

Numerical approach for comparative performance study of tube type and box type hybrid photovoltaic/thermal system

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시뮬레이션을 통한 박스형과 튜브형 태양광열 복합 시스템의 성능 분석

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Abstract

태양광열 복합 시스템(photovoltaic/thermal hybrid solar system, PV/T)은 태양광 모듈 및 태양열 집열판의 단일화를 통한 전기 및 열에너지의 동시 생산이 가능하도록 구성되고 기존 태양광 모듈의 온도 상승에 따른 효율 저하의 문제점을 보완 및 발생하는 열을 회수하여 온수 생산이 가능한 장치이다. 본 연구에서는 액체형 PV/T 시스템의 대표적인 두 형태인 박스형과 튜브형의 성능 검증을 위하여 수학적 모델링을 통한 두 시스템의 열 및 전기적 성능을 비교·분석하였다. 모델링은 에너지 평형식을 이용하여 시간에 따른 각 부분의 온도의 변화를 예측할 수 있도록 수립되었으며 계산된 결과를 기준으로 전기, 열, 및 전체효율을 도출해 내고, 이를 바탕으로 두 시스템의 성능을 분석하였다. 시뮬레이션 결과를 바탕으로, 박스형 PV/T 시스템의 최고 온수 온도는 52°C로 예측되었고, 반면에 튜브형은 48°C에 머물렀다. 또한 열효율은 박스형이 최대 51%, 튜브형이 41%, 전기효율은 박스형이 약 14%, 그리고 튜브형이 13%로 나타났으며, 전체효율은 박스형이 73%, 그리고 튜브형이 64%로 나타나 박스형 PV/T 시스템이 튜브형보다 더 나은 성능을 가지는 것으로 예측되었다. 이는 박스형이 튜브형보다 태양광 모듈과 온수와의 접촉면적이 넓어 더 많은 열전달이 발생하기 때문으로 사료된다.

Keywords : 태양광열(Photovoltaic/thermal), 시뮬레이션(Simulation), 효율(Efficiency), 성능분석(Performance analysis)

Nomenclature

A	: aperture area, m ²	h	: heat transfer coefficient, W m ⁻² K ⁻¹
C	: specific heat capacity, J kg ⁻¹ K ⁻¹	M	: mass, kg
E	: electrical power output, W m ⁻²	\dot{m}	: mass flow rate, kg s ⁻¹
P	: packing factor	Ra	: Rayleigh number
G	: solar radiation, W m ⁻²	T	: temperature, °C
		t	: time, s

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Greek

- σ : Stefan-Boltzmann Constant
- α : absorptance
- ϵ : emissivity
- δ : thickness, m
- η : efficiency
- ρ : density, kg m⁻³
- $(\tau\alpha)_p$: effective absorptance of plate
- ϕ_c : solar cell temperature coefficient, K⁻¹
- τ : transmissivity
- θ : collector tilted angle

Superscript

- + : critical

Subscripts

- a : ambient air
- c : collector
- cd : conductive
- cv : convective
- e : electrical
- g : glazing
- i : inner; inlet; insulation material
- o : outlet
- p : PV plate
- r : radiative
- t : tube; tube bonding
- th : thermal
- tk : tank
- w : water
- wind : wind induced
- 1 : channel or tube inlet
- 2 : channel or tube outlet

1. Introduction

A photovoltaic/thermal (PV/T) solar system is the solar technology that allows for simultaneous conversion of solar energy into both electricity and heat. Photovoltaic(PV) cell cannot absorb the solar energy within the full radiation spectrum range. Most part

of the incident energy (around 85%) is rejected to the surrounding environment in the form of heat and this heat has negative effects in the electrical output of crystalline Si based PV cell. The electrical conversion efficiency reduces 0.4 to 0.5% per degree rise in temperature for crystalline-silicon cells¹⁾²⁾³⁾ which causes significant drop of electric energy. PV/T system overcomes this disadvantage and improves both the electrical and thermal performance of the system. This also increases the aesthetic views, reduces the space and material cost as compared to the separated PV and solar thermal systems being placed side by side⁴⁾. The PV/T system has been analysed both for steady state and dynamic conditions. The steady state analysis was done through the quasi-steady-state analysis using hourly weather data. With the use of steady state models, performance of PV/T collector had been studied both experimentally⁵⁾⁶⁾⁷⁾ and numerically⁸⁾⁹⁾¹⁰⁾. Zondag et al.¹¹⁾ introduced extensive 3D dynamic model which was not developed for the simulation purpose. Later on, Chow¹²⁾ developed the dynamic model for the single glazed flat plate water-heating PV/T collector and verified through experiments.

Water type PV/T systems have been distinguished on the basis of water flow pattern. The commonly used water type PV/T systems are sheet and tube type, channel, free flow, and two absorber type¹³⁾. Zondag et al.¹⁴⁾ studied the various concepts of the PV/T systems and found that channel below transparent PV design gave the best efficiency. The problems reported in the sheet and tube type collectors were fin efficiency and bonding quality¹²⁾. The PV encapsulation

using the TPT (tedlar–polyester–tedlar) and the EVA (ethylene–vinyl acetate) layers caused the good bonding between the PV and thermal absorber. The temperature difference between the front part and the back sides of the absorber was found not more than 1°C ¹⁵⁾. Chow et al.¹⁶⁾ recommended the flat–box thermal absorber PV/T system for the improvement of fin efficiency. The results showed that the flat box structure improved heat transfer and durability of the PV/T system.

The aim of this work is to numerically study the thermal and electrical performances of a box type and tube type PV/T systems. The comparative performance analysis of tube type and box type PV/T system was investigated on the basis of total electrical and thermal output produced per unit area of collector with respect to same packing factor, mass flow rate and weather conditions.

2. Mathematical model

The dynamic model developed by the Chow¹²⁾ and Chow¹⁶⁾ were used for the simulation study of tube type and box type PV/T system respectively. The model was developed for the aperture area of 1 m width and 1 m length. The packing factor was 0.9375, which was the ratio of solar module area to the absorber area. The polycrystalline solar cell of cell conversion efficiency 14.5% was used for the simulation. The solar module having open circuit voltage 37.1 V, maximum power voltage 31 V, short circuit current 8.05 A and maximum power 240 W at standard test conditions was selected. The mass flow rate of each system was

76kg/hr. The flow in the box type was designed for the natural flow system and for the tube type, it is considered as a forced flow system.

2.1 System description

The PV/T system generally consists of glazing, photovoltaic panel, thermal absorber plate and insulations. Solar cell is inserted in the encapsulated materials. Flat box type aluminum alloy collector consists of small channels through which water is passed. The PV module is cleaved to the upper portion of the aluminum alloy thermal absorber. All the above components are also similar to the sheet and tube type PV/T system except bonding the water tubes with absorber plate. There is metallic bond between the absorber plate and the water tubes and the insulation air layer between the front glazing and the PV encapsulation. The basic difference between the tube type and box type systems are shown in Table 1. Due to the greater numbers of water channels, covering the total surface area of the thermal absorber, on the box type collectors, its fin efficiency was expected to be higher than that of tube type system. The tube type system consisted of fewer numbers of tubes in contact with the absorber as shown in Fig. 2 (b) and (c). The edges and bottom of both types of the panel are inserted with thermal insulation. The entire components are housed in a steel frame. The schematic diagram of the components of flat box type and sheet and tube type are shown in Fig. 1 and Fig. 2 (a) and (b) respectively.

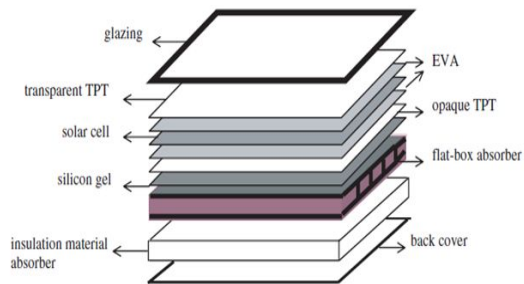


Fig. 1 Constituents layer of box type PV/T system¹⁶⁾

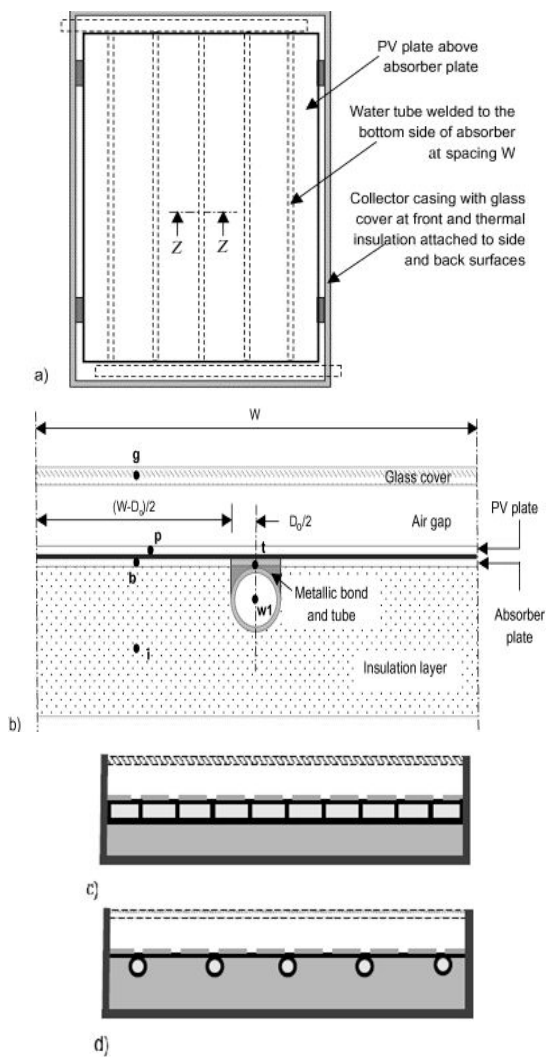


Fig. 2 Sheet and tube type PV/T collector (a) front view (b) section Z-Z¹²⁾ (c) side view of box type (d) side view of tube type PV/T system.

2.2 The system model

To describe a model for both systems, a mathematical simulation using energy balance should be addressed. The full details of energetic models are given in Chow¹²⁾ for the tube type and Chow¹⁶⁾ for the box type.

Table 1. Major differences in design between the box and tube type PVT system

Descriptions	Tube Type	Box type
Tube spacing	Required	Not required
No of channels	5	50
Bonding	Bonding between absorber plate and tube	No bonding
Contacting area between the absorber plate and water channels	Partial	Full

2.2.1 Box type PV/T system

Glazing

$$\rho_g \delta_g C_g \frac{dT_g}{dt} = G\alpha_g + (h_{wind} + h_{r,ga})(T_a - T_g) + (h_{cv,cg} + h_{r,cg})(T_c - T_g)$$

Collector plate

$$\rho_c \delta_c C_c \frac{dT_c}{dt} = G(\tau\alpha)_p - E + (h_{cv,cg} + h_{r,cg})(T_g - T_c) + h_{cv,cw} A_w (T_w - T_c) + \frac{T_a - T_c}{R_{in}}$$

$$E = G\tau_g P\eta_e [1 - \phi_c (T_c - 25)]$$

Water in the channel

$$\rho_w A_w C_w \frac{dT_w}{dt} = h_{cv,cw} A_w (T_c - T_w) - \dot{m}_w C_w (T_{w1} - T_{w2})$$

$$T_w - 0.5T_{w2} - 0.5T_{w1} = 0$$

Where, A_z is the total cross sectional flow area and A_w is the total surface area per unit area of collector. T_w is the mean temperature of inlet (T_{w1}) and outlet temperature (T_{w2}) in the channel.

Water in the storage tank

$$M_{tk} C_{tk} \frac{dT_{tk}}{dt} = m_w C_w (T_{tk,i} - T_{tk,0}) + h_{tk} A_{tk} (T_a - T_{tk})$$

Heat transfer coefficients

The convective heat transfer between the cover glass and the ambient with wind speed (u_{wind}) is given by

$$h_{wind} = 2.8 + 3.0u_{wind}$$

The radiative heat transfer coefficient between the front cover and the ambient environment is

$$h_{r,ga} = \epsilon_g \sigma (T_g^2 + T_a^2) (T_g + T_a)$$

The radiative heat transfer coefficient between the front cover and the collector plate is

$$h_{r,cg} = \frac{\sigma (T_g^2 + T_a^2) (T_g + T_a)}{\frac{1}{\epsilon_g} + \frac{1}{\epsilon_c} - 1}$$

The following correlation equation¹⁸⁾ for the Nusselt number can be applied provided that $0 \leq Ra \leq 10^5$ and $0^\circ < \theta < \theta^+$.

$$Nu = 1 + \left[\left(\frac{Ra \cos \theta}{5730} \right)^{1/3} - 1 \right]^* + 1.44 \left[1 - \frac{1708}{Ra \cos \theta} \right]^* \left[1 - \frac{1708 [\sin(1.8\theta)]^{1.6}}{Ra \cos \theta} \right]$$

Where $[\]^*$ in the equation is defined by $[X]^* = (|X| + X)/2$. θ^+ is the critical angle of the collector slope and can be taken as 60° for a maximum error in Nu about 5%, or as 75° for error up to 10%. For a water flow in a rectangular channel at an aspect ratio of 0.5 with uniform heat flux, the flow induced by the thermosyphon effect can be considered as fully developed and laminar in nature¹⁹⁾ in that $Nu = 4.11$.

2.2.2 Tube type PV/T system

Glass

$$M_g C_g \frac{dT_g}{dt} = A_g G \alpha_g + A_g (h_{wind} + h_{r,ga}) (T_a - T_g) + A_g (h_{cv,cg} + h_{r,cg}) (T_p - T_g)$$

PV module

$$M_p C_p \frac{dT_p}{dt} = A_p G (\tau \alpha)_p - A_p E + A_{gp} (h_{cv,cg} + h_{r,cg}) (T_g - T_p) + h_{cl,cp} A_{cp} (T_c - T_p) + h_{cl,pt} A_{pt} (T_t - T_p)$$

Collector plate

$$M_c C_c \frac{dT_c}{dt} = h_{cl,cp} A_{cp} (T_p - T_c) + h_{cl,ct} A_{ct} (T_t - T_c) + h_{cl,ci} A_{ci} (T_i - T_c)$$

Tube Bonding

$$M_t C_t \frac{dT_t}{dt} = h_{cl,ct} A_{ct} (T_c - T_t) + h_{cl,ti} A_{ti} (T_i - T_t) + h_{cv,tw} A_{tw} (T_w - T_t) + h_{cl,pt} A_{pt} (T_p - T_t)$$

Insulation

$$M_i C_i \frac{dT_i}{dt} = h_{al,ci} A_{ci} (T_c - T_i) + h_{al,ti} A_{ti} (T_t - T_i) + h_{cv,ai} A_{ai} (T_a - T_i)$$

Water in the tube

$$M_w C_w \frac{dT_w}{dt} = h_{cv,tw} A_{tw} (T_t - T_w) + \dot{m}_w C_w (T_{w1} - T_{w2})$$

Storage tank

$$M_{tk} C_{tk} \frac{dT_{tk}}{dt} = \dot{m}_w C_w (T_{tk,i} - T_{tk,0}) + h_{tk} A_{tk} (T_a - T_{tk})$$

Efficiency

Electrical efficiency:

$$\eta_e = P \eta_{cell}$$

$$\eta_{cell} = \eta_{ref} [1 - \phi_c (T_p - 25)]$$

Electrical efficiency depends upon the packing factor (P), solar cell efficiency (η_{cell}) and electrical conversion efficiency (η_{ref}) at reference temperature 25°C and temperature coefficient ϕ_c of the solar cell.

Thermal efficiency:

$$\eta_{th} = \frac{\dot{m} C_p (T_{w2} - T_{w1})}{A_c * G(t)}$$

Thermal efficiency depends upon the mass flow rate, specific heat capacity of working fluid, difference between the inlet and outlet temperature of water in collector, absorber area and solar radiation falling in the system at a specified time.

Table 2. Input parameters for simulation

Glazing	Thickness = 0.004 m
	Density = 2,525 kg m ⁻³
	Specific heat capacity = 810 J kg ⁻¹ K ⁻¹
	normal transmissivity = 0.83
	emissivity = 0.88
	extinction coefficient = 26 m ⁻¹
	Total effective area = 1m ²
PV module	Packing factor = 0.9375
	Solar cell temperature coefficient = 0.005 K ⁻¹
	Absorbptivity = 0.8
	Emissivity = 0.8
Thermal collector	Material = Aluminium
	Specific heat capacity = 903 J kg ⁻¹ K ⁻¹
	Thickness = 0.002 m
	Density = 2702 kg m ⁻³
Tube bonding	Mass density = 8960 kg m ⁻³
	Thickness = 0.002 m
	Specific heat = 385 J kg ⁻¹ K ⁻¹
	Density = 2702 kg m ⁻³
	Thermal conductivity = 210 Wm ⁻¹ K ⁻¹
	Bond width = 0.01m
Insulation	Thickness = 0.03 m
	Thermal conductivity = 0.036 Wm ⁻¹ K ⁻¹
	Mass density = 30 kg m ⁻³
Encapsulation	Thickness of EVA = 0.5
	Thermal conductivity = 0.23 W m ⁻¹ K ⁻¹
	Thickness of Tedlar = 0.0001m
	Thermal conductivity = 0.36 W m ⁻¹ K ⁻¹

Input parameters for the simulation of the both PV/T water heating systems are listed in Table 2.

3. Results and Discussion

The simulation developed in Matlab 7.9.0 (R2009b) computer program was used to investigate the performance of both PV/T systems. In the box type system the dimensions of the small channels were

$1 \times 0.02 \times 0.01 \text{ m}^3$ with total 50 numbers of channels. In sheet and tube type the total number of tubes were 5 with diameter of 0.02 m, spacing of 0.2m and length of 1m. All the results were carried out for the typical day of 14th of September, 2010 with the use of the meteorological conditions of Kangwon National University, Chuncheon Korea.

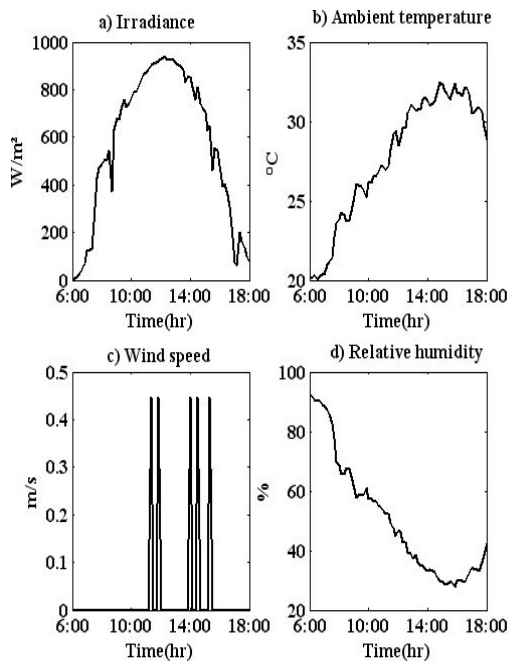


Fig. 3 Meteorological data (a) Solar irradiance (b) Ambient temperature (c) Wind speed (d) Relative humidity

The solar irradiance, ambient temperature, wind speed and relative humidity are shown in Fig. 3. The maximum solar radiation was 934 W m^{-2} and the maximum ambient temperature was 32°C . The solar radiation, wind speed, relative humidity, and air temperature were recorded in the Weather Stations (Watch Dog 2000 Series Spectrum Technologies, Inc. Plainfield, IL, USA). Fig. 4 (b) showed that the collector temperature

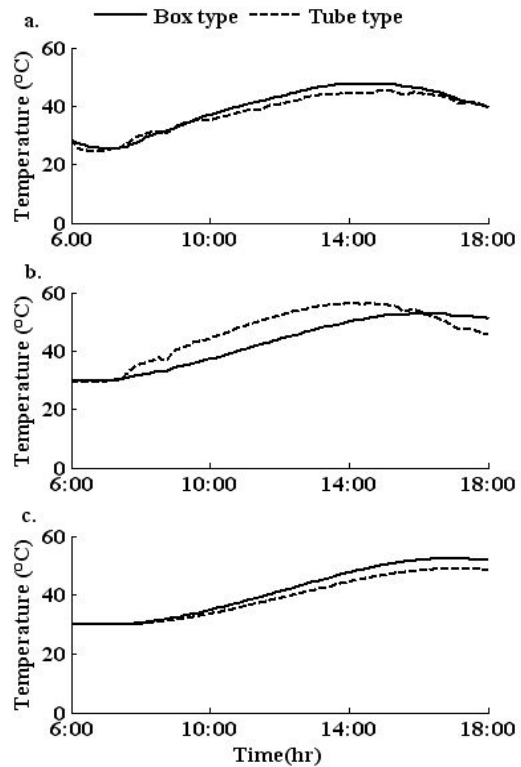


Fig. 4 Calculated temperatures of various layers in tube type and box type collectors (a) glass temperature (b) collector temperature (c) storage tank water temperature.

in tube type system was higher than the box type system. The absorber and water temperature is shown in Fig.4 (c). The temperature difference between the absorber and the water was higher in tube type (7°C), but it was almost same in box type system (0.06°C) (Fig.4 (c)). This showed that there was higher heat transfer from the absorber to the water in the box type and less heat transfer in the tube type system. The reason may be the higher contacting area between the water and the absorber in the box type compared to the tube type system. Due to the less contacting area with the water, tube type absorber temperature was more sensitive

to the fluctuation in solar radiation. The effects of fluctuation of solar radiation on temperature of the tube type absorber could be observed in Fig. 4 (b). After 4 pm, with reduction of solar radiation, the temperature of tube type absorber dropped crossing the temperature of box absorber, whereas in the box type, absorber temperature could be regulated by heat energy stored in water channels (Fig. 4 (b)). The higher PV temperature of tube type system (Fig. 4 b) caused the reduction in cell efficiency (Fig. 5 c). The final temperature of water in the storage tank reached from 30°C to 52°C and 30°C to 48°C (Fig. 4 c) in the box type and the tube type system respectively. The maximum heat gain and cell efficiency were 376W and 14% and 319W and 13% in the box and tube type system respectively (Fig. 5 a and c). The higher performance in the box type system may be due to the improvement in fin efficiency and elimination of metallic bonding between the absorber plate and the tube¹².

3.1 Thermal efficiency

The thermal efficiency of the PV/T systems were shown in Fig. 7. The efficiency was calculated under 800 W/m² solar radiation, 30°C atmospheric temperature and 1 m/s air speed.

The thermal efficiency of the tube type and box type systems were found to be 0.41 and 0.51 respectively, under zero reduced temperature condition (Fig. 7). In previous studies^{3) 11) 16)} the thermal efficiency was found to be greater than 0.5, but in our study for tube type the efficiency was calculated below 0.5.

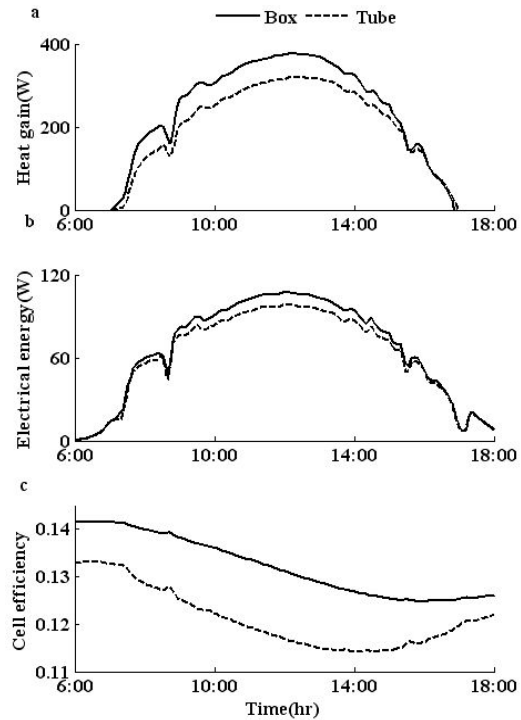


Fig. 5 Variation of (a) heat gain (b) electrical energy (c) cell efficiency in tube type and box type systems with respect to time.

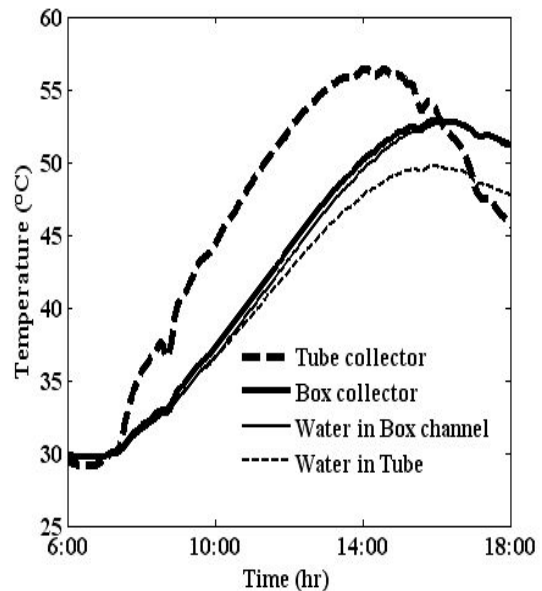


Fig. 6 Water temperature in the collector and absorber temperature of the both PV/T systems.

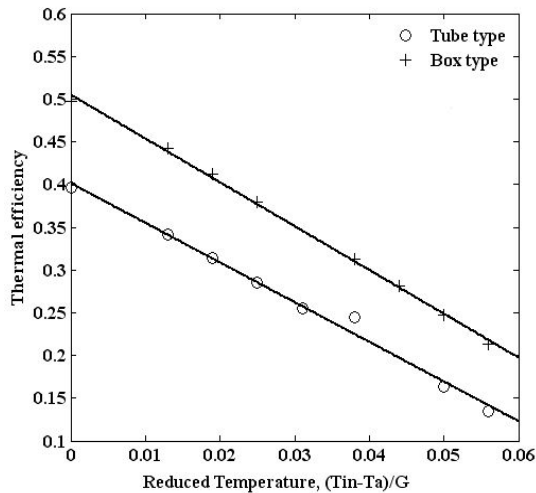


Fig. 7 Thermal efficiency of PV/T systems

The difference between the initial and final temperature of water in the box type and tube type systems were 19°C and 23°C respectively (Fig. 6). The daily thermal efficiency of tube and box type PV/T systems were calculated as 29.5% and 35.8% respectively.

Alternatively, by considering electrical energy as a high grade form of energy gain, the energy efficiency η_f is

$$\eta_f = \frac{\eta_e}{\eta_{power}} + \eta_{th}$$

where, η_{power} is the electric-power generation efficiency of the conventional power plant; its value can be taken as 38%^{6) 20) 21)}. The maximum electrical energy for the box type is 0.141 and that of the tube type is 0.133 (Fig. 5 (c)). The predicted maximum energy efficiency is 0.64 and 0.73 respectively for the tube type and the box type pvt systems. The energy efficiency of the box type system was found higher than that of the tube type system.

4. Conclusions

PV/T systems with the box and tube type flow channels were studied and performance analysis were investigated. The overall performance of the box type PV/T system was found greater than that of tube type system. The thermal efficiency at zero reduced temperature was predicted 0.41 for the tube type, and 0.51 for the box type PV/T system. The higher performance in the box type system may be likely as a result of the improvement in fin efficiency and elimination of metallic bonding between the absorber plate and the tube. Thus, performance of the PV/T system could be enhanced by the use of box type PV/T collector system.

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