4:1 평면수축유동에서 보이는 Phan-Thien Tanner 모델의 수치 모사

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Numerical Simulation of linear Phan-Thien Tanner model in a 4:1 planar contraction flow

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Introduction

Phan-Thien Tanner model was derived from network theories of concentrated polymer solutions and melts, and was first introduced by Phan-Thien and Tanner[1]. As the Phan-Thien Tanner model is one of the nonlinear rheological models, it has been used to describe the rheological properties of shear-thinning solutions such as PAA, PIB/C14, LDPE and so on. Among them, the linear version of Phan-Thien Tanner model can be written like below.

$$\tau + \varepsilon \frac{\lambda}{\eta} tr(\tau)\tau + \lambda \overset{\nabla}{\tau} = 2\eta \mathbf{D} \tag{1}$$

 τ and D are the extra-stress tensor and the deformation-rate tensor, λ is the relaxation

time and η is a constant viscosity. And τ denotes the upper-convected derivative.

$$\overset{\nabla}{\tau} = \frac{\partial \tau}{\partial t} + \mathbf{u} \cdot \nabla \tau - \tau \cdot \nabla \mathbf{u} - (\nabla \mathbf{u})^{T} \cdot \boldsymbol{\tau}$$
 (2)

Though shear parameter, ξ is omitted in the linear version, (1) can tell the shear-thinning behavior of polymer solutions with ε only, where ε is from Trouton viscosity data and linked to the extensional experiments[1].

Theory

To begin the numerical approach the flow of viscoelastic material in a sudden contraction geometry, we should solve the simultaneous equations including the mass conservation, momentum conservation and constitutive equation. By using the stabilizing techniques, we could obtain more accurate solutions. DEVSS-G/DG methods play an important role of stabilizing the system[2, 3]. With a fractional step method, it is possible to analyze the unsteady motions of contraction flow[4]. The final forms of governing equations as a FEM formulation are written as follows:

$$\left\langle \psi; \tau + tr(\tau)\tau + We\left(\frac{\partial \tau}{\partial t} + \mathbf{u} \cdot \nabla \tau - \tau \cdot \mathbf{G}^{\tau} - \mathbf{G}\right) - \eta(1 - \beta)(\mathbf{G}^{\tau} + \mathbf{G})\right\rangle - \sum_{c=1}^{N} \int_{\Gamma} \psi : \mathbf{u} \cdot \mathbf{n}(\tau - \tau^{ce}) d\Gamma = 0$$
(3)

where $\langle A;B\rangle$ denotes $\int_{\Omega}ABd\Omega$ on domain Ω , **n** is a normal vector which has the outward direction at the boundary of finite elements. $\boldsymbol{\tau}^{ex}$ takes the upstream additional stress value in the region of $\mathbf{u} \cdot \mathbf{n} < 0$.

$$\left\langle \phi : Re\left(\frac{\overrightarrow{\mathbf{u}} - \mathbf{u}^{n}}{\Delta t} + \frac{1}{2} (\overrightarrow{\mathbf{u}} \cdot \nabla \overrightarrow{\mathbf{u}} + \mathbf{u}^{n} \cdot \nabla \mathbf{u}^{n}) \right) \right\rangle = -\left\langle \nabla \cdot \phi : p^{n} \right\rangle + \left\langle (\nabla \phi)^{T} : \frac{1}{2} (\tau^{n+1} + \tau^{n}) + \frac{1}{2} (\nabla \overrightarrow{\mathbf{u}} + \nabla \mathbf{u}^{n}) \right\rangle$$

$$-\left\langle (\nabla \phi)^{T} : (1 - \beta) \left(\frac{3}{2} (\mathbf{G}^{n} + (\mathbf{G}^{n})^{T}) - \frac{1}{2} (\mathbf{G}^{n-1} + (\mathbf{G}^{n-1})^{T}) \right) \right\rangle$$

$$(4-1)$$

$$\left\langle \phi; Re \frac{\mathbf{u} \cdot \mathbf{u}}{\Delta t} \right\rangle = \left\langle \nabla \cdot \phi; \frac{1}{2} p^n \right\rangle \tag{4-2}$$

$$\left\langle \nabla \cdot \phi; \frac{1}{2} \nabla p^{n+1} \right\rangle = \left\langle \nabla \cdot \phi; \frac{Re}{\Delta t} \mathbf{u}^{\star} \right\rangle \tag{4-3}$$

$$\left\langle \phi; Re \frac{\mathbf{u}^{n+1} - \mathbf{u}^*}{\Delta t} \right\rangle = -\left\langle \nabla \cdot \phi; \frac{1}{2} p^{n+1} \right\rangle \tag{4-4}$$

$$\left\langle \varphi; \mathbf{G}^{n+1} - \left(\nabla \mathbf{u}^{n+1} \right)^r \right\rangle = 0 \tag{5}$$

where ψ , ϕ and φ are linear basis function, Reynolds number and Weissenberg number are the dimensionless groups like as $Re = \frac{L\overline{u}\,\rho}{\eta}$, $We = \frac{\overline{u}\,\lambda}{L}$ respectively. L is the downstream width and \overline{u} is the average velocity in a downstream. With above algorithms, we can show the different phenomena in a complicated flow predicted by linear Phan-Thien Tanner model and Oldroyd-B model. And β is assumed to be 1/9 in both cases.

Results & Discussion

We obtained the steady solutions of high We flow with relative finer mesh which consists of 2641 elements. The time increment was $\Delta t=2\times10^{-3}$ and the relative error for steady criterion was order of ten to -6.

The differences of the numerical results predicted by another constitutive models are found at a glimpse of vortex dynamics evidently. In Fig. 1, linear Phan-Thien Tanner model shows the corner vortex enhancement mechanism. Contrary to those, the so-called lip vortex enhancement mechanism is discovered in case of the Oldroyd-B model in Fig. 2.

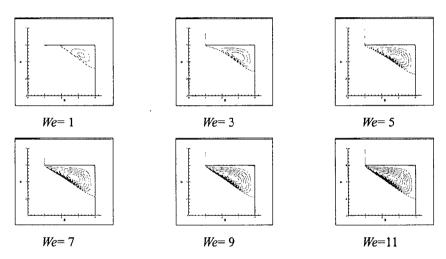


Fig. 1. Vortex dynamics of LPTT model ($\varepsilon = 0.25$) in case of $Re=10^{-1}$ ($\Delta \psi = 5 \times 10^{-4}$).

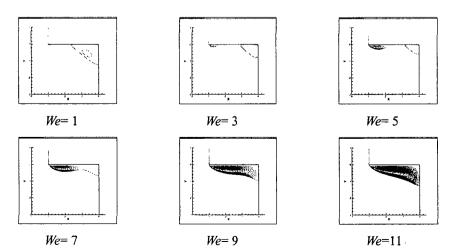


Fig. 2. Vortex dynamics of Oldroyd-B model in case of $Re=10^{-1}$ ($\Delta \psi = 5 \times 10^{-4}$).

Also the notable differences between two models can be observed in case of the stress distributions near the contraction plane. The normalized first normal stress difference,

 $N_{\rm t} (= \tau_{\rm sv} - \tau_{\rm xx})$ with $T_{\rm w} = 3\eta \overline{u} / L$ are shown in Fig. 3.

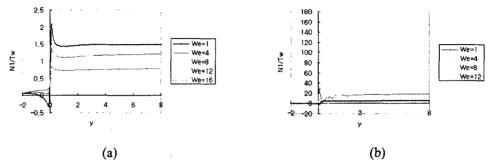


Fig. 3. First normal stress difference along the downstream wall of LPTT model (a) and Oldroy-B model (b).

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