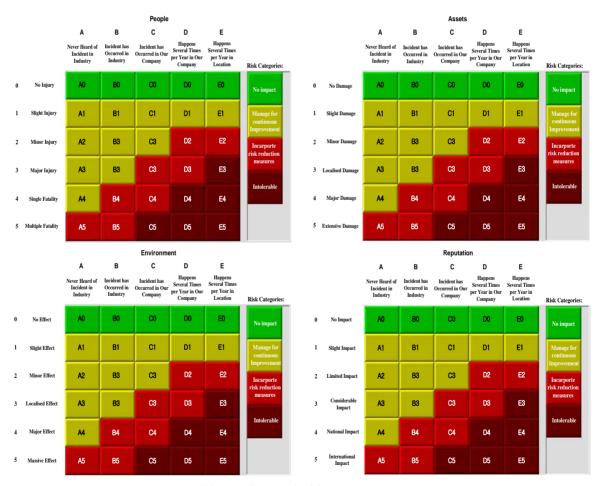


Figure 15. Bow-tie risk assessment.

Bow-tie model is essentially a probabilistic technique, but in time it has developed in different versions, depending on the system under analysis.

This paper has introduced a new methodology that

integrates FMEA and bow-tie, presenting the proper way for application in process industry. This paper has thus described an application case in a large industrial scale, called Emisal company which located in Fayoum

city, Egypt. As a result of this methodology, the detection rating to the failure mode, the values of RPN are calculated based on FMEA analysis. A set of corrective actions are suggested to improve the values of RPN. As a result of the subsequent bow-tie analysis, safety critical barriers are identified and each of these is assigned to industrial process with an individual responsible. The results show the effectiveness of the proposed methodology in process industry.

The current research can be further extended in future research work through various directions. The first direction can be the integration of the proposed methodology with other risk assessment techniques. Furthermore, the proposed method can be applied to other industrial and risk environments.

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