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1.

(Dakin

가 1968, De Bruin and Keeney 1969).

Chavalley(1975 and 1991)

, Wilson (1993)

(McMaster and others 1987).

Lees(1973)

가

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가

가

가

(premix)

가

. DeBruin and Keeney (1973)

가

(SEM)

, Heathcock (1985)

2.

Table 1. Combination of water, sugar, chocolate and peanut meal mixtures

2.1.

(Hershey's unsweetened baking chocolate), (peanut meal)

	Components (%)				Sample I.D.
	Water	Sugar	Chocolate	Peanut meal	
	30	50	20	0	W30 S50 C20
	30	45	25	0	W30 S45 C25
	30	40	30	0	W30 S40 C30
	30	35	35	0	W30 S35 C35
2.2.	30	70	0	0	W30 S70
	55	0	45	0	W30 C45
(Partially defatted peanut) (Thomas-Wiley Laboratory Mill Model 4, Philadelphia, PA) 가	30	65	0	5	W30 S65 P5
	30	60	0	10	W30 S60 P10
	30	55	0	15	W30 S55 P15
	30	50	0	20	W30 S50 P20
2000 um 가	60	0	25	15	W60 C25 P15
(Model M-MS3, Morehouse Industries, Anaheim, CA) 2	60	0	27.5	12.5	W60 C27.5 P12.5
	60	0	30	10	W60 C30 P10
, 1 127 μm	60	0	32.5	7.5	W60 C32.5 P7.5
	60	0	35	5	W60 C35 P5
76.2 μm	60	0	40	0	W60 C40
	50	20	10	20	W50 S20 C10 P20
5.77%	50	20	15	15	W50 S20 C15 P15
	50	20	20	10	W50 S20 C20 P10
	50	20	25	5	W50 S20 C25 P5

2.3.

0.5% , 0.5% (95%) , 0.5% 60 10 가 3가 Malvern Mastersizer (Malvern Instruments, Inc., Southborough, MA) . Volume mean diameter (D[4,3]) mass median diameter(D(V,0.5))가 (Devaux and others 1998).

630 nm

2.5.

Table 1

가

가

hand mixing

가

20

2.4.

perchloric acid (Nakamura and Suzuki 1977). 52% perchloric acid glucose 가 glucose 0.2% anthrone

2.6.

behavior index)

, , (flow 40, 50, 60

Brookfield Viscometer(Programmable DV-II model, Brookfield Engineering Laboratories Inc., Stoughten, MA)

circulator(RTE- 100, NESLAB Instruments Inc., Newington, NH)

10 15 가 spindle No.31 small sample adapter

(consistency index), (true shear rate), (shear stress), (apparent viscosity)

Rao and Webb (1988)

(low true shear rate, <100 s⁻¹) (Chevalley 1975, Chevalley 1991, Wilson and others 1993).

(consistency indexes, η) (activation energy, E_a)

Arrhenius equation (Ibanoglu and Ibanoglu 1999).

$$\eta = \eta_0 \exp(-E_a/RT)$$

η_0 = (an apparent viscosity index at a reference temperature, $T =$), E_a = (activation energy for flow), $R =$ (universal gas constant, 8.314 J/mol.K), $T =$ (absolute temperature).

3.

3.1.

0.5% volume mean diameter mass median diameter 80.19 55.00 μm . 0.5% 95% volume mean diameter mass median diameter 78.50 56.13 μm , 0.5% 가 volume mean

diameter mass median diameter가 61.97 40.69 μm 가 가

3.2.

5.13 8.10%

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3.3. , ,

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(Fig. 1, 2, 3). W30 S70

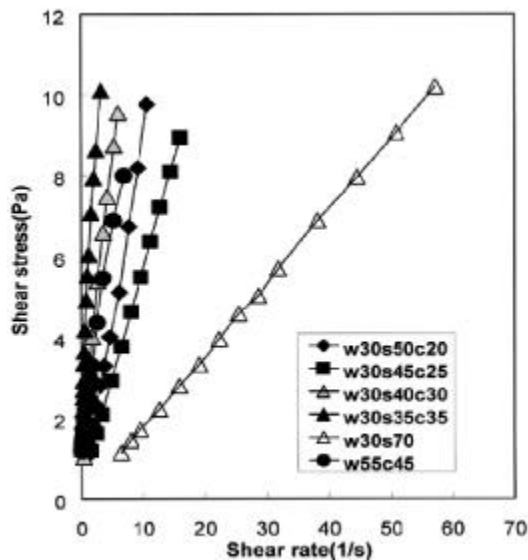


Fig. 1. Plot of shear stress vs true shear rate of water, sugar and chocolate mixtures at 40

Table 2. Effect of temperature(K) on $\ln\eta_0$ (Pa.sⁿ) of water, sugar and chocolate mixtures

1/K	Shear* rate(s ⁻¹)	$\ln\eta_0$					
		W30S50C20	W30S45C25	W30S40C30	W30S35C35	W30S70	W30C45
		11.8440	16.9200	4.0608	0.4061	47.3759	6.7680
0.0030		-1.2050	-1.2331	0.8748	2.9081	-2.7272	-0.0071
0.0031		-0.8079	-0.9444	0.2081	2.7883	-2.3167	0.0479
0.0032		0.1936	-0.6390	0.6109	2.1959	-1.7850	0.1648

* Constant shear rate at which η_0 is estimated

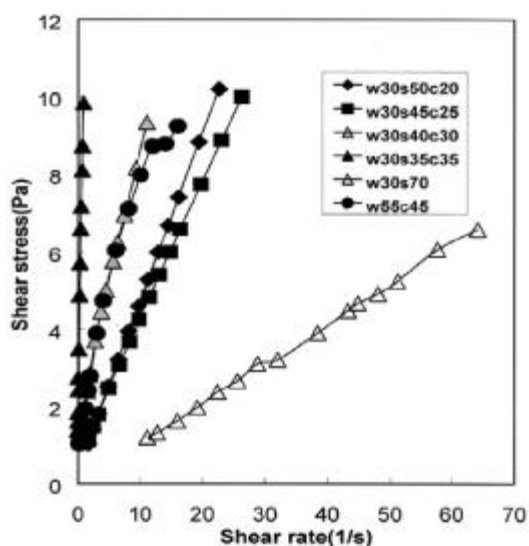


Fig. 2. Plot of shear stress vs true shear rate of water, sugar and chocolate mixtures at 50

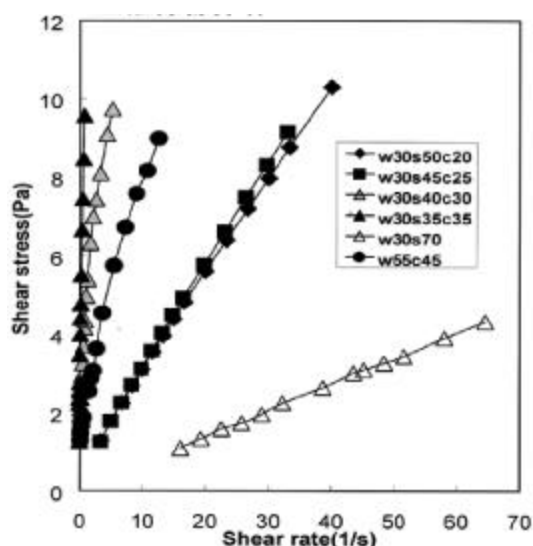


Fig. 3. Plot of shear stress vs true shear rate of water, sugar and chocolate mixtures at 60

Table 3. Activation energy (E_a) and Arrhenius constant (η_0) of water, sugar and chocolate mixtures

Mixture	E_a (KJ/mole.K)	η_0 (Pa.s ⁿ)
W30 S50 C20	42.044	0.000
W30 S45 C25	24.697	0.000
W30 S40 C30	-10.970	105.109
W30 S35 C35	-29.606	864580.762
W30 S70	39.167	0.000
W30 C45	7.146	0.075

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W55 C45 W30 S40 C30
(Fig. 2).
1
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가 가
25%
(+) 가 가

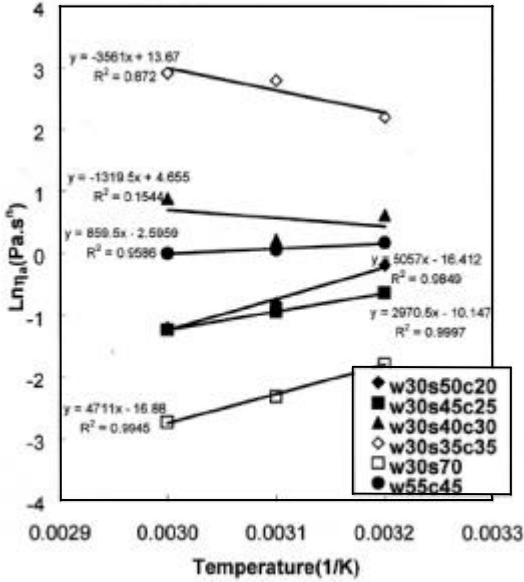


Fig. 4. Effect of temperature on apparent viscosity of water, sugar and chocolate mixtures

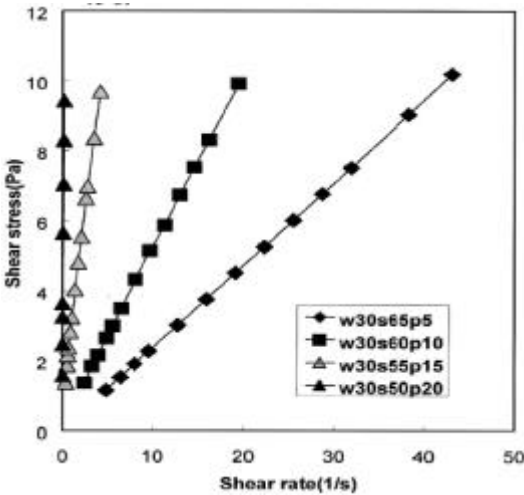


Fig. 5. Plot of shear stress vs true shear rate of water, sugar and peanut meal mixtures at 40

가
(Table 3). 30%
(-)

Table 4. Effect of temperature(K) on $\ln\eta_a$ (Pa.sⁿ) of water, sugar and peanut meal mixtures

1/K	$\ln\eta_a$				
	Shear* rate(s ⁻¹)	w30s65p5	w30s60p10	w30s55p15	w30s50p20
		45.6839	20.3040	4.0608	0.1692
0.0030		-2.1928	-1.5362	0.3106	3.4234
0.0031		-1.8585	-1.1530	0.6068	3.8282
0.0032		-1.4992	-0.7172	0.8697	4.0206

* Constant shear rate at which η_a is estimated

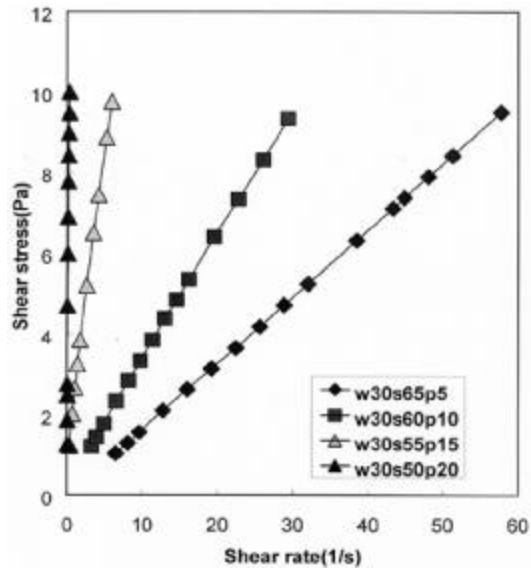


Fig. 6. Plot of shear stress vs true shear rate of water, sugar and peanut meal mixtures at 50

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(Fig. 4, Table 2).

3.4. , ,

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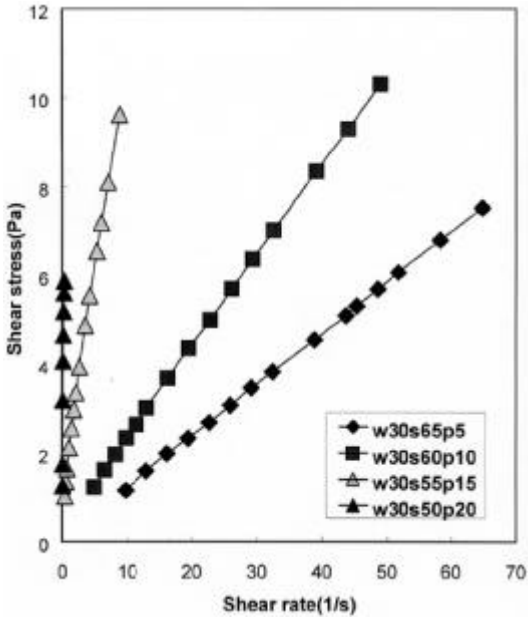


Fig. 7. Plot of shear stress vs true shear rate of water, sugar and peanut meal mixtures at 60

Table 5. Activation energy(E_a) and Arrhenius constant(η_0) of water, sugar and peanut meal mixtures

Mixture	E_a (KJ/mole.K)	η_0 (Pa.s ⁰)
W30 S65 P5	28.833	0.000
W30 S60 P10	34.046	0.000
W30 S55 P15	23.242	0.000
W30 S50 P20	24.826	0.004

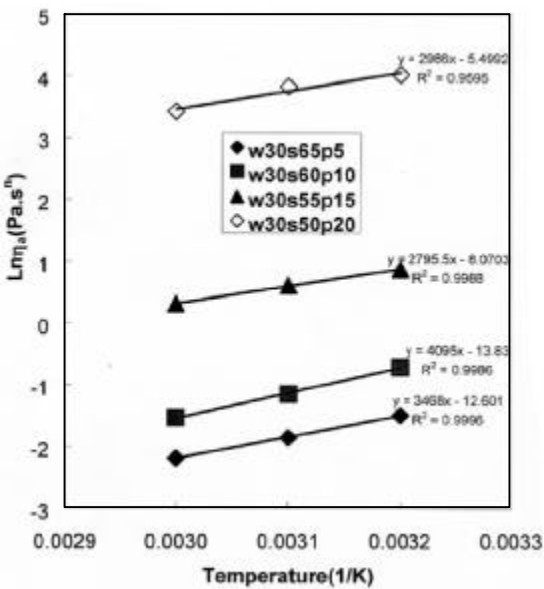


Fig. 8. Effect of temperature on apparent viscosity of water, sugar and peanut meal mixtures

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 (Fig. 5, 6, 7). W30 S65 P5
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 가 (+)
 (Table 5), 가 가
 (Fig. 8, Table 4).

3.5. , ,

Fig. 9, 10, 11
 가 가
 W60 C40
 5- 15%
 5%
 35%
 가 가 (-)
 가 가 (Fig. 12,
 Table 6). 35%

Table 6. Effect of temperature(K) on $\ln\eta_e$ (Pa.sⁿ) of water, chocolate and peanut meal mixtures

1/K	$\ln\eta_e$						
	Shear* rate(s-1)	W60C40	W60C35P5	W60C32.5P7.5	W60C30P10	W60C27.5P12.5	W60C25P15
		40.6079	10.1520	10.1520	5.7528	5.0760	4.0608
0.0030		-1.7339	-0.0920	-0.1350	0.3508	0.3468	0.3736
0.0031		-2.0843	-0.1954	-0.0748	0.4021	0.4941	0.4902
0.0032		-2.1103	-0.2623	-0.0343	0.5509	0.6140	0.8319

* Constant shear rate at which η_e is estimated

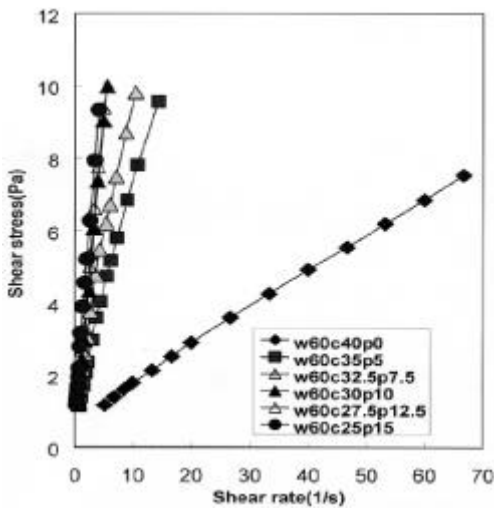


Fig. 9. Plot of shear stress vs true shear rate of water, chocolate and peanut meal mixtures at 40

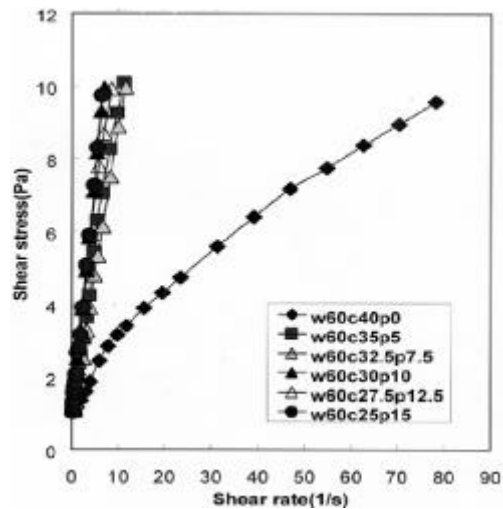


Fig. 11. Plot of shear stress vs true shear rate of water, chocolate and peanut meal mixtures at 60

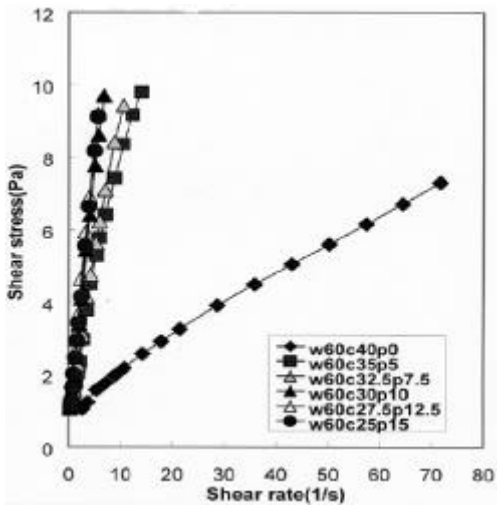


Fig. 10. Plot of shear stress vs true shear rate of water, chocolate and peanut meal mixtures at 50

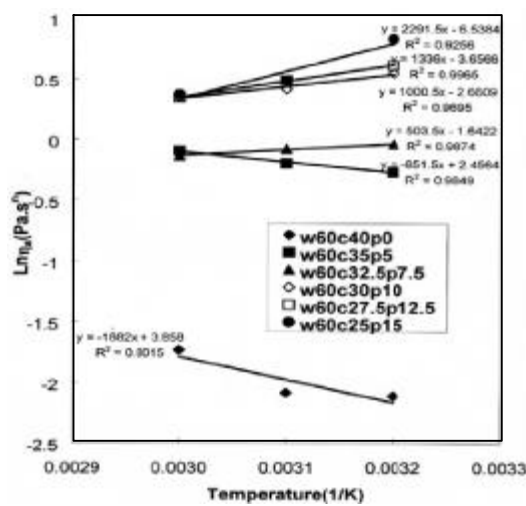


Fig. 12. Effect of temperature on apparent viscosity of water, chocolate and peanut meal mixtures

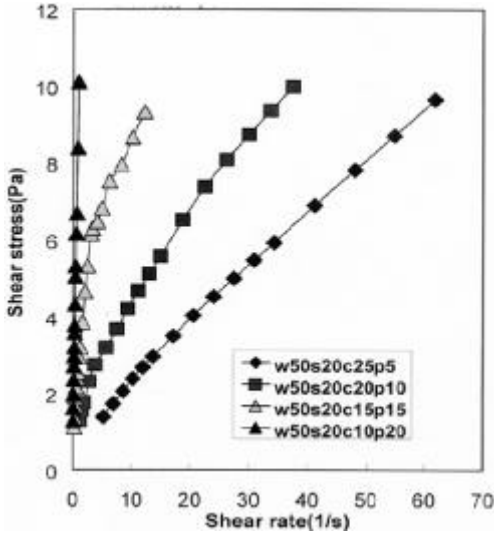


Fig. 13. Plot of shear stress vs true shear rate of water, sugar, chocolate and peanut meal mixtures at 40

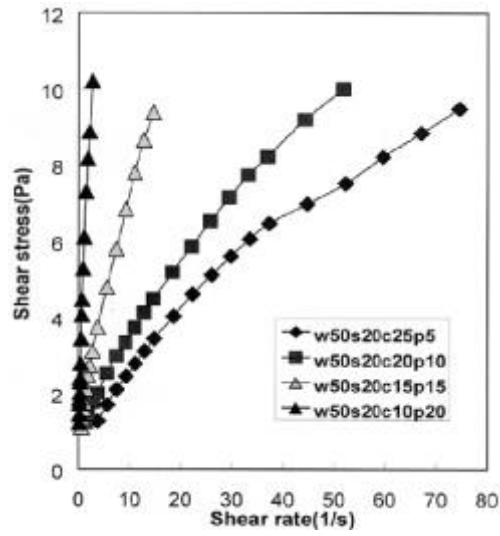


Fig. 15. Plot of shear stress vs true shear rate of water, sugar, chocolate and peanut meal mixtures at 60

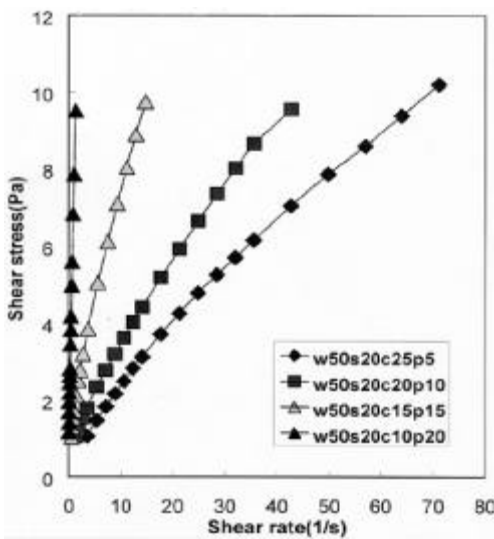


Fig. 14. Plot of shear stress vs true shear rate of water, sugar, chocolate and peanut meal mixtures at 50

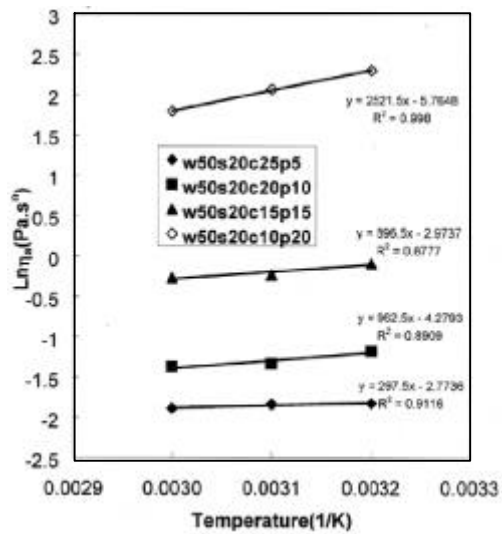


Fig. 16. Effect of temperature on apparent viscosity of water, sugar, chocolate and peanut meal mixtures

3.6. , , ,

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가 가

(Fig. 13)

14, 15). 가 가 50 60 가 가
 가 , 가 40 s⁻¹ 가 가
 (가) W50 S20 C25 P5 , 40 s⁻¹ 가
 가 40 50 가
 가 가 가

Table 7. Activation energy(E_a) and Arrhenius constant(η₀) of water, chocolate and peanut meal mixtures

Mixture	E _a (KJ/mole.K)	η ₀ (Pa.s ⁿ)
W60 C40	- 15.646	47.371
W60 C35 P5	-7.075	11.663
W60 C32.5 P7.5	4.186	0.194
W60 C30 P10	8.318	0.070
W60 C27.5 P12.	11.107	0.026
W60 C25 P15	19.051	0.001

Table 8. Effect of temperature(K) on lnη₀ (Pa.sⁿ) of water, sugar, chocolate and peanut meal mixtures

1/K	Lnη ₀			
	Shear* rate (s ⁻¹)	W50S20C25P5	W50S20C10P10	W50S20C15P15
	54.1439	30.4559	10.1520	1.0152
0.0030	-1.8865	-1.3724	-0.2649	1.7932
0.0031	-1.8407	-1.3345	-0.2332	2.0647
0.0032	-1.8270	-1.1799	-0.0856	2.2975

* Constant shear rate at which η₀ is estimated

Table 9. Activation energy(E_a) and Arrhenius constant(η₀) of water, sugar, chocolate and peanut meal mixtures

Mixture	E _a (KJ/mole.K)	η ₀ (Pa.s ⁿ)
W50S20C25P5	2.473	0.062
W50S20C20P10	8.002	0.014
W50S20C15P15	7.454	0.051
W50S20C10P20	20.964	0.003

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 (Table 8), 가 가
 가 (Fig. 16, Table 9).

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