

## Effect of H<sub>2</sub> on Formation Behavior of Carbon Nanotubes

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The effect of H<sub>2</sub> gas on the carbon nanotubes (CNTs) synthesis with CO-H<sub>2</sub> gas mixture was investigated using mass measurements and scanning electron microscopy (SEM). The maximum weight and yield of the synthesized carbon were obtained when the mixture ratio of H<sub>2</sub> : CO was 3 : 7 and 9 : 1, respectively. In case of 100% carbon monoxide (CO) without hydrogen (H<sub>2</sub>) addition, the weight of carbon increased, but CNTs were not observed. The CNTs began to be made when the contents of H<sub>2</sub> reaches at least 10%, their structures became more distinct with an increase of H<sub>2</sub> addition, and then the shapes of CNTs were more thin and straight. When the contents of H<sub>2</sub> was 80% (H<sub>2</sub> : CO = 8 : 2), the shapes and growth of CNTs showed an optimal condition. On the other hand, when the contents of H<sub>2</sub> was higher than the critical value, the shapes of CNTs became worse due to transition into inactive surface of catalyst. It was considered that the inactive surface of catalyst resulted from decrease of carbon (C) and H<sub>2</sub> concentration by facilitation of methane (CH<sub>4</sub>) gasification reaction ( $C + 2H_2 \rightarrow CH_4$ ) between C and H<sub>2</sub> gases. It was also found that H<sub>2</sub> addition had an influence considerably on the shape and structure of CNTs.

**Key Words :** H<sub>2</sub>, Carbon nanotubes, Synthesized carbon, Catalyst, Gasification reaction

### Introduction

A great deal of interest has been generated in the carbon nanotubes (CNTs) due to their unique properties.<sup>1,2</sup> Extensive research on the solid carbon formed from decomposition of gaseous phase has been performed due to their various types of shapes and structures.<sup>3,4</sup> Since the discovery of CNTs by Iijima,<sup>5</sup> attention has been focused on the control of shapes and structures in their applications such as efficient field emitters, nano-probes, quantum wire, reinforcing components for composite materials, and methane and hydrogen storages.<sup>6-10</sup>

The deposition of carbon from gaseous phase results in a few different morphologies. The form of the deposited carbon is very important in the practical application.<sup>11</sup> It has been reported that H<sub>2</sub> could play a role in the growth of CNTs and the carbon deposition from carbon monoxide.<sup>12,13</sup> Nolan<sup>14</sup> investigated the dependence of H<sub>2</sub> on Ni catalyst in the growth of nanotubes, and it was agreed with results obtained by Chen *et al.*<sup>15</sup> In the previous study, acetylene, CH<sub>4</sub>, and C<sub>6</sub>H<sub>6</sub> are used as a carbon source<sup>16,17</sup> but the synthesis of CNTs using CO-H<sub>2</sub> gas mixture is still not known well.

The purpose of this research is to investigate the shapes and structures of CNTs with H<sub>2</sub> addition in CO using a cheap iron oxide catalyst, and to provide optimal condition for CNTs synthesis, and to examine possibility of economical efficiency and mass production.

### Experimental Section

The major equipment for a reduction and synthesis of

samples consists of SiC electric tube furnace and a gas flow control system including a gas mixing chamber, an alumina boat, and thermocouples. The detailed experimental apparatus has been described in our previous work.<sup>18</sup> The total Fe content of iron oxide used as catalyst for synthesis of CNTs was approximately 60%. The size distribution of particles was measured using an optical microscope, and the average particle size was found to be 45-65 μm. The iron oxides were sieved using a sieve shaker to obtain a homogeneous size distribution after crushing by ball mill. Before charging samples, N<sub>2</sub> gas with a flow rate of 1.0 L/min at 800 °C was provided into the reactor for 10 min, and the reduction of iron oxide carried out under H<sub>2</sub> gas atmosphere with flow rate of 1.2 L/min for 15 min at 800 °C. The gas mixture, used for CNTs synthesis of metal Fe after reduction, was composed of H<sub>2</sub> and CO gases. The images of the synthesized carbon materials were taken using SEM technique. The experimental conditions are shown in Table 1.

### Results and Discussion

**Optimal reduction condition of catalyst.** The preliminary

**Table 1.** Experimental conditions for reduction and synthesis

Variables	Conditions
Reaction temperature and time	Reduction : 800 °C, 15 min Synthesis : 680 °C, 70 min
Gas flow rate and ratio	Reactor cleaning → N <sub>2</sub> (1.0 L/min) Reduction → H <sub>2</sub> (1.2 L/min) Synthesis → CO+H <sub>2</sub> (1.0 L/min) H <sub>2</sub> /CO = 0-9 → CO (0.3 L/min) H <sub>2</sub> (0.1-2.0 L/min)
Sample charging weight	0.25 g

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experiment was performed to decide optimal reduction condition of catalyst before CNTs synthesis. Figure 1 shows reduction degree of catalyst after reducing under  $H_2$  gas atmosphere with a flow rate of 1.2 L/min for 15 min in the range of 450 to 900 °C. The change in the sample weight was measured and the reduction degree was calculated from Eqs. (1) and (2).

$$RD (\%) = \frac{\Delta W}{[(W_i - d_o)(1 - F_{gm})]} \times 100 \quad (1)$$

$$\Delta W = W_i - W_f \quad (2)$$

where RD (%) is the reduction degree,  $W_i$  is the sample weight (g) before reduction,  $W_f$  is the sample weight (g) after reduction,  $d_o$  is a mass fraction (-) of oxygen in the iron oxide, and  $F_{gm}$  is the mass fraction (-) of gangue in the iron oxide.

In Figure 1, reduction degree gradually increased as reaction temperature increases, but it was little affected by temperature when reaction temperature is higher than 800 °C, and then, sample was reduced completely. Therefore, the experimental condition for reduction determined at 800 °C. The high reduction degree of catalyst before synthesis is an essential condition for high yield of CNTs because low reduction degree means the insufficiency of an active catalyst required to make CNTs.<sup>19</sup>

**Effect of gas ratios in CO- $H_2$  gas mixture.** The gas mixture, for CNTs synthesis of metal Fe after reduction, was composed of  $H_2$  and CO gases. And then, total gas flow rate was kept at 1.0 L/min, they were synthesized at 680 °C with various gas ratios of  $H_2/CO = 0$  to 9. As shown in Figure 2,

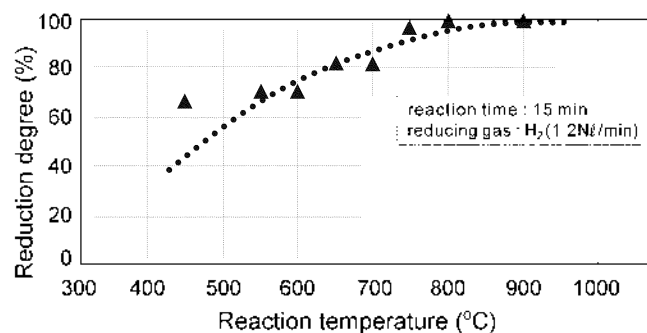


Figure 1. Effect of reaction temperature on reduction degree.

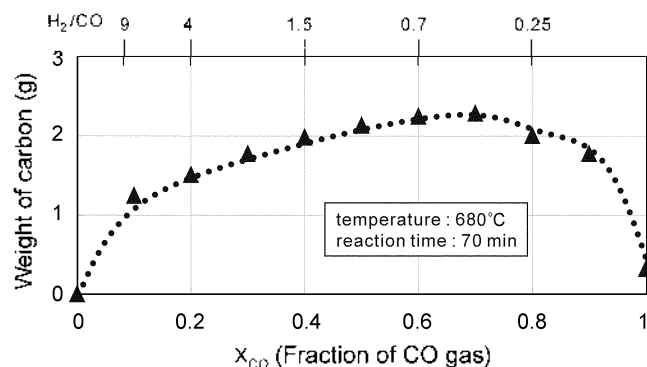


Figure 2. Effect of  $H_2$  addition on synthesis of carbon nanotubes.

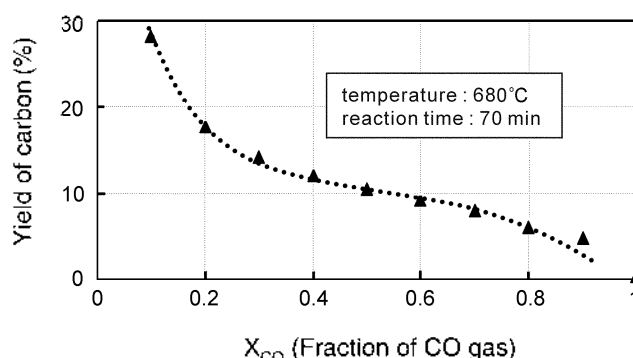


Figure 3. Effect of  $H_2$  addition on synthesis yield of carbon nanotubes.

weight of the synthesized carbon solid was maximum at a gas ratio of  $H_2 : CO = 3 : 7$ , and weight of the synthesized carbon solid using 100% CO was very small as compared with  $H_2$  addition. It was found that  $H_2$  facilitated synthesis reaction of carbon.

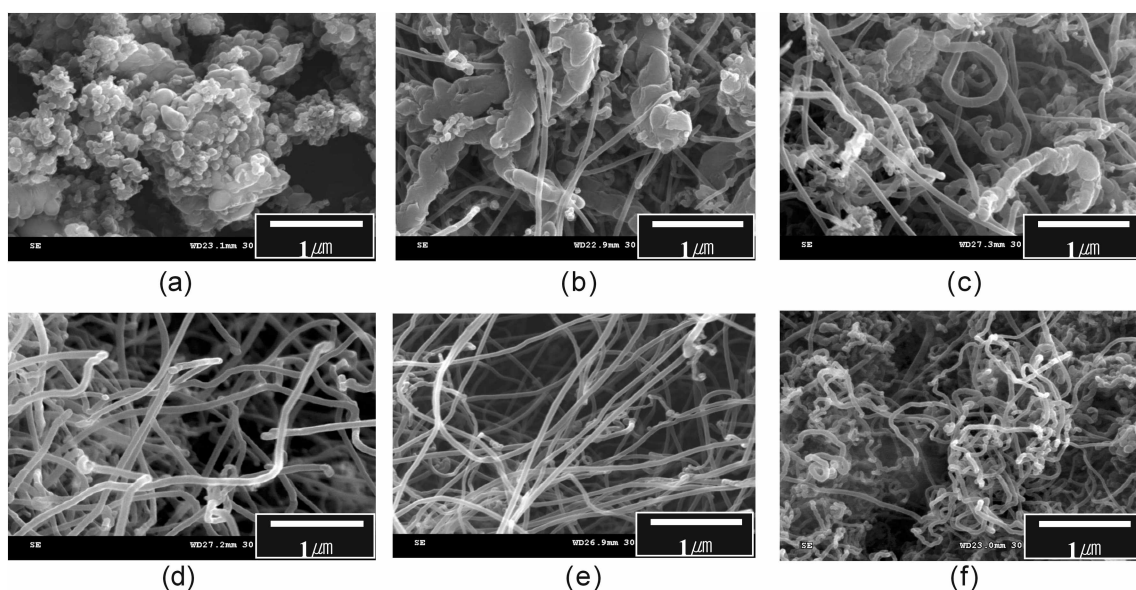
Figure 3 shows yield of synthesized carbon at various gas ratios of CO- $H_2$  gas mixture. The yield was maximum value at a gas ratio of  $H_2 : CO = 9 : 1$ , and its value decreased with an increase of CO gas. The yield value was calculated by Eq. (3) as follows;

$$\text{yield} (\%) = \frac{\text{obtained carbon weight (g)}}{\text{supplied carbon weight (g)}} \times 100 \quad (3)$$

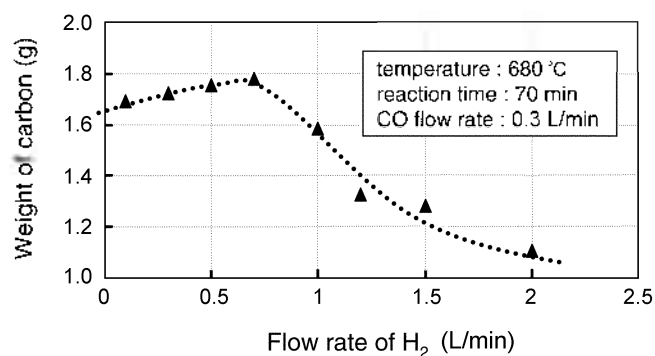
From these results, it was also found that  $H_2$  gas was a major parameter in the synthesis of CNTs and carbon deposition reaction ( $2CO \rightarrow C + CO_2$ ) by decomposition of CO gas.<sup>20</sup> Owing to conversion to active catalyst from inactive catalyst by  $H_2$  addition, the formation of CNTs can be accelerated.<sup>21,22</sup>

Figure 4 shows SEM morphologies of CNTs after synthesis at various gas ratios. In case of 100% CO without  $H_2$  addition ( $H_2 : CO = 0 : 1$ ), as shown in Figure 4(a), CNTs were not observed. It is considered that carbon is not grown to CNTs due to existence of inactive catalyst by insufficiency of  $H_2$  gas, they are precipitated to the amorphous carbon.<sup>23</sup> The CNTs were formed with 10%  $H_2$  addition ( $H_2 : CO = 1 : 9$ ), and their shapes and structures were more distinct as  $H_2$  gas increases. Especially, when the mixture ratio of  $H_2 : CO$  was higher than 6 : 4, the amorphous carbon was completely disappeared, and then, the shapes of CNTs were more thin and straight. When the contents of  $H_2$  gas was 80% ( $H_2 : CO = 8 : 2$ ), the shapes and growth of CNTs showed the optimal condition. On the other hand, when the contents of  $H_2$  were higher than the critical value (over 80%  $H_2$ ), the shapes of CNTs became worse due to transition into inactive surface of catalyst. It was considered that an inactive surface of catalyst was resulted from decrease of C and  $H_2$  concentration by methane ( $CH_4$ ) gasification reaction ( $C + 2H_2 \rightarrow CH_4$ ) between C and  $H_2$  gases. It was also found that  $H_2$  played a major role in the growth of CNTs.

**Effect of  $H_2$  flow rate.** To investigate the effect of a flow

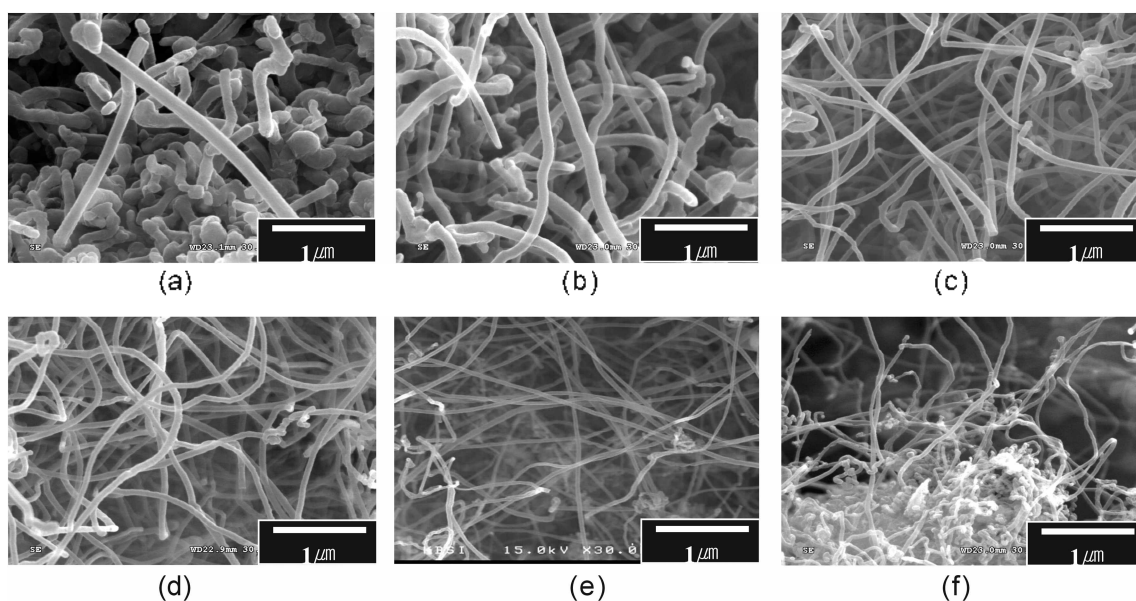


**Figure 4.** SEM morphologies of catalyst after synthesis at 680 °C with various gas ratios of H<sub>2</sub> : CO; (a) 0 : 1, (b) 1 : 9, (c) 5 : 5, (d) 6 : 4, (e) 8 : 2, and (f) 9 : 1, respectively.



**Figure 5.** Effect of H<sub>2</sub> gas flow rate on synthesis of carbon nanotubes.

rate of H<sub>2</sub>, the flow rate of CO was kept at 0.3 L/min, and metal catalysts were synthesized at 640 °C with various H<sub>2</sub> gas flow rates of 0.1 to 2.0 L/min. The images of the synthesized carbon materials were observed using SEM. As shown in Figure 5, the synthesized carbon weight increased with H<sub>2</sub> addition, and the value showed maximum in the H<sub>2</sub> gas with a flow rate of 0.7 L/min. When H<sub>2</sub> value was higher than 0.7 L/min, it decreased as H<sub>2</sub> contents increase. The synthesized weight was rapidly decreased in the H<sub>2</sub> gas with a flow rate of 2.0 L/min. Therefore, H<sub>2</sub> plays an important role in the growth and synthesis of CNTs. This result agreed with SEM analysis in Figure 4. From these results, to decide optimal content of H<sub>2</sub> addition is very important in the CNTs



**Figure 6.** SEM morphologies of catalyst after synthesis at 680 °C with CO gas of 0.3 L/min at various flow rates of H<sub>2</sub>; (a) 0.1 L/min, (b) 0.3 L/min, (c) 0.5 L/min, (d) 1.0 L/min, (e) 1.2 L/min, and (f) 1.5 L/min, respectively.

production because of consideration of the quality and economic efficiency by the excellent yield rate.

Figure 6 shows SEM images of metal catalyst after synthesis with various ratios of CO-H<sub>2</sub> gas mixture. As H<sub>2</sub> addition increases, the shapes of CNTs became a straight from spiral and more thin in the diameter. However, when H<sub>2</sub> contents were more than critical value (H<sub>2</sub>; 1.5 L/min), the growth of CNTs was so repressed. It was also found that H<sub>2</sub> addition had an influence considerably on the shape and structure of CNTs.

### Conclusions

The effect of H<sub>2</sub> addition on the CNTs synthesis was intensively investigated by SEM characterization. The weight of the synthesized carbon solid was maximum in a gas ratio of H<sub>2</sub> : CO = 3 : 7. The yield of synthesized carbon was maximum value at H<sub>2</sub> : CO = 9 : 1. In case of 100% CO gas without H<sub>2</sub> addition, CNTs were not observed. It is considered that carbons are not grown to CNTs due to existence of inactive catalyst by insufficiency of H<sub>2</sub> gas, finally these are precipitated to the amorphous carbon. The CNTs were formed with 10% H<sub>2</sub> addition, their shapes and structures were more thin and straight with an increase of H<sub>2</sub> gas. When the contents of H<sub>2</sub> gas was 80% (H<sub>2</sub> : CO = 8 : 2), the shapes and growth of CNTs showed the optimal condition. With an increase of H<sub>2</sub> contents, CNTs were obviously grown, and their shapes became a straight from spiral and more thin in the diameter. However, when H<sub>2</sub> contents were more than critical value, it acted as a barrier on the growth of CNTs.

From these results, to decide optimal content of H<sub>2</sub> addition is very important in the CNTs production because of consideration of the quality and economics efficiency by

the excellent yield rate. It was also found that H<sub>2</sub> gas was a major factor in the shape and growth of CNTs.

### References

1. Wilddoer, J. W. G.; Venema, L. C.; Rinzler, A. G.; Smalley, R. E.; Dekker, C. *Nature* **1998**, *391*, 59.
2. White, C. T.; Todorov, T. N. *Nature* **1998**, *391*, 59.
3. Baker, R. K.; Harris, P. S. *Chemistry and Physics of Carbon*. New York, 1978; pp 83-87.
4. Audier, M.; Coulon, M. *Carbon* **1985**, *23*, 317.
5. Ijima, S. *Nature* **1991**, *354*, 56.
6. Qian, D.; Dickey, E. C.; Andrews, R.; Rantell, T. *Appl. Phys. Lett.* **2000**, *76*, 2868.
7. Chen, P.; Wu, X.; Lin, J.; Tan, K. L. *Science* **1999**, *285*, 91.
8. Trans, S. J.; Verschuere, A. R. M.; Dekker, C. *Nature* **1998**, *393*, 49.
9. Saito, Y.; Hamaguchi, K.; Hata, K.; Uchida, K. **1997**, *389*, 554.
10. Dai, H. J.; Hafner, J. H.; Rinzler, A. G.; Colbert, D. T.; Smalley, R. E. *Nature* **1996**, *384*, 147.
11. Rodriguez, N. M. *J. Mater. Res.* **1993**, *8*, 3233.
12. Yan, H.; Li, Q.; Zhang, J.; Liu, Z. *Chem. Phys. Lett.* **2003**, *380*, 347.
13. Pinheiro, P.; Schouler, M. C.; Gadelle, P.; Mermoux, M.; Dooryhee, E. *Carbon* **2000**, *38*, 1469.
14. Nolan, P. E. *PhD Thesis, Hydrogen Control of Catalytic Carbon Deposition*. University of Arizona, USA, 1995.
15. Chen, P.; Zhang, H. B.; Lin, G. D.; Hong, Q.; Tsai, K. R. *Carbon* **1997**, *35*, 1495.
16. Hernadi, K.; Fonseca, A.; Nagy, J. B.; Bernaerts, D.; Lucas, A. A. *Carbon* **1996**, *34*, 1249.
17. Toan, L. Q.; Schouler, M. C.; Garden, J.; Gadelle, P. *Carbon* **1999**, *37*, 505.
18. Hwang, H. S.; Chung, U. C. *Met. & Mater. Int.* **2004**, *10*, 77.
19. Yongdan, L. *Applied Catalysis A* **1997**, *163*, 45.
20. Park, C.; Baker, R. T. K. *J. Catalysis* **1998**, *179*, 361.
21. Charanjeet, S.; Milo, S. P.; Alan, H. W. *Carbon* **2003**, *41*, 359.
22. Lijie, C.; Jinqun, W., *et al.* *Carbon* **2001**, *39*, 329.
23. Krishnankutty, N., *et al.* *J. Catalysis* **1996**, *158*, 217.