

합성윤활유 및 첨가제 관련 특허정보 분석

(I)

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개 요

합성윤활유와 윤활유 첨가제의 생산과 응용에 관련된 각종 특허정보를 몇가지 주요 분야로 나누어서 분석하였다. 본고에서 수집, 분석된 특허정보는 다음과 같다. 합성윤활유 부문

- A. LINEAR ALPHA OLEFIN OLIGOMERS(PAO)
- B. NEOPOLYOL ESTERS
- C. DIBASIC ACID ESTERS

윤활유 첨가제 부문

- A. POLYALKENYL SUCCINIMIDE
- B. ZINC DIHYDROCARBYLDITHIOPHO-SPHATES
- C. SULFONATES
- D. ETHYLENE PROPYLENE COPOLY-MERS
- E. ALKYLPHENATES

본고에서 분석된 특허정보가 윤활유 생산 및 응용 등의 연구개발에 관계하는 분들에 게 조금이나마 도움이 되었으면 한다.

Ⅰ. 합성윤활유 특허정보 분석

A. LINEAR ALPHA OLEFIN OLIGOMERS(PAO)

Monomer(s)	Catalyst	D .: 0 11.:	
		Reaction Conditions	Hydrogenation
AO ≥ 3C	(1) Alkyl aluminum halide(2) Organic halide	Continuous high reaction rates without cooling; no solvent.	Not shown.
st for oligomerizin	ng olefins for lubricant produc	ction.	
AO, such as -decene	(1) BF ₃ (2) Promoter such as n-butanol	Not shown.	Special procedure to give desired introduction of desired methyl and ethyl groups onto trimer chains. Unsaturated oligomer is trickled down hydrogenation column. 600 psi and 200°C
	AO, such as decene	st for oligomerizing olefins for lubricant production. AO, such as (1) BF ₃ decene (2) Promoter such as n-	solvent. st for oligomerizing olefins for lubricant production. AO, such as (1) BF ₃ Not shown. decene (2) Promoter such as n- butanol

Assignee	Monomer(s)	igomerization	Position Carditions	Under
		Catalyst	Reaction Conditions	Hydrogenation
Gulf	LAO, such as 1-decene	(1) BF ₃ (2) Promoter such as decanol	2-stage continuous. Tank reactor in first stage and a tube reactor in the second stage. Example had 110°F in first reactor and 120°F in tube reactor; both at 50 psig.	Conventional catalysts such as Pd, Pt, Ni with elevated temperatures and pressure.
Method of r	naking alpha olefin o	oligomers.		
Gulf	LAO, such as 1-decene	(1) BF ₃ (2) Promoter such as n-butanol	Multi-stage continuous. Tank reactors in series. Example had two reactors. 120°-130°F, and 50 psig in both reactors.	Conventional catalysts such as Pd, Pt, Ni with elevated temperature and pressure.
Method of o	ligomerizing 1-olefi	ns.		
Uniroyal	LAO, ≥ 3C	(1) Alkyl aluminum halide (2) Organic halide	Continuous. High reaction rates without cooling; no solvent. 40-60 min, 23°-152°C.	Optional, for added thermal oxidative stability.
Oligomeriza hydraulic oi	tion catalyst contain ls.	ning aluminum alkyl halide a	and organic halide for conver	rting olefins to lubricants and
Oil	LAO, ≥ 6C oil preparation using	(1) Multivalent alcohol derivative. (2) Aluminum halide. Catalyst may be used repeatedly for further oligomerization (a catalyst derived from alumetrical content of the	Example showed 5hrs and 120°C	Not shown.
Exxon	LAO, preferably 10-14 C atoms	Alumino-silicate molecular sieve	One representative, set of conditions is 600°F, 600 psig and 1 hr residence time.	Conventional hydrofinishing conditions employing conventional catalysts such as Ni and cobalt molybdate. Example showed 500°F, 800 psi hydrogen and 1 hr with 5% Ni catalyst.
Uniroyal Oligomeriza lubricating	LAO, $\geq 3C$ tion of alpha olefins oils.	(2) Organic halide.	Example showed 120°C and 30 minutes. ning aluminum alkyl halide, u	
Liquichi- mica S.P.A Synthetic lu	C ₆₋₂₄ n-olefins	Friedel-Crafts(NaAl Cl ₄ used in example)	Example showed 130°C and 2.5 hrs.	Example showed 10% Rane Nickel catalyst 200°F and 50 atm for 4 hrs.
Mobil oil	C ₆₋₁₂ alpha olefins	(1) BF ₃ in presence of water or alcohol Promoter. (2) Low boiling ester of	Examples showed 15° to 50°C and 104 to 205 minutes.	Mentioned but not described.

Assignee	Monomer(s)	Catalyst	Reaction Conditions	Hydrogenation
Oil	Olefin or olefin mix- ture having > 6C atoms	 Polyhydric alcohol derivative. Aluminum halide. Metallic aluminum powder. oligomer. 	Examples showed 100°C for 5 hrs.	Raney nickel catalyst, 10 kg/cm hydrogen pressure, 150°C, 3 hrs. Catalyst is used 10 times.
Lion Fat &	LAO, ≥ 6C	(1) Polyhydric alcohol	Examples showed 5 hrs	Raney nickel catalyst,
Oil		derivative having all hydrogen atoms of hydroxyl groups replaced by acyl groups and alkyl groups, both groups having 1 to 20 carbon atoms. (2) Aluminum halide.	and 100°-130℃.	10kg/cm hydrogen pressure, 150°C, 3 hrs.
Stauffer Synthetic lu ture of trim	TMP bricants, based on a eric and tetrameric o	Heptanoic acid mixture of liquid neopolyol e lecene-1), plus additives.	Not given. ster and a liquid alpha-olefir	n oligomer (hydrogenated mix
Lion Fat & Oil		(1) Aluminum chloride(2) Ketone having 4 or more carbon atoms.(3) Olefin catalyst constituent.	Examples showed 100°C and 6 hrs.	Raney nickel catalyst, 70kg/cm hydrogen pres- sure, 150°C, 3 hrs.
Method for	preparation of hydro	(4) Ester, ether, or alcohol. carbon liquid polymers.		
Lion Fat & Oil	Olefins having 6 or more carbon atoms	 Polyhydric alcohol completely substituted with 1-20 acyl and/or alkyl groups. Aluminum halides. 	Examples showed 100°C and 5 hrs.	Raney nickel catalyst, 150°C, 3 hrs.
Preparation	of olefin oligomers i	n presence of aluminum halid	e and esterified polyhydric a	lcohol.
Uniroyal	LAO, \geq 3C	(1) Alkyl aluminum halide.		Not shown.
Alpha-olefi ing oligomer	n oligomerization cars used as lubricants	(2) Organo-halide compound talyst system comprising alky and hydraulic fluids.		no-aluminum compounds, gi
Lion Fat & Oil	LAO having 8-10 (atoms	C(1) Titanium halide and not less than 1 alkyl Al compound. (2) A teritary catalyst formed from an alkali metal hydride, Al halide and Ti halide.	Examples with $EtAICI_2+$ TiCI ₄ , 20° ~40°C, 4 hrs Example with $AICI_3+$ Lihalide 100°-120°C, 4 hrs.	Raney nickel catalyst 150°C, 20kg/cm hydrogen pressure.
Polyolefin-l	pased lubricating oils	with reduced viscosity at low	v temperatures, derived from	8-10 C olefin mixtures.
Lion Fat & Oil	Alpha olefins having 6-14 C atoms	 (1) Alkali metal hydride. (2) Boron or aluminum halide. (3) Titanium halide. Above 3 items for ternary catalyst. A quaternary catalyst may be used having (4) Metallic lithium or sodiun 	70° – 200°C	Raney nickel catalyst.

	Monomer(s)	gomerization		
	monomor (6)	Catalyst	Reaction Conditions	Hydrogenation
	LAO having 6-12 C atoms	 (1) Anhydrous aluminum chloride modified with a nitro paraffin. (2) TiCl₄ can also be included and can be replaced by dibutyl or tributyl tin chloride. 	180° – 250° F appears to be most desirable temper- ature range.	Raney nickel catalyst preferred;50–2500 psig hydrogen pressure. 250°-500° F, 4-24 hrs.
Polymerization	on process.			
etti (LAO having 4-18 C atoms	 (1) Compound of a transition metal from the IV to VIII Group of the Periodic Table plus two coordinated anionic co-catalysts. (2) Aluminum compound of an inorganic nature. (3) Aluminum compound of the conventional Ziegler type. 	for 5 hrs.	Pd on alumina catalyst, 220°C, 80kg/cm hydrogen pressure, 5 hrs.
Production o	of synthetic lubrican	ts from alpha-olefins through	a ternary catalytic system.	
į	C ₁₆ · 1-Decene in preferred	(1) ${\rm BF_3}$ (2) Water promoter. normal alpha-olefin oligomer	Batch. BF ₃ in molar excess of water. 0-500 psig, 10°-60°C, 1-4 hrs.	Pt or Pd on charcoal, Raney nickel, nickel on kieselguhr, copper, chromite alumina-supported copper and palladium. 100-2000 psig, 150°-200°C.
!	LAO, such as C ₆ - C ₁₆ · 1-Decene is preferred	(1) BF ₃ (2) Alcohol promoter	Batch. BF ₃ in molar excess of alcohol. 0-500 psig, 10°-60°C, 1-4 hrs.	Same as above.
Synthetic lub	oricants by oligomer	ization and hydrogenation.		
	LAO having 6-12 C atoms	Alkali metal tetra- haloalanate	Examples showed 125°-150°C from 110 minutes to 4 hrs.	Nickel on kieselguhr catalyst, 200°C, 1500 psig hydrogen pressure, 8 hrs.
Synthetic oils	s from alpha-olefns			
	LAO having 4-18 C atoms	(1) Compound of a transition metal from the IV to VII Group of the Periodic Table.	Examples showed 80° C. and 3 hrs.	Pt supported on alumina; 180℃, 50kg/cm, 2 hrs.
	the preparation of s	(2) Aluminum compound which is a linear polyminic polymer. ynthetic lubricating oils from	olefins.	
Process for t	the preparation of s LAO having 7-17 C atoms	which is a linear polyminic polymer. ynthetic lubricating oils from	olefins. Examples showed 0-50℃ for 30 minutes.	Nickel on kieselguhr catalyst, 250°C, 70 kg/cm, 5 hrs.

Assignee	Monomer(s)	Catalyst	Reaction Conditions	Hydrogenation
Institut Francais Du Petrole Preparation	Alpha-olefins having 6-16 C atoms of synthetic lubrical	Organic peroxides	Examples showed 250° -320°C and 3-5 hrs.	Raney nickel catalyst, 200°C, 50kg/cm hydrogen pressure(time not given).
Mobil Oil	1-Decene or mix- tures of 1-olefins between 6-12 C atoms having mean of 10 C atoms ion of olefins with B	(1) BF ₃ (2) Promoter such as 1~decanol	Examples showed 25°-35°C and 1-3 hrs.	Not shown.
	with b	Г 3.	***************************************	***************************************
Sun Oil	LAO having 6-14 C atoms	 Aluminum alkyl sesquich- loride or aluminum dialkyl monochloride or aluminum monoalkyl dichloride. Titanium tetrachloride. Oxygen-containing organic compound which is either an oxirane or a methyl alkyl ether. 	Examples showed 30°C and 20 hrs.	Raney nickel catalyst. 150° -250°C, 1000-2000 psig hydrogen pressure.
Preparation	of synthetic lubricat	ing oil.		
Sun Oil	LAO having 6-14 C atoms	 (1) Aluminum alkyl sesquichloride. (2) TiCl₄ (3) Oxirane or methyl alkyl ether (4) Diene capable of chelating with a metal component of the catalyst. 	Examples showed 30°C and 20 hrs.	Not shown.
Synthetic lu	bricating oil prepara			
Gulf	At least two alphaolefins having 6-16 C atoms. Mean C number per molecule is between 9 and 14.	Any Friedel-Crafts metal halide catalyst, AlCl ₃ preferred.	Examples showed 209°F and 35 minutes.	Not shown.
Copolymeriz		number and high carbon num	ber olefin fractions.	
Sun Oil	LAO having 6-14 C atoms	(1) TiCl ₄ (2) Aluminum alkyl compound. Above can be modified by the addition of certain oxygen-containing compounds.	Deposition of brown gummy film on surfaces within reactor prevented by carrying out reaction in the presence of activated carbon. Examples showed 30°C and 20 hrs.	150°-250°C and 1000-2500

Monomer(s)) having 6–14 oms	Catalyst (1) Alkyl aluminum sesquichloride. (2) TiCl ₄ (3) Oxygen-containing organic compound which is either an oxirane or	Reaction Conditions	Hydrogenation Raney nickel catalyst, 150°-250°C, and 1000-2500 psig, hydrogen pressure.
oms	sesquichloride. (2) TiCl ₄ (3) Oxygen-containing organic compound which	. -	250°C, and 1000-2500 psig,
ynthetic lubricat	a methyl alkyl ether.		

oms	sesquichloride. (2) TiCl ₄ (3) A tetraalkyl silicate.	Examples showed $15^{\circ}-30^{\circ}C$ for 20 hrs.	Not shown.
ring synthetic lu	bricating oil.		
) having 10-14 oms	Synthetic zeolites	Examples showed 400° - 650°C and 1/2-5 hrs.	Not shown. Mention is made of hydrogenation to reduce any unsaturation which may be present.
oricating oils.			oc prosent.
) having 6-12 oms			Nickel-on-kieselguhr catalyst, 300°F, 1500 psig hydrogen pressure, 3 hrs.
	oms 6-14 oms 9-14 oms 9-14 oms 9-14 oms 9-14 oms 9-12 oms 9-12 oms 9-12	O having 6-14 (I) Aluminum alkyl sesquichloride. (2) TiCl ₄ (3) A tetraalkyl silicate. ring synthetic lubricating oil. O having 10-14 Synthetic zeolites oms Oricating oils. O having 6-12 Di-tertiary butyl peroxide or Friedel-Crafts catalysts	O having 6-14 (I) Aluminum alkyl sesquichloride. (2) TiCl ₄ (3) A tetraalkyl silicate. Fing synthetic lubricating oil. O having 10-14 Synthetic zeolites O having 10-14 Synthetic zeolites O having 6-12 Di-tertiary butyl peroxide or Friedel-Crafts catalysts such as BF ₃ or AlCl ₃ Examples showed 15°-30°C for 20 hrs. Examples showed 400°-650°C and 1/2-5 hrs.

B. NEOPOLYOL ESTERS

Abbreviations
NPG: neopentyl glycol
PE: pentaerythritol
TME: trimathylolethans

TME: trimethylolethane TMP: trimethylolpropane

Assignee(s)	Polyol(s)*	Acid(s) †	Reaction Conditions
Texaco	PE	2-12 C atoms	Not given
	itable for bus or truck turbir I a methacrylate pour point de		een depressed by blending with at
Stauffer	TMP	Heptanoic acid	Not given.
	sed on a mixture of liquid neo americ decene-1), plus additi		olefin oligomer (hydrogenated mix-
Snamprogetti	PE, Di-PE, TMP	Heptanoic, caprylic, lauric, hexadecanoic.	210°240°C, no catalyst, no azeotroping agent.

Synthetic lubricants, suitable for base stocks for internal combustion engines having low volatility in relation to viscosity, high viscosity index, high thermal stability, good resistance against oxidation, good lubricating power and good compatibility with mineral oils.

	Abbreviations
NPG:	neopentyl glycol
PE:	pentaerythritol
TME:	trimethylolethane
TMP:	trimethyloloropane

Assignee(s)	Polyol(s)*	Acid(s) 1	Reaction Conditions
.F.P	TMP	Heptanoic, lauric, isostearic C_{10-16} saturated aliphatic monocarboxylic, adipic, azelaic.	Temperatures not given. No catalyst, no azeotroping agent.
	ble as base stock for automobile ing multigrade oils(20w-50) with		
I.F.P	TMP Polypropylene glycol	Heptanoic, isostearic, lauric, adipic. Esterification is completed with acetic anhydride.	lyst (p-toluenesulfonic acid)
	pared from esters by using a def cyl groups were then esterified by		
Unilever-Emery N. V.	PE, TMP	Heptanoic, pecargonic, isononanoic, isostearic	225°-250°C, no catalyst, either with azeotroping agen (toluene) or without azeotroping agent.
Synthetic lubricants, suitaindex, satisfactory rubber	able as base stock for piston eng seal swelling, good viscosity stab	ines, having low pour point, lility and good mineral or comp	high flash point, high viscosi patibility.
Hercules Inc.	PE. C_{6-10} alkanols, average $C=8$. C_7 alkanols.	5-9 C atoms, average C=6. 1. Trimellitic.	Not given.
Synthetic lubricants, suita cosities.	ble as base stock for jet engines,	having low pour point, suitable	e high and low temperature v
Texaco	PE(including di-tri-and tetra-), TMP	5-10 C atoms, straight and branched chain alipatic cycloaliphatic, aromatic and mixtures.	Not given.
	able for gas turbines or jet engin ti-wear, load-carrying and anti-		nperature range and exhibiting
Inventa A.G.	NPG, PE, TMP. Polyethylene glycol 200. 2-Ethy1-1- hexanol	Obtained as by-product in oxidation of cyclohexane to cyclohexanol/cyclohexanone. Butyric, valeric, caproic, hydroxycaproic, adipic.	No temperatures given. Sodium bisulfate, sulfuric acid or ptoluenesulfonic acid catalyst; toluene azeotroping agent.
Synthetic lubricants, suita	ble for jet engines, having low po	ur point, high flash point, high	viscosity index.
Ethyl Corp.	Di-PŁ, TMP	Valeric, caproic, caprylic, capric	150°-251°C, either with catalyst (sodium bisulfate or ptoluenesulfonic acid) or without catalyst, either with azeotroping agent (xylene) without azeotroping agent.
	able for use in turbines and turbo temperature stability and high a		subsonic and supersonic jet a

Abbreviations

NPG: neopentyl glycol PE: pentaerythritol TME: trimethylolethane TMP: trimethylolpropane

Assignee(s)	Polyol(s)*	Acid(s)	Reaction Conditions
Ruhrchemie	NPG	Pelargonic, 3, 5, 5-trimethyl- hexanoic	153°C, sulfuric acid catalyst, cumene azeotroping agent.
Synthetic lubricants, suit	able for use in turbojet subson	nic aircraft engines, noncorrosive a	and having low pour point, suit

Synthetic lubricants, suitable for use in turbojet subsonic aircraft engines, noncorrosive and naving low pour point, suitable high and low temperature viscosities, high flash point, adequate thermal and oxidation stability.

Nyco, S.A.

NPG, PE, di-PE, TME.
Trimethylolbutane, pentanediols, trimethylpentanediols

5-9 C atoms. Adipic, azelaic, Not given. sebacic

Synthetic lubricants, suitable for use in hydraulic transmissions and in racing-car engines.

Mobil Oil NPG, PE, di-PE, 5-10 C atoms. Not given. TME, TMP

Synthetic lubricants, suitable for use in jet aircraft turbine engines, having high temperature stability and low pour point.

Ethyl Corp.

Di-TMP

Average 4-9 C atoms.

Caprylic, capric, capric,
butyric, pivalic(2, 2-dimethyl 2 TMP 100°-250°C Di-TMP propanoic acid).

p-Toluenesulfonic acid catalyst, toluene azeotroping agent.

agent.
Esterification:

Temperatures not given. p-Toluenesulfonic acid catalyst, xylene azeotroping agent.

Synthetic lubricants, suitable for use in gas turbine aircraft engines, having high temperature stability, low viscosity at low temperature and a satisfactory lubricating viscosity at high temperature.

Mobil Oil Technical PE, TMP, 2methyl-2-ethyl-propane,
1, 3-diol Pelargonic, isopentanoic caprylic. Mono-carboxylic
acid having 1 to about 30
C atoms.

Synthetic lubricants, suitable for jet aircraft engines, having resistance to high temperature oxidation, complete fluidity at high and low temperatures, low rubber swell, high flash point, and resistant to breakdown.

at high and low temperatures, low rubber swell, high flash point, and resistant to breakdown.

Texaco

PE, di-PE, TMP

Straight-chain, branchedChain, cycloalipnatic,

aromatic and mixtures of these. 2-12 C atoms.

Synthetic lubricants, suitable for aircraft turbine engines, said to have outstanding oxidation and corrosion resistance and deposit-inhibiting properties.

Esso

2-Hydroxymethyl-2-decyl1, 3-propanediol

2, 2-Dimethyl pentanoic acid. No temperatures given. pPelargonic acid.

Toluenesulfonic acid catalyst,
xylene azeotroping agent.

Synthetic lubricants, suitable for SST-type jet engines, having high oxidative stability at engine temperatures up to 500°F(260°C), high viscosity indices, minimal corrosiveness, minimum high temperature evaporation loss and low pour points.

Abbreviations
NPG: neopentyl glycol
PE: pentaerythritol
TME: trimethylolethane
TMP: trimethylolpropane

Assignee(s)	Polyol(s)*	Acid(s) †	Reaction Conditions
Deutsche Erdol	2-Butyl-2-hexylpropanediol, 2-hexyl-2-octylpropanediol, 2-octyl-2-decylpropanediol	Caprylic, pelargonic, capric.	Not given.
Synthetic lubricants, suita	ble for use in aircraft engines and	l jet turbines, having low volat	ility and high viscosity index.
Geigy	PE	Mixture of straight and branched-chain aliphatic monocarboxylic acids. Mean C number of mixed acids within 7.2 8.5. % C atoms contributed by straight-chain acids greater than 60%. Heptanoic, caprylic, 2-ethyl-hexanoic.	200°-220°C, no catalyst, toluene azeotroping agent.
Synthetic lubricants, suita seal swell.	able for jet engines, having low v	colatility at elevated temperatu	ires and not causing excessive
B. P. Chemicals	Di-PE, TMP, ethoxylated with ethylene oxide of propylene oxide	Heptanoic, pelargonic, butyric, lauric.	115°-195°C, benzenesulfonic acid catalyst, xylene or toluene azeotroping agent.
Synthetic lubricants, suita	ble for internal combustion engine	es or stationary jet engines.	
British Petroleum	TMP, PE	Caprylic, sebacic, heptanoic, 2-ethylhexanoic	Not given.
Synthetic lubricants, suita capacity.	able for jet aircraft engines, havi	ng good resistance to oxidation	n and corrosion, and good loa
Sinclair	PE, TMP	3, 3-Dimethylpentanoic acid, 5, 5-dimethylhexanoic acid.	161°-210°C, no catalyst, xylene azeotroping agent.
Synthetic lubricants which viscosity indexes, lower po	h are subjected to higher temper our points and greater heat stabil	atures, such as in combustion ity than mineral oils of corresp	turbine engines, having higher onding viscosity.
Emery Industries, Inc.	NPG, PE, TMP. 2,2,4-Tri -methylpentanediol	Valeric, pelargonic	210°C, no catalyst, xylene azeotropic agent.
	se in aircraft gas turbine engines ving good low temperature viscosi		res, showing oxidation and co
Shell	PE, di-PE, TMP	C ₅₋₉ acids. Azelaic acid.	Not given.
Lubricants stable against	air oxidation.		
I.F.P.	NPG	Quaternary acids having 5-20 C atoms.	Chlorides of C_{15} – C_{19} acids + NPG, 80°C.
Thermally stable ester lub	pricants of low pour point.		
Tenneco	РЕ, ТМР	Pelargonic. Di-2-methyl- pentanoic.	Not given.

Abbreviations
NPG: neopentyl glycol
PE: pentaerythritol
TME: trimethylolethane
TMP: trimethylolpropane

Assignee(s)	Polyol(s)*	Acid(s) †	Reaction Conditions
British Petroleum	PE, TMP	Caprylic, capric, caproic, pelargonic, heptanoic, sebacic azelaic	Not given.
Synthetic lubricants, suita high temperatures.	•	having resistance to oxidation and	loss of load-carrying ability at
Drew Chemical Corp.	Technical PE	2-6 alkanoic acids, 5-9 C atoms, 6-7. 25 average number of carbon atoms, 60% = maximum number of C atoms contributed by caprylic and pelargonic acids. 45% = maximum number of C atoms contributed by branched-chain acids.	no azeotroping agent.
Synthetic lubricants, suita	able for jet engines, able to v	vithstand temperatures above 300°F	and down to -40°F.
Socony Mobil	Technical PE	Commercial isopentanoic(2 parts by wt valeric+1 part by wt isovaleric), pelargonic.	_
	ty, no coke or sludge format	nd fluid over a wide temperature ra	inge, low volatility at high tem-
British Petroleum	TMP	Caprylic, sebacic	Not given.
Synthetic lubricants, suit noncorrosive to metal.		es, resistant to high temperatures,	having a high viscosity index
Shell	PE, TME, TMP	Pivalic	Pivalyl chloride+ pyridine+PE, 4°-85°C
tures of such engines.		idation and thermal decomposition	at the high operating tempera
Shell	TME	4-10 C atoms, including, 4-6 mol% capric acid or capric halides. At least two different acvl groups. Even number of C atoms preferred.	azeotroping agent.
Synthetic lubricants, suit aircraft or other gas turb	oine lubricants.	rature machinery operating at 400°	F(204°C) or above. For use a
Geigy	NPG, PE, TMP	3–10 C atoms. Saturated straight–chain dicarboxylic acid having 4–14 C atoms.	No temperatures given, no catalyst. Toluene azeotroping agent.
	ing better viscosity charactengines subjected to extremes	ristics than conventional diester lub in temperature.	ricants, particularly suitable fo
Geigy	NPG, PE(mono-, di-, TMP, 2-methyl-2-n- ₁ 1,3-propanediol	tri-) Acetic, butyric, valeric, propyl-caproic, heptanoic.	80°-160°C. p-Toluenesulfor ic acid catalyst. Benzene o xylene azeotroping agent.

Synthetic lubricants, also suitable for use as plasticizers. Made from capryl alcohol by-product in the manufacture of sebacic acids.

Assignee(s)

Abbreviations

NPG: neopentyl glycol

PE: pentaerythritol
TME: trimethylolethane
TMP: trimethylolpropane trimethylolpropane

Reaction Conditions 5

TME	4-6 C atoms for two hydroxyl groups, 7-10 C atoms for third hydroxyl group. Butyric, iso-butyric, n-valeric, isovaleric, 2-ethylbutyric, caproic, heptanoic, caprylic, 2-ethylhexanoic, pelargonic, capric. Average chain length of 5.6 -7.0 carbon atoms.	175°C, no catalyst, xylene azeotroping agent.
lash point and sufficient viscosity	at high temperature.	***************************************
IME, IMP	caprylic, pelargonic, capric, lauric.	175°-180°C, no catalyst, xylene azeotroping agent.
		temperature and oxidation sta
Di-PE	2-12 C atoms, in proportions to give an average chain length of 5-10 C atoms.	147°-237°C, no catalyst, toluene azeotroping agent.
gas turbine aircraft engines, suitab	ole for bulk oil temperatures ab	ove 150℃.
TMP, TME, PE. Also alkanols with 8-10 C atoms	5-8 C atoms. Alkane dioic acids of 6-10 C atoms.	158°-253℃, no catalyst, xylene azeotroping agent.
use in jet engines and having opti	mum high and low temperatur	e properties with low degree of
NPG, TME, TMP, PE, 2-butyl-2-ethyl-1, 3-propanediol, 2, 2, 4-trimethyl-1, 3-pentanediol	Average chain length of between 4 and 12 C atoms, preferably between 5 and 9 carbon atoms. No more than 2 carbon atoms in side chains if branched chains are used.	216°-259°C, no catalyst, xylene azeotroping agent. Yields: On polyols: 86-95.5% s, On acids: 90.4-96.6%
	et aircraft engines, having high vilash point and sufficient viscosity: TME, TMP gas turbine aircraft engines, having a dood low temperature propertion. Di-PE gas turbine aircraft engines, suitable aircraft engines, suitable aircraft engines, suitable alkanols with 8-10 C atoms alkanols with 8-10 C atoms use in jet engines and having optimals. NPG, TME, TMP, PE, 2-butyl-2-ethyl-1, 3-propanediol, 2, 2, 4-trimethyl-1,	hydroxyl groups, 7-10 C atoms for third hydroxyl group. Butyric, iso-butyric, n-valeric, isovaleric, 2-ethylbutyric, caproic, heptanoic, caprylic, 2-ethyl- hexanoic, pelargonic, capric. Average chain length of 5.6 -7.0 carbon atoms. et aircraft engines, having high viscosity indexes, good oxidation lash point and sufficient viscosity at high temperature. TME, TMP Butyric, valeric, caproic, caprylic, pelargonic, capric, lauric. gas turbine aircraft engines, having high viscosity indexes, high and good low temperature properties. Di-PE 2-12 C atoms, in proportions to give an average chain length of 5-10 C atoms. gas turbine aircraft engines, suitable for bulk oil temperatures ab TMP, TME, PE. Also alkanols with 8-10 C atoms acids of 6-10 C atoms. suse in jet engines and having optimum high and low temperatur NPG, TME, TMP, PE, 2- butyl-2-ethyl-1, 3-prop- anediol, 2, 2, 4-trimethyl-1, 3-pentanediol Average chain length of between 4 and 12 C atoms, preferably between 5 and 9 carbon atoms. No more than 2 carbon atoms. No more than

Polyol(s)*

Synthetic lubricants, having high thermal stability, for high performance jet aircraft engines, cannot be made from neopentyl polyols and alkanoic acids having an average chain length of between 4 and 12 carbon atoms, if acid catalyst has a dissociation constant higher than that of acetic acid.

Heyden Newport Chemical Corp.

NPG, TME, TMP PE. Trimethylolbutane

Saturated aliphatic dicarbox- 160°-181°C, phosphoric acid ylic and aromatic dicarbox-ylic acids having from 2–36 agent.

Acid(s) 1

C atoms. Mono-carboxylic acids, including those with branched chains, and having

from 2-22 C atoms.

Synthetic lubricants suitable for jet aircraft engines, suitable for high and low temperatures can be made from neopolyols, dibasic acids, and monocarboxylic acids.

Abbreviations

NPG: neopentyl glycol

Reaction Conditions 5

PE: pentaerythritol
TME: trimethylolethane
TMP: trimethylolpropane

E. F. Drew & Co., Inc. Mixture of mono-and dibasic 147°-230°C, no catalyst. Mono-and di-PE, TME, acids, sufficient to combine hexanetriol, glycerol

Polyol(s)*

with hydroxyl groups. Adipic, maleic, terephthalate, isophthalic, azelaic, sebacic, capric, caprylic.

Acid(s) ↑

Synthetic lubricants for aviation engines, suitable from below o°F to above 500°F can be made from mixed linear esters of polynydric alcohols and mixtures of mono-plus dicarboxylic acids.

 260° – 280° C with PE. Yield 98–100% theoretical. I.C.I. PE and poly-PE. Also more than 10 carbon atoms. Also includes cycloaliphatic. includes other polyhydric alcohols. Saturated or unsaturated. Also includes polycarboxylic acids.

Use of heat-activated alumina as catalyst overcomes disadvantage of sulfuric acid catalyst which causes charring of many polyhydric alcohols. Spent alumina is insoluble and can be mechanically separated and reactivated.

* Technical grade PE is 88 wt % PE plus 12 wt % Di-PE.

Acids are linear aliphatic monocarboxylic, unless otherwise specified.

Esterification pressure is atmospheric, unless otherwise specified.

C. DIBASIC ACID ESTERS

Assignee(s)

	(A) Dodecane diacid, (B) azelaic acid s to decrease pour points or indith higher branched primary ald Mixture of dicarboxylic acids having 8-12 carbon atoms	Tetrabutyl titanate catalyst, 180°-200°C. crease viscosities of mineral oils. cohols. Excess alcohol, catalyst, azeotroping agent, 8 hrs
diacid and azelaic acid w	ith higher branched primary ald Mixture of dicarboxylic acids	Excess alcohol, catalyst,
Ethylhexanol		
		reflux. No temperature given.
ed dicarboxylic acids hav		
Butyl alcohol, l-butanol	Heptadecanodioic acid	No examples given.
	Trimethyladipic acid	5 hrs under reflux at 155°C, cumene azeotroping agent, ptoluenesulfonic acid catalyst.
	Butyl alcohol, l-butanol istant and cold-resistant. atic alcohols of less than "Oxo"-octanol, n-"Oxo"-oranol	

Synthetic lubricants for turbine engines, which meet MIL-L-7808 specifications. Esters of easily obtainable, commercially available alcohol and acid components. Mixture of diol diester, neopolyol esters, and dibasic acid diester.

Assignee	Alcohol(s)	Acid(s)	Reaction Conditions
Monsanto	B,B-Dimethylphenylethyl alcohol	3,3-Dimethylglutaric anhydride	p-Toluenesulfonic acid catalyst, toluene azeotroping agent, 155°C to solution. Esterification temperature not given. Toluene removed until 180°C reached. Further heating for 4 hrs at 165°C. (Acyl chloride examples also given.)
high temperatures, having	at temperatures well below 32 g high thermal and oxidative st ta carbon atoms of the alcohol of	ability. Diesters having termin	viscosity relatively unaffected a al dimethylphenyl groups and no
Castrol	Branched aliphatic primary alcohols	C ₅ -C ₁₇ dicarboxylic acids	No examples given.
Synthetic lubricants, suita dicarboxylic acids and bra	able for use in gasoline and die anched aliphatic primary alcohol	sel piston engines and in indu ls. Miscible with mineral oil in	strial and gas turbines. Esters o all proportions.
Scholven-Chemie AG	n-Butanol, n-hexanol, n- octanol, n-decanol, n- nonanoi, n-dodecanol	Trimethyladipic acid	No reaction examples given. Residual acidity removed by magnesium oxide or magnes- ium hydroxide.
losses at operating temper gines. Esters of trimethyl	ratures and adequate shearing,	oxidation and thermal stability	nigh flash point, low evaporation y. Lubricants suitable for jet er erification with mixtures of alco
Technochemie GmbH	2-Ethylhexanol	C ₁₉ -dicarboxylic acid	100% excess alcohol, sulfuric acid catalyst, toluene azeotro- ping agent, 36 hrs reaction. No temperatures given.
Synthetic heavy duty lubr having 4 carbon atoms.	cicants prepared from esters of	dicarboxylic acid having 19 ca	rbon atoms and primary alcohol
Technochemie GmbH	2-Ethylhexanol	Heptadecanedicarboxylic acid	Benzene azeotroping agent, conc. sulfuric acid catalyst, 35 hrs reflux. No temperature: given.
chain dicarboxylic acids h	suitable viscosity characteristic naving 19 carbon atoms with st e for blending with natural or o	raight or branched chain prim	repared from esters of branched- ary alcohols having 3–19 carbo
chain dicarboxylic acids h	naving 19 carbon atoms with st	raight or branched chain prim ther synthetic lubricants. (Normal+150)-C ₁₉ -dicarbo	ary alcohols having 3-19 carbo
chain dicarboxylic acids hatoms. Lubricants suitable. Ruhrchemie	naving 19 carbon atoms with stee for blending with natural or o 2-Ethylhexanol;3,5,5- trimethyl-hexanol	raight or branched chain prim ther synthetic lubricants. (Normal+150)-C ₁₉ -dicarbox ylic acid	ary alcohols having 3–19 carbo x- 100% excess alcohol, p- toluenesulfonic acid catalyst or without catalyst, toluene azeotroping agent or without azeotroping agent, 85–90% molar yield. No temperatures given. Up to 24 hrs esterifica-
chain dicarboxylic acids hatoms. Lubricants suitable	naving 19 carbon atoms with stee for blending with natural or o 2-Ethylhexanol; 3,5,5- trimethyl-hexanol greater than 300°C range betw	raight or branched chain prim ther synthetic lubricants. (Normal+150)-C ₁₉ -dicarbox ylic acid	x- 100% excess alcohol, p-toluenesulfonic acid catalyst or without catalyst, toluene azeotroping agent or without azeotroping agent, 85-90% molar yield. No temperatures given. Up to 24 hrs esterification.

Ⅱ. 윤활유 첨가제 특허정보 분석

A.1 POLYALKENYL SUCCINIMIDE

	Objective	Mol Wt Polymer	Amine	Mol Ratio Amine:SA	Solvent	<u>Temperature</u>	Time (hr)
	Improve sludge dispersion and varnish inhibition	Approx. 900 min	Polyethylene Polyamines	0.1:1 to 1:1			
	Combined dispersant- VI improver	40,000- 200,000	Polyethylene- Polyamines	0.5:1 to 0.1:1	Toluene	110℃ (230°F)	6
	Improved dispersant	900	Tris(5-amino- -thiapentyl) amine	3	Methanol	155℃ (311°F)	3
	Reduce required additive concentration in lube oil	900	Aminoalkoxy- amines	0.4:1 to 0.6:1	Lube oil	140-180℃ (284-356°F)	4
	Shear-stable VI improver-dispersant	1,700	Polyamines	1:1	Mineral oil	125℃ (257°F)	2
	Pure amine raw material	1,870	3-(2-Amino- propylamino)- ethane		Toluen e	100-200°C (212-392°F)	. 3
	Dispersant-VI improver	1,300- 5,000	Ethylene polyamines	0.25:1 to 2:1	Oil	150-210℃ (302-410°F)	2-4
	Dispersant-detergent		Diamines		Oil	125℃ (256°F)	2
	ene copolymer. Improved dispersant	6,000	(Octadecylamino)			170°C (338°F)	3
	High nitrogen content cal initiator, e. g., 0.5-1.29	750- 1,500 5% organic	Mono- or polyamines peroxide	2:1 to 5:1		90℃ (194°F)	1-3
	Dispersant with corrosion and foam inhibition	1,000	N, N, N ¹ , N ¹ - tetrakis(3- aminopropyl) ethylenediamir	Various	Oil	120-150℃ (248-302°F)	4-5
	Basic dispersion agent	1,300	Polyethylene- imine		Xylene	160℃ (320°F)	3
	Antirust dispersant	300- 7,000	Alkylene polyamines		Oil	100-200°C (212-392°F)	4
Alkenyl SA reacted	with a bis-succinimide or ar	n ester of a	n alkenyl SA.		,		
	Improved dispersant	1,000	Polyamine eth	er		160℃ (320°F)	3
Polyamine ether pre	epared by cyanoethylation an	d hydrogen	ation of triethar	nolamine.			
	Mixed dispersants	875 and 1,300	TEPA	-	Toluene	202℃ (396°F)	25
0 11 11 1	on PIB of 875 mol wt heated	LL DID	أوالم المساورة والمساورة	la bused on 1	200 mal	t to aivo mived	imid

	Objective	Mol Wt Polymer	Amine	Mol Ratio MA:PIB		Temperature	Time (hr)
	Economic purification process	900- 2,000	Polyethylene- polyamines	0.1:1 to 1:1		100-200℃ (212-392°F)	8
Reaction product treat	ted with in ganic base.						
Texaco Inc.	High nitrogen content	900- 2, 000	Alkylene polyamines	0.5:1 to 2:1		100-200℃ (212-392°F)	6
SA made from dehydr	ohalogenated PIB.						
Texaco Development Corp.	Detergent-dispersant	1,250	Ethylenedi- amine	1:6.25	None	100-200℃ (212-392°F)	************
Treated with NaOH a	t 20-150℃ (68-302°F) at	fter reaction	with amine.				
USSR	Simplified process		Polyamines				
MA removed from co	ndensation produced by h	ydrolysis.					
Sanwa Kasei Kogyo Co., Ltd.	Dispersant-VI improver	500– 5,000	Diethylene- triamine	1:1	Toluene, mineral oil	95℃ (203°F)	3
Heated with LiOH · H	I ₂ O to give final product.						
Texaco Inc.	Dispersant with anticorrosion properties	500- 3,000	Ammonia	1:1	Polyisob- utene	100-250℃ (212-482°F)	2
Used as intermediate	for overbased Ca salt.						
Texaco Inc.	Improved thermal stability	700- 3,000	Polyethylene- amines	1:1		200℃ (392°F)	
Unstable compounds o	decomposed by heating to	250-300℃,	extracting with al	cohol.			
Lubrizol Corp.	Minimize emulsion formation	700- 5,000	Polyoxyalkolene polyamines	0.1:1 to 2:1		125-250℃ (256-482°F)	1.5- 6
Preferred amines hav	e mol wt of at least 400.						
Lubrizol Corp.	Increase demulsifying characteristics	700- 5 , 000	Polyoxyalkylene polyamines	0.1:1 to 2:1	Mineral oil	150-200℃ (302-392°F)	4-5
Use of polyoxyalkyler	ne amines prevents forma	tion of emuls	ion in crankcase.				
British Petroleum Co. Ltd.	Highly basic ashless dispersant	840 max.	Polyamine and sec. or tert. monoamine	1:1	Aromatic hydrocarbo	160-170°C (320-338°F) on	5
	of polyamine and monoar from low molecular weig			recovered f	rom reaction	mixture. High	h base
	Increased high temperature perfor mance		Polyethylene- polyamine	#7#		145-155℃ (293-311°F)	

A.2 POLYALKENYL SUCCINIC ANHYDRIDE

	Objective	Mol Wt Polymer	Mol Ratio MA:PIB	Promoter	Temperature	Time (hr)	% PIB Conversion
	Simplify process	300-3,500	C.5:1 to 2.0:1	Oxygen(air)	180-225℃ (356-437°F)	5-10	45-52
Texaco Inc.							
Orobis, Ltd.	Make polyalkenyl bis(succinic anhydride)	500-2,100	1:1 to 3:1	Nickel iodide	230-250℃ (446-482°F)	6-12	70
Reaction carried out	under 30–45 psig N ₂ . Pro	duct is mixtur	e containing	up to 40% bis	(succinic anhy	dride)	•
Shell oil Co.	Reduce C1 ₂ content of product	300-200,000	1.7:1	Chlorine	180℃ (356°F)	9	83
Ratio C1 ₂ : MA = 0.67	:1. Chlorination time:5 hr	at 180°C, the		nt: 4 hr at 180	o℃.		
Texaco Inc.	Improve yield, reduce tar formation		0.9:1	Brominated phenol, e.g., orthobromo- phenol	235–265℃ (455–509°F)	6	
Preferred Br concent	ration: 10-250 ppm.						
Shell International Research Maatschappii B.V.	Increase conversion of PIB	500-250	1:1 to 2:1	Chlorine	160-210℃ (320-410°F)	3-7	78-90
After chlor ation, mi with alcohol-wate m	xture heated at 160-210° ixture.	C for about 2	thr under ref	lux. Tars and	excess MA re	move	l by washi
Lubrizol Corp.	Reduce C1 ₂ consumption	750-3,000	1:1	Chlorine	175-200℃ (347-392°F)		}
Molar ratio C1 ₂ :MA	=0.5:1.0 to 0.7:1.0 Cl ₂ m	nay be added i	intermittently				
Texaco Inc.	Increase nitrogen content of succinimide	900-2,000	0.2:1 to 2:1	Chlorine	100-250℃ (212-482°F)		
Polyalkene chlorinate	ed at about 120°C then de	hydrochlorina	ted at about	235℃ to increa	ase reactivity	with N	IA.
Standard Oil Co. (Indiana)	Improve yield, reduce tar formation	300-3,000	0.9:1.0	Chlorinated or brominated carboxylic or sulfonic acid	(480°F)	6	64-74
(mgiana)				sulforne acid			

MA = Maleic anhydride.

PIB = Polyisobutene.

B. ZINC DIHYDROCARBYLDITHIOPHOSPHATES

Earliest Date	Assignee	Objective
6/19/80	Chevron Research Co.	Inhibit oxidation and corrosion
Zinc salt of lower(2-3 carl alkenyl or alkyl succinimide.	oon atoms) dialkyldithiophosphoric	c acid reacted with an oil-soluble
2/25/80	Shell International Research	Extreme pressure antioxidant
Zinc salts prepared from alkylsalicylates.	acid based on alcohols cont	aining oxyalkylene groups, e.g.,
5/31/79	Lubrizol Corp.	Extreme pressure antioxidant
Additive consists of mixed malicyclic carboxylic acid.	netal salts of di(hydrocarbyl)dithio	phosphoric acid and an aliphatic or
4/2/79	Chevron Research Co.	Extreme pressure additive with improved wear prevention properties.
	phenyl, oly(oxyalkylene)dithiophos nol with 1,2-epoxybutane, P ₂ S ₅ , ar	phate. Example compound prepared and ZnO.
3/9/79	Orogil SA	Novel extreme pressure antiwear additive

Additive is a metallic (preferably Zn) dithiophosphate made by reacting ZnO with

Where Rl is an alkyl, olefinyl, cycloaliphatic aryl, or heterocyclic radical and R_2 and R_3 are alkyl radicals containing 1-4 C atoms.

3/9/79 Orogil SA Novel extreme pressure antiwear additive with improved heat stability

Zinc dithiophosphate of composition shown in (486145) is reacted with an alkyl ester with the aid of a sulfurization agent.

	Assignee	Objective
3/1/79	Mobil Oil Corp.	Antiwear, antioxidant additives with improved oil solubility, odor, and corrosivity characteristics
	ting the reaction product of alkyl-ctive olefin, epoxide, unsaturated alde	or aryldithiophosphoric acids and a sul chyde, or other reactive compound.
12/29/78	Standard Oil Co.(Indiana)	Haze-free zinc dihydrocarbyl- dithiophosphates
Surface active agent add	ed to reactants just before addition of	of zinc oxide.
6/29/77	Chevron Research Co.	New method for preparing mixed alkyl-aryldithiophosphates
	phosphoric acids mixed and heated a hiophosphoric acid, which is then ne	at 55-95°C to form approximately 20- utralized with ZnO.
5/23/77	Standard Oil Co.(Indiana)	Improve neutralization, reduce amount of excess metal base required
		xcess promoter neutralized a nitrogen
or urea).	rms a salt and does not replace met	al in the dithiphosphate (e.g., ammoni
	rms a salt and does not replace met Standard Oil Co.(Indiana)	al in the dithiphosphate (e.g., ammoni Continuous neutralization of dithiophosphoric acids
3/28/77 Neutralization mixture parease contact time. Wat	Standard Oil Co.(Indiana)	Continuous neutralization of dithiophosphoric acids
3/28/77 Neutralization mixture parease contact time. Wat	Standard Oil Co.(Indiana) bumped through a static mixer, cocer of reaction removed by blowing was a static mixer.	Continuous neutralization of dithiophosphoric acids
Neutralization mixture percease contact time. Wat temperature 100-170°F	Standard Oil Co.(Indiana) bumped through a static mixer, concer of reaction removed by blowing v (38-77°C); excess ZnO, 20-60%. USSR 0.15-1:1 mol ratio mixture of polya	Continuous neutralization of dithiophosphoric acids oler, and a small holding vessel to in with nitrogen in stirred tanks. Reactio Increased antioxidant and detergent properties alkylene glycol C ₁₋₁₀ alkylphenyl ether
Neutralization mixture perease contact time. Wat temperature 100-170°F	Standard Oil Co.(Indiana) bumped through a static mixer, concer of reaction removed by blowing v (38-77°C); excess ZnO, 20-60%. USSR 0.15-1:1 mol ratio mixture of polya	Continuous neutralization of dithiophosphoric acids oler, and a small holding vessel to in with nitrogen in stirred tanks. Reactio Increased antioxidant and detergent properties
Neutralization mixture perease contact time. Wat temperature 100-170°F 3/10/77 Hydroxyl compound is 0 and polyalkylene glycol 0 3/10/77 Mono- and polyglycol et	Standard Oil Co.(Indiana) bumped through a static mixer, coder of reaction removed by blowing v (38-77°C); excess ZnO, 20-60%. USSR 0.15-1:1 mol ratio mixture of polya C ₃₋₂₀ alkylphenyl ether. USSR	Continuous neutralization of dithiophosphoric acids oler, and a small holding vessel to in with nitrogen in stirred tanks. Reaction Increased antioxidant and detergent properties alkylene glycol C ₁₋₁₀ alkylphenyl ether improved additives toms in the alkyl group and 1-7 glycon
Neutralization mixture perease contact time. Wat temperature 100-170°F 3/10/77 Hydroxyl compound is 0 and polyalkylene glycol 0 3/10/77 Mono- and polyglycol et	Standard Oil Co.(Indiana) bumped through a static mixer, coder of reaction removed by blowing v (38-77°C); excess ZnO, 20-60%. USSR 0.15-1:1 mol ratio mixture of polya C ₃₋₂₀ alkylphenyl ether. USSR hers of alkylphenols with 1-10 C at	dithiophosphoric acids oler, and a small holding vessel to in with nitrogen in stirred tanks. Reaction Increased antioxidant and detergent properties alkylene glycol C ₁₋₁₀ alkylphenyl ether improved additives toms in the alkyl group and 1-7 glycon

Earliest Date	Assignee	Objective
3/27/76	Edwin Cooper and Co., Ltd.	Improve neutralization for zinc diaryldithiophosphates
Reaction of ZnO with acid	d promoted by conducting it in miner	ral oil treated with NO ₂ .
2/25/76	Chevron Research Co.	Prepare mixed dialkyldithiophos- phates
•	secondary alcohols reacted with P ₂ S°C) to form Zn-dialkyldithiophosphar	$_{5}$ at 176°F (80°C), added to slurry of tes.
12/19/74	Texaco Inc.	Improved additive for automatic transmission oil
Additives prepared from n-octadecyloxyethyoxyet	long, straight-chain alcohols, acids, a	and thiols, e.g.,
12/1/72	USSR	Antiabrasive additive
	hiophosphoric acids neutralized with	
Dialky- or dialkylaryldit	hiophosphoric acids neutralized with	
Dialky- or dialkylaryldit treated with a Cl-contair 10/12/7	hiophosphoric acids neutralized with hing hydrocarbon.	n KOH solution and the resultant salt
Dialky- or dialkylaryldit treated with a Cl-contair 	Chiophosphoric acids neutralized with ning hydrocarbon. Texaco Development Corp.	n KOH solution and the resultant salt
Dialky- or dialkylaryldit treated with a Cl-contain 10/12/7 Mixture of methylisobuty	Chiophosphoric acids neutralized with hing hydrocarbon. Texaco Development Corp. I alcohol and dimethylcarbinol used. Czechoslovakia	Improve stability Improve thermal stability
Dialky- or dialkylaryldit treated with a Cl-contain 10/12/7 Mixture of methylisobuty 1/10/72 Mixture of 2-ethylhexan	Chiophosphoric acids neutralized with hing hydrocarbon. Texaco Development Corp. I alcohol and dimethylcarbinol used. Czechoslovakia	Improve stability Improve thermal stability
Dialky- or dialkylaryldit treated with a Cl-contain 10/12/7 Mixture of methylisobuty 1/10/72 Mixture of 2-ethylhexan ZnO in benzene.	Czechoslovakia ol and isobutyl alcohol reacted with I Texaco Inc. thiophosphate and Zn-bis[(2-alkyl-	Improve stability Improve thermal stability P ₂ S ₅ , diluted with ethanol, reacted with Nitration inhibition phenoxy)ethyl] dithiophosphate added
Dialky- or dialkylaryldit treated with a Cl-contain 10/12/7 Mixture of methylisobuty 1/10/72 Mixture of 2-ethylhexan ZnO in benzene. 12/9/70 Mixture of Zn-dialkyldit	Chiophosphoric acids neutralized with hing hydrocarbon. Texaco Development Corp. I alcohol and dimethylcarbinol used. Czechoslovakia ol and isobutyl alcohol reacted with land to the	Improve stability Improve thermal stability P ₂ S ₅ , diluted with ethanol, reacted with Nitration inhibition phenoxy)ethyl] dithiophosphate added
Dialky- or dialkylaryldit treated with a Cl-contain 10/12/7 Mixture of methylisobuty 1/10/72 Mixture of 2-ethylhexan ZnO in benzene. 12/9/70 Mixture of Zn-dialkyldit to lubricating oil. 7/24/70	Chiophosphoric acids neutralized with hing hydrocarbon. Texaco Development Corp. I alcohol and dimethylcarbinol used. Czechoslovakia ol and isobutyl alcohol reacted with land to the	Improve stability Improve thermal stability P ₂ S ₅ , diluted with ethanol, reacted with Nitration inhibition phenoxy)ethyl] dithiophosphate added High temperature stability